## EXHIBIT 4

#### VOL I

#### Exhibit 4

## U.S. Army Center for Health Promotion and Preventive Medicine

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WASTEWATER TREATMENT PLANT
PERFORMANCE EVALUATION
SOLO POINT WASTEWATER TREATMENT PLANT
PROJECT NO. 32-EE-05Y1-07
FORT LEWIS, WASHINGTON
29 NOVEMBER-7 DECEMBER 2006





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HPPM FORM 433-E (MCHB-CS-IPD), OCT 03

The U.S. Army Center for Health Promotion and Preventive Medicine (USACHPPM) lineage can be traced back over 50 years to the Army Industrial Hygiene Laboratory. That organization was established at the beginning of World War II and was under the direct jurisdiction of The Army Surgeon General. It was originally located at the Johns Hopkins School of Hygiene and Public Health, with a staff of three and an annual budget not to exceed \$3000. Its mission was to conduct occupational health surveys of Army operated industrial plants, arsenals, and depots. These surveys were aimed at identifying and eliminating occupational health hazards within the Department of Defense's (DOD) industrial production base and proved to be beneficial to the Nation's war effort.

Until 1995, it was nationally and internationally known as the U.S. Army Environmental Hygiene Agency or AEHA. Its mission is expanding to support the worldwide preventive medicine programs of the Army, DOD and other Federal Agencies through consultations/ supportive services; investigations and training.

Today, AEHA is redesignated the U.S. Army Center for Health Promotion and Preventive Medicine. Its mission for the future is to provide worldwide technical support for implementing preventive medicine, public health and health promotion/wellness services into all aspects of America's Army and the Army Community anticipating and rapidly responding to operational needs and adaptable to a changing work environment.

The professional disciplines represented at the Center include chemists, physicists, engineers, physicians, optometrists, audiologists, nurses, industrial hygienists, toxicologists, entomologists, and many other as well as sub-specialties within these professions.

The organization's quest has always been one of excellence and continuous quality improvement; and today its vision, to be the nationally recognized Center for Health Promotion and Preventive Medicine, is clearer than ever. To achieve that end, it holds ever fast to its values which are steeped in its rich heritage:

- ♦ Integrity is the foundation
- ♦ Excellence is the standard
- ♦ Customer satisfaction is the focus
- Its people are the most valued resource
- ♦ Continuous quality improvement is its pathway

The organization, which stands on the threshold of even greater challenges and responsibilities, has General Officer leadership. As it moves into the next century, new programs are being added related to health promotion/wellness, soldier fitness and disease surveillance. As always, its mission focus is centered upon the Army Imperatives so that we are trained and ready to enhance the Army's readiness for war and operations other than war.

It is an organization fiercely proud of its history, yet equally excited about the future. It is destined to continue its development as a world-class organization with expanded services to the Army, DOD, other Federal Agencies, the Nation and the World Community.

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### DEPARTMENT OF THE ARMY US ARMY CENTER FOR HEALTH PROMOTION AND PREVENTIVE MEDICINE 5158 BLACKHAWK ROAD ABERDEEN PROVING GROUND MD 21010-5403

# EXECUTIVE SUMMARY WASTEWATER TREATMENT PLANT PERFORMANCE EVALUATION SOLO POINT WASTEWATER TREATMENT PLANT PROJECT NO. 32-EE-05Y1-07 FORT LEWIS, WASHINGTON 29 NOVEMBER-7 DECEMBER 2006

1. PURPOSE. Evaluate the performance of the Solo Point wastewater treatment plant (WWTP) and verify compliance.

#### 2. CONCLUSIONS

- a. Data collected during the WWTP evaluation verified the following:
  - 1) The WWTP effluent was in compliance with permit effluent limits.
- 2) The WWTP unit process removal efficiencies (for BOD and TSS) were within acceptable ranges.
- b. Based on a review of WWTP records (2004 to 2006), the WWTP was operated in compliance with permit effluent limitations, with one exception, when treatment was inhibited by an unknown pollutant in May 2006. Treatment in one of the two trickling filters was upset and effluent pH levels were below the lower effluent limit for six days.
- c. Several pollutants that are typically associated with "non-domestic discharges" were detected in WWTP samples. These included total petroleum hydrocarbons (TPH), and ten metals and eighteen organic compounds listed as toxic pollutants (per 40 CFR 122, Appendix D, Tables II and III).
- 1) TPH was detected in influent, effluent and sludge grab samples. The WWTP removed approximately 79 percent of influent TPH, some of which accumulated in the sludge with solids. The discharge permit requires TPH monitoring, but does not limit it. Available TPH data from Fort Lewis and this evaluation indicate that some components of influent TPH persist through the anaerobic digestion and composting processes. Biosolids management regulations (i.e., WAC 173-308) do not address TPH concentrations in biosolids.
- 2) Detected non-domestic pollutants will be identified as pretreatment pollutants of concern (POCs) and will be further evaluated as part of an initial pretreatment evaluation.

- d. The Fort Lewis WWTP has the ability to produce biosolids that can meet the Class B biosolids criteria (i.e., pollutant ceiling concentrations and pathogen and vector attraction reduction), of WAC 173-308 (Biosolids Management).
- e. A review of WWTP operating conditions and discussions with WWTP operators identified concerns related to treatment process equipment and operations. See the report conclusions for specifics.
- f. The WWTP was staffed with only five operators and one lab technician, who covered day, night, and swing shifts for 24-hours per day, seven days per week. Operators were required to perform lab work in the absence of the lab technician and to work over-time to cover routine operations.
- g. Per Washington Administrative Code (WAC) 173-230, the "operator in responsible charge" is defined as "the individual who is routinely on-site and in direct charge." A Class III WWTP requires a Group III (or higher) "operator in responsible charge" with at least a Group II "operator in charge of each shift." While the USEPA issued permit does not specify requirements for certification of operators, Army Regulation 420-49 (Facility Engineering Utility Services) states (in paragraph 2-4) that "utility plant operators... will meet applicable ... State... certification requirements for the State in which they are located." The WWTP supervisor was not routinely on site and did not have a Group III license.

#### 3. RECOMMENDATIONS.

- a. Initiate a pretreatment program to: 1) verify the presence/absence of non-domestic pollutants identified in this evaluation, 2) identify pollutants of concern (POCs) and discharges that may interfere with the operation of a WWTP, pass through the WWTP, or interfere with sludge management (digestion, use, or disposal), 3) trace POCs (e.g., TPH, metals, toxic organic compounds) back to discharge source areas in the collection system and 4) provide a mechanism to enforce limits on dischargers of POCs.
- b. Investigate alternative regulatory criteria (e.g., TPH soil remediation action levels) for reuse of TPH-containing biosolids and pursue regulatory approval for land application or properly dispose of biosolids.
- c. Address treatment process equipment and operations concerns as outlined in the report conclusions.
  - d. Increase WWTP staff by one lab technician and at least one operator.
- e. The operator in responsible charge should be routinely on site and have a Group III WWTP operator license.

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# WASTEWATER TREATMENT PLANT PERFORMANCE EVALUATION SOLO POINT WASTEWATER TREATMENT PLANT PROJECT NO. 32-EE-05Y1-07 FORT LEWIS, WASHINGTON 29 NOVEMBER-7 DECEMBER 2006

- 1. PURPOSE. Evaluate the performance of the Solo Point wastewater treatment plant (WWTP) and verify compliance.
- 2. AUTHORITY. Proposal, Fort Lewis Wastewater Management and Pretreatment Evaluation, accepted by Mr. Phillip Crawford, Fort Lewis Environmental Office, September 2006.
- 3. EVALUATION APPROACH.
  - a. Document the WWTP operating conditions.
  - b. Conduct a sampling-based performance evaluation to include the following:
- 1) Sample the WWTP influent and effluent and in/out of major unit processes for three consecutive 24-hour periods to determine pollutant removal efficiencies, and verify permit compliance.
- 2) Sample the supernatants from the sludge thickener, and primary and secondary anaerobic digesters to determine pollutant concentrations and mass loadings.
  - 3) Sample digester and drying bed sludge to determine pollutant concentrations.
- c. Evaluate existing WWTP data (from approximately January 2004 through September 2006) to summarize performance and compliance trends.
  - d. Provide recommendations for improved operation/treatment.

#### 4. WWTP DESCRIPTION

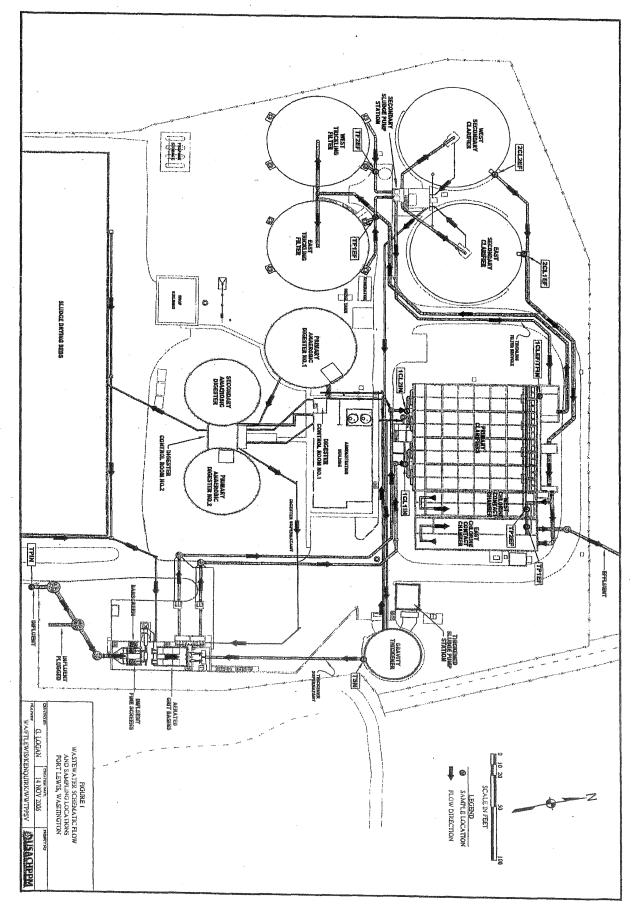
a. The Fort Lewis WWTP operates under National Pollutant Discharge Elimination System (NPDES) Permit No. WA-002195-4 (effective 1 February 2004 through 1 February 2009) issued by Region 10 of the United States Environmental Protection Agency (USEPA 2004). The permit establishes numeric effluent limits and non-numeric compliance requirements and conditions. Monthly numeric effluent limits include 30 mg/L biochemical oxygen demand (BOD) and 30 mg/L total suspended solids (TSS).

- b. Biosolids generated by the WWTP are regulated under a General Permit for Biosolids Management (No. BA-0021954) issued by the Washington Department of Ecology (WDOE 1998). The permit was administratively extended until issue of a new general biosolids permit (WDOE 2004).
- c. The Solo Point WWTP, constructed in 1955 for primary treatment and upgraded to provide secondary treatment in 1974, provides preliminary, primary, and secondary treatment of both domestic and industrial wastewater. The WWTP was upgraded in 2005. Improvements included new preliminary treatment processes (fine screens and grit removal), sludge pumps, scum pumps, waste gas burner sytem, propane storage, digester gas system, and boilers. WWTP effluent is discharged to the Puget Sound via a 500-foot pipe (with diffusers) that is approximately 70 feet deep. The WWTP receives wastewater from Fort Lewis, McChord Air Force Base, Camp Murray and a Veterans Hospital. The WWTP has a design average flow of 7.0 million gallons per day (mgd). Per WWTP records, actual flow rates averaged 3.4 mgd (based on 2004 through 2006 data). Figure 1 provides a schematic of the WWTP.

#### 5. OBSERVED WWTP OPERATING CONDITIONS

The following is a summary of unit processes and observed operating conditions.

- a. Preliminary Treatment. The preliminary treatment processes were upgraded in 2005.
- 1) Two parallel, mechanically cleaned, bar screens removed larger materials from influent wastewater and automatically deposited them in a dumpster via screw augers and conveyor belts. One screen was in operation; the other served as a backup, but was not operational. The repair required a hoist to lift the screen out of position. The screen had been out of service for approximately two years.
- 2) Two parallel aerated grit chambers removed grit to a dumpster for removal as solid waste. One grit chamber was in operation; the other served as a backup, but was not in operation because the upstream screen was not operational. Aeration of the grit chamber is necessary to prevent settling of lighter solids. After screening and grit removal, influent wastewater mixed with return flows from the sludge thickener and secondary digester before flowing into the primary clarifiers.
- b. Primary Clarification. Primary settling was achieved with up to four parallel, rectangular primary clarifiers. Three of the primary clarifiers were in use at the time of sampling; one was being renovated due to general deterioration and was out of service for five months, which included the wet season. The installation plans to renovate the other three as part of a \$1.2 million upgrade project. Flow entered through two pipes. The east pipe fed one clarifier and the west pipe fed the other two clarifiers. The wastewater entering through the east pipe was darker, presumably because it received a higher concentration of digester supernatant, which is returned upstream of the primary clarifiers. Primary sludge was mechanically collected by scrapers and continuously pumped from a collection pit to the sludge thickener. One of the two primary



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sludge pumps was not operational at the time of sampling, but was repaired shortly thereafter. The pumps were older (~1970s) constant speed pumps and lacked modern electronic controls. They were controlled by timers in the past to manage sludge pumping, but the timers are no longer operational.

#### c. Trickling Filters.

- 1) Secondary treatment was provided by two parallel, high rate rotary arm trickling filters. A portion of the trickling filter effluent was returned to a wet well at the end of the primary clarifiers where it mixed with primary clarifier effluent. Then one of three constant speed pumps returned the mixture to the influent of the trickling filters. The pumps were older (1970s) constant speed models and lacked modern electronic controls. Plant personnel estimated the pumping rate at approximately 7 mgd. No flow measurement was available on this pump or on the return line. A level sensor in the trickling filter feed wetwell controlled a throttling valve in the recirculation line to maintain a constant flow over the filters. Therefore, the recirculation ratio was increased as plant influent decreased and vice versa. The flow across the trickling filters remained constant, regardless of the influent flow rate. (Note: Variable speed pumps would allow treatment to be optimized with better control of trickling filter flow rates.) Prior to secondary clarification, a portion of the trickling filter effluent was pumped to the sludge thickener as "dilution water" to facilitate sludge settling.
  - 2) Broken plastic trickling filter media was observed on the top of the filters.
- d. Secondary Clarification. Secondary clarification was provided by two parallel, circular, center feed secondary clarifiers. Secondary sludge was pumped to the sludge thickener. The pumps were older (1970s) constant speed pumps and lacked modern electronic controls. Clarified effluent flowed to the chlorine contact chambers.

#### e. Disinfection.

- 1) Disinfection was performed in two parallel chlorine contact chambers (CCCs). An aqueous sodium hypochlorite solution was added to a mixing chamber at the head of the CCCs. An analyzer monitored the chlorine concentration in the mixing chamber. A software program (Wonderware<sup>TM</sup>) was linked to the analyzer and sodium hypochlorite metering pumps. It automatically adjusted the pump feed rate to maintain a pre-set chlorine concentration in the mixing chamber. WWTP personnel indicated that they were planning to replace the chlorine feed metering pumps and chlorine probe analyzers because the technology has advanced and more reliable equipment (low vibration pumps and direct read analyzers) is available. Personnel also indicated that the existing chlorine feed system had not been calibrated within the last two years.
- 2) Sodium thiosulfate was used for dechlorination. It was added to the discharge from the CCCs to reduce the effluent total residual chlorine (TRC) concentration below 0.5 mg/L (permit limit). An analyzer monitored the chlorine concentration after sodium thiosulfate addition. A software program (Wonderware<sup>TM</sup>) was linked to the analyzer and sodium

thiosulfate metering pumps. It automatically adjusted the feed rate to maintain compliance with the residual chlorine permit limit.

- f. Grease Collection. Grease and scum skimmed from the clarifiers and CCCs were pumped to a rectangular grease vault. Once per week, the grease was pumped to a grease concentrator and then deposited in a dumpster. The grease was further dewatered in a dedicated drying bed before disposal as solid waste.
  - g. Sludge Management.
    - 1) Sludge Thickener.
- a) A circular (45-ft diameter) sludge thickener was used to increase the solids content of primary and secondary sludge before it was sent to the digesters. Dilution water from the trickling filter effluent was added to the thickener to maintain aerobic conditions.
- b) Approximately 16,000 gpd of thickened sludge was pumped from the thickener to the primary digester. The thickener produced sludge with a total solids concentration of 3.1 percent with a total volatile solids component of 82 percent, based on 2006 WWTP data. Supernatant was returned to the primary clarifier influent.

#### 2) Sludge Digesters.

- a) Sludge was digested in a two-stage anaerobic process consisting of one or two mixed, heated primary digesters followed by one unheated secondary digester. Only one primary digester was in service at the time of sampling. The other digester was out of service for cleaning and maintenance. Approximately 16,000 gal/day of raw sludge was pumped to the 460,000 gallon primary digester. The primary digester provided approximately 29 days of residence time. In 2006, the primary digester was heated to a minimum temperature of 35 °C (95 F). This combination of time and temperature meets the Class B biosolids pathogen reduction requirements of WAC 173-308-170, which requires values for the mean cell residence time and temperature to be between fifteen days at 35 to 55 °C and sixty days at 20 °C. When in service, the other primary digester (800,000 gallons) would provide 50 days of residence time. The secondary digester (460,000 gals) provided approximately 29 days of residence time. In 2006, the secondary digester temperature was a minimum of 29 °C. Supernatant from the secondary digester was returned by gravity to the head of the plant. The supernatant was very dark and thick with solids, which is typical when there is incomplete digestion in the primary digester. This generates gases in the secondary digester and causes floating solids and fine sized solids that have poor settling characteristics.
- b) The digesters were heated with methane gas, a natural by-product of the digestion process. Excess methane gas was burned off in a flare. Propane was also available as a backup heat source.

- c) Cracks and evidence of leaking gas (i.e., bubbles when wet) were observed in the cover/roof of primary digester No. 2. Leaking gas may contribute to air emissions, inefficient operation and unsafe working conditions.
- 3) Biosolids Drying Beds. A total of 24 biosolids drying beds were available. The beds had an asphalt base with no sand layer or underdrains; drying was by evaporation only, and resulted in inadequate drying during the wet season. Installation personnel indicated that valves feeding digester biosolids to drying beds were not water tight. When attempting to feed biosolids to one drying bed, biosolids leaked through valves to other beds. A roof was in place over the entire biosolids drying bed area to prevent precipitation from contacting the drying biosolids. A project was approved to replace the deteriorated roof covering. The WWTP treats and processes approximately 120 dry tons of biosolids annually (based on 2004 and 2005 data).
  - 4) Biosolids Composting, Beneficial Reuse, and Disposal.
- a) After drying, the biosolids were typically composted to Class A standards at Fort Lewis' Sequalitchew Creek Eco-Park and Earth Works or hauled off-site by a licensed biosolids handler to a permitted beneficial use facility (Fire Mountain Farms, Inc.). That facility applied the biosolids at two sites in Lewis County, WA (Burnt Ridge Ranch and Lincolm Creek Unit).
- b) Recent concerns about the petroleum hydrocarbon content of the biosolids resulted in the temporary landfill disposal of biosolids. Composting of the biosolids in a covered and contained area (i.e., runoff from the area drains to the WWTP) would eliminate concerns about potential total petroleum hydrocarbon (TPH) runoff during composting.
- c) The installation was planning to modify the on-site biosolids drying bed facility to incorporate improved biosolids dewatering (e.g., belt filter press, solid-bowl centrifuge) and on-site composting under the existing roof. Mechanical dewatering prior to composting could produce cake solids concentrations of 18-35 percent and reduce the requirements for supplemental bulking agents (e.g., wood chips) or amendments during composting. A filter press or centrifuge would require a small footprint and could readily reduce moisture content to desired levels for composting; however, these processes would require shelter and additional manpower to operate and maintain.
  - h. Flow Measurement and Automatic Sampling.
- 1) Effluent flow (which also approximates influent flow) was measured with ultrasonic sensors and flow meters at the effluent weirs of the chlorine contact chambers. The influent flow to the primary clarifiers was also measured with two in-line magnetic flow meters. The primary clarifier influent flow includes WWTP influent flow, sludge thickener supernatant, anaerobic digester supernatant, drying bed drainage, and storm water inflow from portions of the WWTP. WWTP personnel indicated that the magnetic flow meters had not been calibrated since they were installed in 2005. Flow rates were not recorded for primary sludge pumping, trickling filter influent, trickling filter recycle, secondary sludge pumping, thickener supernatant, and digester supernatant.

2) Automatic samplers were programmed to collect modified time composite samples, where samples were collected less frequently during typical low flow periods (e.g., at night). The NPDES permit requires samples to be representative of the "volume and nature" of the monitored discharge. Although a modified time composite may be representative of the volume during dry periods, it would not be representative during and after precipitation events when the sanitary sewer is subject to infiltration and inflow.

#### 6. STAFFING EVALUATION.

- a. At the time of the evaluation, five personnel operated the WWTP and another served primarily as a lab technician. One operator had recently retired and another was re-assigned to sewer maintenance. The low staffing levels required personnel to work significant overtime to cover routine operations. Operators were often required to perform lab tests in addition to their normal operator responsibilities. One additional operator and one additional lab technician would relieve the overtime burden on the existing staff. The WWTP supervisor did not serve as an "active operator," because he had other supervisory responsibilities.
- b. Together, the five operators and lab technician possessed two Group II, three Group III, and one Group IV license. Per Washington Administrative Code (WAC) 173-230, the WWTP is a Class III plant (secondary treatment WWTP, with a design flow between 1 and 10 MGD, WAC 173-230). The code further states that the "operator in responsible charge" must be certified at a level that is equal to or greater than the level of the plant. The "operator in responsible charge" is defined as "the individual who is routinely on-site and in direct charge." A Class III WWTP requires a Group II (or higher) "operator in responsible charge," with at least a Group II "operator in charge of each shift." While the USEPA issued permit does not specify requirements for certification of operators, Army Regulation 420-49 (Facility Engineering Utility Services) states (in paragraph 2-4) that "utility plant operators... will meet applicable ... State... certification requirements for the State in which they are located"; therefore, Fort Lewis should comply with the requirements of WAC 173-230.

#### 7. PERFORMANCE EVALUATION

a. Sampling. During three 24-hour periods beginning at 0700 hours on 4 December 2006 and ending at 0700 hours on 7 December 2006, samples were collected from locations throughout the WWTP, as outlined in Table 1 and in accordance with procedures described in the WWTP Performance Evaluation Work Plan (USACHPPM 2006). The sample locations are shown on Figure 1.

#### b. Flow Measurements.

1) Flow rates corresponding to sampling locations were measured, if possible, or calculated/estimated based on available information. WWTP influent and effluent flow rates were measured with flow measuring devices as described in Table 1 and are summarized in Table 2. The average of these flow rates was 31% lower than Solo Point WWTP average effluent flow data for the same time period.

#### Keport No. 32-EE-05Y1-07, 29 November – 7 December 2006

Table 1. Sample Summary

Sample Location	Sample. ID	-Sample Type	Sampling Frequency	Analytes of the second	Comments
Wastewater Treatment Plant (WWTP) Influent	TPIN	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	Biochemical oxygen demand (BOD), TPH (diesel, lube oil, gasoline) (grab), Grease and Oil (grab), Ammonia Nitrogen, Nitrite/Nitrate-Nitrogen (NO <sub>2</sub> /NO <sub>3</sub> -N), Total Kjeldhal Nitrogen (TKN), Phosphate, Total Suspended Solids (TSS), Volatile Organic compounds (VOCs), Semi-Volatile Organics (SVOCs), Organochlorine Pesticides/PCBs, Organophosphorus Pesticides, Total Metals (Aluminum, Arsenic, Cadmium, Chromium, Copper, Iron, Lead, Mercury, Molybdenum, Nickel, Selenium, Silver, Zinc), Phenol	Flow composite samples were collected from a manhole with access to the WWTP influent pipeline. Flow was measured with an area/velocity probe and flow meter. This manhole was located outside of the WWTP fence line along Solo Point Road.
Primary Clarifier(s) Influent	1CLIN	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	BOD, TPH (diesel and lube oil) (grab), Grease and Oil (grab), Ammonia Nitrogen, NO <sub>2</sub> /NO <sub>3</sub> -N, TKN, Phosphate, TSS, Total Metals	Flow through two pipes was measured with two area/velocity probes and two flow meters. Flow composite samples were collected from the two influent channels and manually combined based on flow ratios.
Primary Clarifier(s) Effluent	1CLEF	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	Same as above.	Flow composite samples were collected from the channel that receives primary clarifier effluent from three operational clarifiers. The sampler was flow-paced via connection to a WWTP effluent flow meter.
Trickling Filter Influent	TFIN	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	Same as above.	The primary clarifier effluent was considered as the trickling filter influent. A portion of the trickling filter effluent is continuously returned (recycled) to the trickling filter; therefore, we neglected the recycle stream and evaluated the trickling filter(s) performance based on the difference in pollutant mass exiting the primary clarifiers and the mass entering the secondary clarifiers.
East Trickling Filter Effluent	TFIEF	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	Same as above.	Flow was assumed to be one-half of the primary clarifier influent/effluent flow. Flow composite samples were collected from an under-drain. The sampler was flow-paced via connection to a primary clarifier influent flow meter. Effluent samples from each trickling filter were collected to evaluate the performance of each filter, as one filter was recently "out of service" and restarted.
West Trickling Filter Effluent	TF2EF	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	Same as above.	Same as above.

Table 1. Sample Summary (continued)

Sample		Sample Type	Sampling	Analytes " " To see Light 2.8	Comments
Secondary Clarifier Influent/ Combined Trickling Filter Effluent	2CLIN	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	BOD, TPH (diesel and lube oil) (grab), Grease and Oil (grab), Ammonia Nitrogen, NO <sub>2</sub> /NO <sub>3</sub> -N, TKN, Phosphate, TSS, Total Metals	Flow composite samples were collected in the junction box that receives and mixes flow from the two trickling filters and feeds the two secondary clarifiers. Trickling filter recycle wastewater was also drawn from this junction box. The sampler was flow-paced via connection to one of the primary clarifier influent flow meters.
Secondary Clarifier Effluent	2CLEF	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	Same as above.	Flow composite samples [2CL1EF and 2CL2EF) were collected from each clarifier effluent drain. The samplers were flow-paced via connection to an effluent flow meter. Equal amounts of each sample were combined to form a composite sample.
Combined WWTP Effluent	TPEF	24-Hour Flow Composites and Grabs	Three consecutive 24-hour periods	BOD, TPH (diesel, lube oil, gasoline) (grab), Grease and Oil (grab), Ammonia Nitrogen, NO <sub>2</sub> /NO <sub>3</sub> ·N, TKN, Phosphate, TSS, VOCs, SVOCs, Organochlorine Pesticides/PCBs, Organophosphorus Pesticides, Total Metals, hardness, Phenol (grab)	Samples were collected from the effluent end of each CCC. Flows were measured with the existing weirs and bubbler transducers and flow meters. The two effluent samples were manually combined based on flow ratios.
Sludge Thickener Supernatant	TSN	24-Hour Time Composites and Grabs	Three consecutive 24-hour periods	BOD, TPH (diesel and lube oil) (grab), Grease and Oil (grab), Ammonia Nitrogen, NO <sub>2</sub> /NO <sub>3</sub> -N, TKN, Phosphate, TSS, Total Metals	Samples were collected from the thickener effluent channel
Primary Digester Supernatant	1DSN	Grab	Once	BOD, TPH (diesel and lube oil) (grab), Grease and Oil, Ammonia Nitrogen, NO <sub>2</sub> /NO <sub>3</sub> -N, TKN, Phosphate, TSS, Total Metals	The sample was collected from the digester supernatant discharge (located on top of the digester)
Secondary Digester Supernatant	2DSN	Grab	Once	Same as above.	The sample was collected from the digester supernatant discharge (located on top of the digester)
Thickener Sludge	TSL	Wet Sludge Grab	Опсе	Total Solids (% of wet), Total Volatile Solids (% of dry), TPH (diesel and lube oil), Metals	The sample was collected from a sampling spigot in the thickener piping room.
Primary Digester Sludge	1DSL	Wet Sludge Grab	Once	Same as above.	The sample was collected from a sampling spigot in the digester piping room.
Secondary Digester Sludge	2DSL	Wet Sludge Grab	Once	Same as above.	The sample was collected from a sampling spigot in the digester piping room or from sludge being poured to a drying bed.
Drying Bed Sludge	DRYSL	Composite	Once	Same as above.	The sample was collected from the drying bed sludge in the north-east corner. WWTP personnel indicated the bed had been poured approximately 6 months prior.

2) The flow rates of individual "return flows" (e.g., primary clarifier sludge, secondary clarifier sludge and dilution water for the sludge thickener) were approximated by drawing down the level in the sludge thickener and filling it with a known volume during a known period of time. This procedure was performed using individual pumps and the combination of pumps operated during sampling. These approximate flow rates are presented in Table 3.

Table 2. Influent and Effluent Flow Rate Measurements

Date	Time	. WWTP Influent*	WWTPEffluent*	Average of Influent/Effluent Flow/Rates
4 - 5 Dec 06	0700 - 0700	2.52	2.37	2.45
5 – 6 Dec 06	0700 - 0700	2.54	2.37	2.46
6 – 7 Dec 06	0700 - 0700	2.08	3.10	2.59
Average		2.38	2.61	2.50

<sup>\*</sup> Field flow measurements generally have  $\pm 10\%$  error. Temporary equipment problems resulted in segments of unusable data when flow measuring equipment was out of calibration. These segments were replaced with reliable data from another day with similar flow trends.

Table 3. Pump System Characteristics.

	The state of the s	Approximate flow rate during consument pumping*
Primary Clarifier Sludge Pump Aurora 663A SF, Size 4X4X9 Motor drive: 15 HP @ 1150 rpm Pump plate flow rating: 135 gpm @ 22 ft TDH	362 gpm	~293 gpm (0.422 mgd)
Secondary Sludge Pump: Weinman 4 inch Pump plate flow rating: 140 gpm @ 25 ft TDH	354 gpm	~287 gpm (0.413 mgd)
Dilution Pump: Weinman 4 inch 7.5 HP @ 1750 rpm Pump plate flow rating: 570 gpm @ 27 ft TDH	603 gpm	~488 gpm (0.703 mgd)
Total Measured Flow during concurrent pumping		~1068 gpm (~1.54 mgd)

<sup>\*</sup> Pumps discharge to a common discharge pipe prior to thickener discharge; assumes a common proportional flow reduction for each pump.

3) Influent to the primary clarifiers enters through two 24-inch pipes. Flow rates were measured with flow measuring devices as described in Table 1. The flow rates are summarized in Table 4. It should be noted that the average of these flow rates was 18% higher than Solo Point WWTP average primary clarifier influent flow data for the same time period. An attempt to "balance" the field measured flows resulted in a discrepancy. The difference between influent/effluent average flow rates and primary clarifier influent flow rates should approximate the sum of the estimated flows from the pumps listed in Table 3. The data indicated an average discrepancy of 0.56 mgd. Factoring in a ±flow measurement error (i.e., 10% low on influent effluent flow and 10% high on primary clarifier influent) would reconcile the discrepancy. Rather than "alter" both sets of flow data, a decision was made to use the average of the influent and effluent flow rates as a basis for influent and effluent mass loading calculations, and to use

the approximate flow rates from Table 3 to calculate mass loadings through unit processes. A summary of inputs and outputs (including flow rates) to each unit process is provided in Table 5.

Table 4. Primary Clarifier Influent Flow Rate Measurements

Date	Time	Primary Clavifier Influent I* (East)	Primary Clarifier Influent 2* i(West)	Sum of Primary Clarifier Influent 1 and Influent 2 Plow Rates
		mgd	ingå	noga
4 - 5 Dec 06	0700 - 0700	1.24	3.41	4.65
5 - 6 Dec 06	0700 - 0700	1.23	3.30	4.53
6-7 Dec 06	0700 - 0700	1.29	3.35	4.64
Average		1.25	3.35	4.60

<sup>\*</sup>Field flow measurements generally have ±10% error.

Table 5. WWTP Unit Process Inputs and Outputs.

	inpils 1	CH_Unit Processes	Outpuis
	WWTP influent (~2.50 mgd) ► Sludge Thickener supernatant (~1.54 mgd) ► Secondary Anaerobic Digester supernatant (~0.016 mgd) ►	Headworks/Preliminary Treatment (Screening and Grit Removal)	<ul> <li>▶ Headworks effluent (~4.04 mgd)</li> <li>▶ Screenings</li> <li>▶ Grit</li> </ul>
camen	Headworks effluent (~4.04 mgd) ▶	Primary Clarifiers	<ul> <li>▶ Primary Clarifier effluent (~3.62 mgd)</li> <li>▶ Primary Clarifier sludge (~0.42 mgd)</li> </ul>
ewater Trea	Primary Clarifier effluent (~3.62 mgd) ► Partial Trickling Filter effluent recycle (volume varies) ► Multi-Media Filter backwash ►	Trickling Filter	► Trickling Filter effluent (~3.62 mgd)
Wast	Trickling Filter effluent minus dilution water (pumped continuously to sludge thickener at ~0.70 mgd) and partial Trickling Filter recycle flow (volume varies) = ~2.92 mgd ▶	Secondary Clarifiers	➤ Secondary Clarifier effluent (~2.50 mgd)  ➤ Secondary Clarifier sludge (pumped to Sludge Thickener at ~0.42 mgd)
	Secondary Clarifier effluent (~2.50 mgd) ▶ Chlorine ▶ Dechlorinating Agent ▶	Chlorine Contact Chambers	▶ WWTP effluent (~2.50 mgd)
Shidge Managerhent	Primary Clarifier sludge ► Secondary Clarifier sludge ► Dilution water (from Trickling Filter effluent at 0.70 mgd)) ►	Sludge Thickener	<ul> <li>▶ Thickened sludge (to anaerobic digesters at ~ 0.016 mgd)</li> <li>▶ Sludge Thickener supernatant (to Headworks at ~1.54 mgd)</li> </ul>
N (Ma)	Thickened sludge (~0.016 mgd) ▶	Anaerobic Digesters	<ul> <li>▶ Supernatant (returned to Headworks at ~ 0.016 mgd)</li> <li>▶ Digested sludge (to drying beds)</li> </ul>

#### c. Wastewater Sampling Results.

- 1) A summary of detected parameters for each wastewater sample is provided in Appendix B, Table B-1. A summary of parameters detected in WWTP influent, primary clarifier influent (i.e., WWTP influent + recycle flows from WWTP processes), and effluent samples is provided in Table 6. Effluent concentrations were compared to applicable Washington marine surface water toxic substance criteria for the protection of aquatic life [WAC 173-201A, Table 240(3)] (see Appendic C). It should be noted that the Washington toxic substance criteria apply to the receiving water, not the WWTP discharge; however, the criteria were compared to effluent concentrations to screen for pollutants that have potential to impact receiving waters.
- 2) In addition to conventional wastewater pollutants (e.g., BOD<sub>5</sub>, TSS, ammonia) influent and effluent samples were analyzed for toxic metals [from 40 CFR 122, Appendix D, Table III with Washington surface water criteria per WAC 173-201A, Table 240(3)], TPH, and toxic organic pollutants (VOCs, SVOCs, and pesticides/PCBs per 40 CFR 122, Appendix D, Table II) to provide data to support a planned pretreatment program. Additional pretreatment sampling will be conducted in May 2007 as part of an initial pretreatment evaluation and the detected toxic metals and organic compounds will undergo further analysis as pretreatment pollutants of concern.
- a) TPH was detected in influent and effluent samples (see Table 6). Effluent grab sample TPH concentrations ranged from 2.3 to 10.9 mg/L. The discharge permit requires TPH monitoring, but does not include a concentration or mass limit. Washington does not have a surface water quality criteria for TPH.
- b) Ten metals and eighteen organic compounds listed as toxic pollutants (per 40 CFR 122, Appendix D, Tables II and III) were detected in WWTP influent and/or primary clarifier influent samples. Five of the metals (arsenic, copper, lead, nickel, and zinc) were detected in WWTP effluent samples. Only copper was detected in effluent samples at concentrations that exceeded the Washington marine surface water toxic substance criteria for the protection of aquatic life. Four of the organic compounds [chloroform, bis (2-ethylhexyl) phthalate, naphthalene, and alpha chlordane] were detected in WWTP effluent samples at trace concentrations. Only alpha chlordane was detected (at estimated trace concentrations) in effluent samples above Washington marine surface water toxic substance criteria for the protection of aquatic life.

Table 6. Parameters Detected in WWTP Influent and/or Effluent Samples.

		1.79	Principle of the second	10 Co	Primary	400		
	Analyte	Date	Time	- WWTP	«Clarifier	WWTP.	Comments	
		1,350		Influent	Influent	Bffluent -		
	Rogins III.	- 1. VII. 45/074. )	Wall of Branch	<b>建四级分析的数</b> 2	48-11-66		生物 人名英格兰 医克里克斯氏 医克里克氏 医克里克氏	
				)	1		Effluent sample concentrations were	
BC	D (mg/L)	4-5 Dec 06	0700-0700	78	61	9.3	below permit limit (30 mg/L). Day	
100		.					two and three data discarded due to	·
	No de la Mina de la Mi	7 67 4 7 72 4 42 4	THE PERSON NAMED IN COLUMN	no stoke engline en la produce	7.78	San Francisco	lab QA/QC findings	
11. 化酸物	767			43/43/21/1900				
	<b>建</b>	4-5 Dec 06	0700-0700	54	228	20	Effluent sample concentrations were	
3,41	SS.(mg/L)	5-6 Dec 06	0700-0700	98	220	24.7	below effluent limit (30 mg/L).	
14.74	.0.4	6-7 Dec 06	0700-0700	204	178/220	26.4		
- 14/2		1.544 1550				7 2 M 1 2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		
		4-5 Dec 06	0700-0700	24	21	3.5	No permit limit, but monitoring	
Amn	nonia (mg/L)	5-6 Dec 06	0700-0700	25	23	4.5	required. Effluent sample concs.	
	witte (IIIB) C)	( 7 D 06	0700 0700		04/07	<i>c</i> 0	above WA TSC: Acute = 0.233	
(c)		6-7 Dec 06	0700-0700	26	24/26	5.8	mg/L, Chronic = 0.035 mg/L	
12.00	entral de la lati	35.00 (100 pm		Digwill the	7. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	TO THE WAY TO STATE		
	<b>%</b> (3)	4-5 Dec 06	0700-0700	ND (<0.050)	1.3	20	No permit limit, but monitoring	
Nitrate	Nitate (mg/L)	5-6 Dec 06	0700-0700	ND (<0.050)	3.5	21	required.	
1	医精制 法不行	6-7 Dec 06	0700-0700	ND (<0.050)	4/3.6	24	No WA TSC.	
2.30	Table 1881 118	TO COME SA				100		
15.00	E PANESSA STATE	4-5 Dec 06	0700-0700	29	33	6.7	No permit limit, but monitoring	
T Tr	CN (mg/L)	5-6 Dec 06	0700-0700	37	38	8,1	required.	
		6-7 Dec 06	0700-0700	39.	39/38	8.8	No WA TSC.	
	3000 je iz r	6-7 Dec 06	0700-0700	39	39/38	0,0 	No wa ise.	
19364 Q.4856"A	MEMORRAL SERVICE OF THE	4-5 Dec 06	Second to the last second second		The Art of	Charles and Constitution of the Constitution o	No permit limit; monitoring not	
Toja	li Phosphorus	-	0700-0700	3.61	6.17	3.72		
	(mg/L)	5-6 Dec 06		4.2	6.25	4.34	required. No WA TSC.	
The said of the said of the	and the second s	6-7 Dec 06	0700-0700	4.8	6.25/6.3	4.54	1	
Acres Manager			Service State	appropriate the second	The state of the s			
Oil	and Grease	4-Dec 06	grab	21	26	ND (<5.30)	No permit limit; monitoring not	•
	(mg/L)	5-Dec 06	grab	7.79	7.33	ND (<5.00)	required.	
4.1	Property Commencer	6-Dec 06	grab	6.33	6.56	ND (<5.10)	No WA TSC.	
	THE TANK	7.14.0				ALC: Tong		-
	-Diesel Range	4-Dec 06	grab	15	53	0.690J	No permit limit, but TPH monitoring	
	(mg/L)	5-Dec 06	grab	12	14	0.830	required.	
er a serie		6-Dec 06	grab	18	13	4	No WA TSC.	
	286. cm		2 (1) (1) (2)	Barrier Market	100	4,047	Market and the second second second	
7 P. 18	Heavy Range	4-Dec 06	grab	11	27J	1,6J	No permit limit, but TPH monitoring	
		5-Dec 06	grab	7.2J	11	1.6	required.	
P. 计模块数	(mg/L)	6-Dec 06	grab	11J	13J	6.9	No WA TSC.	
21.38		77.74E4786	Vi. 34. 175.18					
		4-Dec 06	grab	0.280	NA	ND(<0.048)	No permit limit, but TPH monitoring	
T. A.	H-Gasoline	5-Dec 06	grab	0.140J	NA	ND(<0.048)	required.	
图 温量	(mg/L)	6-Dec 06	grab	0.150J	· NA	ND(<0.048)	No WA TSC.	
21.19.2		N. S. C. AU	11/2 12/4	0.1503				
170.4	250 (4) (4)	4-5 Dec 06	0700-0700	0.208	1.34	0.243	No permit limit.	330 mgl
	ninum (mg/L)	5-6 Dec 06	0700-0700	0.208		0.243	No WA TSC.	33010
		6-7 Dec 06		-	1.46	the same of the sa	THO WALLDON	
7.4(1-0.9)	AND SECTION	CONTRACTOR SOFT	0700-0700	0.547	1.36	0.246	And the second s	
	Marian.		9000 0000			2 (1		0
TO THE PROPERTY.	THE PARTY OF THE P	4-5 Dec 06	0700-0700	ND(<1.00)	1.49	1.03-	No permit limit.	1,3 M912
	senio (µg/L)	5-6 Dec 06	0700-0700	1.15	1.74	1.17	Detected below the WA TSC.	1 . 3
	10000	6-7 Dec 06	0700-0700	ND(<2.00)	ND(<2.00)	ND(<2.00)		1
100					1.0			,
		4-5 Dec 06	0700-0700	ND(<2.00)	ND(<2.00)	ND(<2.00)	No permit limit.	14.00.0
	imium (µg/L)	5-6 Dec 06	0700-0700	ND(<2.00)	ND(<2.00)	ND(<2.00)	Detected below the WA TSC.	100
图 流程		6-7 Dec 06	0700-0700	1.06	1.39	ND(<1.00)		
	AVAK HANDE	1276	18. 18. 18.	0.30	Harris and			
		4-5 Dec 06	0700-0700		2.71	ND(<2.00)	No permit limit, but monitoring	1. 6.5
13/20/ 3/27/2005	omium (μg/L)	5-6 Dec 06	0700-0700		2.63	ND(<2.00)	required.	1.3 mg/l we 6.0
Chr	CHARLEST A LEAD TO A							

<sup>1</sup> Primary Clarifier Influent = WWTP Influent + WWTP recycle flows
J: estimated value ND: not detected WA TSC: Washington marine surface water toxic substance criteria for the protection of aquatic life.

Example: (<5.00) = the analyte was not detected above the 5.00 mg/L reporting limit

Table 6. Parameters Detected in WWTP Influent and/or Effluent Samples (continued).

	Analyte	Date	Time	WWTP Influent //	Primary Clarifler Influent	WWTP Effluent	<sub>ri</sub> Comments	1
4,13	44	4-5 Dec 06	0700-0700	45.8	100	32.7	No permit limit, but monitoring	so wel
	Coppen(µg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	51.3 78.5	108	36.7	required.  Detected in effluent samples above the WA TSC: Acute = 4.8 µg/L,  Chronic = 3.1 µg/L	M.B. usl
	a de la como				112 3 4 1 1 1 1 1 1	1450 Sec. 2 (1834)		
		4-5 Dec 06	0700-0700	1.28	6.08	3.37	No permit limit, but monitoring	1.3 v3/l
3	Lead (Lig/L)	5-6 Dec 06	0700-0700	1.22 .	5.26	1.05	required.	11200
		6-7 Dec 06	0700-0700	ND(<5.00)	6.67	ND(<5.00)	Detected in influent/effluent samples below the WA TSC.	
			Transfer of		14 S. C. C.			
		4-5 Dec 06	0700-0700	ND(<0.200)	0.278	ND(<0.200)	No permit limit, but monitoring	
1	A MARKET	5-6 Dec 06	0700-0700	ND(<0.200)	0.699	ND(<0.200)	required.	0.1 43/
	Mercury (µg/L)	6-7 Dec 06	0700-0700	0.297	0.527	ND(<0.200)	Not detected in effluent samples at the MRL (0.200 µg/L); MRL was below acute but above the chronic criteria. WA TSC: Acute = 4.8 µg/L, Chronic = 3.1 µg/L	
13	race and the second		10 1	13400	1000	100		
	Maria de la companya	4-5 Dec 06	0700-0700	12.4	11.7	5.67	No permit limit, but monitoring	Mer in promit
7	Molybdenigm (µg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	11.1 23.3	11.2	9.91	required. No WA TSC.	Brawn I
	To the second	0-7 Dec 00	0700-0700 24782455344		17.2	10.6		
	all a second	4-5 Dec 06	0700-0700	11.2	4.49	2.45	No permit limit.	143
	片Nickel (真g/L) 。ti	5-6 Dec 06	0700-0700	6.93·	3.79	2.64	Effluent sample concs. below WA	0- 4
1		6-7 Dec 06	0700-0700	6.56	3.71	ND(<2.00)	TSC. Maritanas regulary	
		4 6 D 06	0200 0200	Maria (190)	4	ND(<1.00)	No permit limit, but monitoring	
		4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<1.00) ND(<1.00)	1.15	ND(<1.00) ND(<1.00)	required.	0.65
2. C. X. Y	'Yelenium((ug/L)	6-7 Dec 06	0700-0700	ND(<2,00)	ND(<2.00)	ND(<2.00)	All sample concs. below the WA TSC.	0,00
158	AMERICAN STREET	1. T. C. S. S. C. S.	State Top (Lugarde	X		restriction to	Not detected in effluent samples.	
		4-5 Dec 06	0700-0700	ND(<1.00)	1.26	ND(<1.00)	No permit limit.	33.2
No.	Silver (µg/L)	5-6 Dec 06	0700-0700	ND(<1.00)	1.19	ND(<1.00)	All sample cones, below the WA	(5)
		6-7 Dec 06	0700-0700	ND(<1.00)	1.02	ND(<1.00)	TSC.	,
4		12.6				2070	Detailed to the second	. 6
	Zinc (ibg/L)	4-5 Dec 06 5-6 Dec 06	0700-0700	0.08	0.243	0.070	All sample concentrations were below the WA TSC.	33.2
	Constituent)	6-7 Dec 06	0700-0700	0.093	0.237	0.079	11/2 100.	
	7							
		4-Dec	grab	ND	NA	ND	No permit limit.	1
1	Chloroform (µg/L)	5-Dec	grab	ND	NA	ND	No WA TSC.	X
		6-Dec	grab	ND	NA	1J	J estimated	γ /
		4-Dec	grab	2J	NA	ND	No permit limit.	
	1 4-dichlorobenzene	5-Dec	grab	3J	NA.	ND	No WA TSC.	
ľ	(Upl)	6-Dec	grab	2J	NA :	ND		,
		LEGISLAN.					OF STATES	
	1,2-diohlorobenzene	4-Dec	grab	2J	NA	ND	No permit limit.	
	(PE/P)	J. Der	grab	11	NA	ND	No WA TSC.	
F		6-Dec	grab	4J	NA NA	ND		
+	59 New 7		grab	3J	NA	ND	No permit limit.	1
T.	Tetrachloroethene	5-Dec	grab	ND	NA	ND	No WA TSC.	
	(lg/L)	6-Dec	grab	ND	NA	ND	-	
		1, 1, 2, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1,	Visite 1				20. 精神的影响。20. All State (19. All St	
1	A CONTRACTOR	4-Dec	grab	2.J	NA	מא	No permit limit.	
1	Toluene (µg/L)	5-Dec	grab	2J	NA	ND	No WA TSC.	,
-1.5		6-Dec	grab	3J	NA	ND		i

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Table 6. Parameters Detected in WWTP Influent and/or Effluent Samples (continued).

			intidone and/o	1 Dilluciii i	Jumpies (co	initioa).
	142.4			Primary		
Analyte	: Date	Time 1	WWIP	Clarifier	WWTP:	Comments
		<b>建筑的电影</b>	Influent	Influent <sup>1</sup>	Effluent .	
11112375	4-5 Dec 06	0700-0700	6	NA	∙ND	No permit limit.
≠ a Rhenol	5-6 Dec 06	0700-0700	24	NA NA	ND	No WA TSC.
	6-7 Dec 06	0700-0700	11	NA NA	ND	NO WA ISC.
5.25 C 200 F 302 C 302 C 502	E TOTAL CANADA CANADA	Contract Con				
The second secon		300000		CALCULATION OF THE PARTY AND ADDRESS.		
AND SECTION OF SECTION SEC	4-5 Dec 06	0700-0700	0.5J	NA	ND	No permit limit.
Asenaphithene (µg/L)	5-6 Dec 06	0700-0700	0.4J	NA	ND	No WA TSC.
	6-7 Dec 06	0700-0700	ND	NA	ND	
	41.201.7					
Diethylphthalate	4-5 Dec 06	0700-0700	41	NA.	ND	No permit limit.
	5-6 Dec 06	0700-0700	6	NA.	ND	No WA TSC.
CUBLIF	6-7 Dec 06	0700-0700	5	NA	ND	
		58,400		A Company	4.0	
	4-5 Dec 06	0700-0700	2J	NA	ND	No permit limit.
disp-bytylphthalate	5-6 Dec 06	0700-0700	2J	NA	ND	No WA TSC.
<b>《新聞·西西斯斯斯</b>	6-7 Dec 06	0700-0700	1]	NA.	ND	
	THE SECRETARY	3-03-07-07-07			ND	
	4-5 Dec 06	0700-0700	0.4J		ND	No permit limit.
Rjuorene (nig/L)	5-6 Dec 06	0700-0700		NA NA	THE RESERVE THE PERSON NAMED IN THE PERSON NAM	No WA TSC.
			0.61	NA NA	ND	NO WA Tac.
	6-7 Dec 06	0700-0700	0.4J	NA	. ND	
7	204401.0	100				
Bu But beierschilalaie	4-5 Dec 06	0700-0700	4 J	NA	ND	No permit limit.
	5-6 Dec 06	0700-0700	7	NA	ND	No WA TSC.
5 200	6-7 Dec 06	0700-0700	7	. NA	ND	
THE PERSON OF	TRACE O	4000	Andreas and the	A THE SECTION	10 11 EV 10 2 S	
GULLER BIOLOGIC	4-5 Dec 06	0700-0700	10	NA	13	No permit limit.
Is Delhythesy lookthalate	5-6 Dec 06	0700-0700	16	NA	. 7	No WA TSC.
	6-7 Dec 06	0700-0700	16	NA	7	1
A TRACTOR BUT TO SERVE OF THE	75.000	HE STATE OF		region of	2.0000000000000000000000000000000000000	that the contract with the second
	4-5 Dec 06	0700-0700	1J	NA	ND	No permit limit.
r, dr.24D e Hojobenzene	5-6 Dec 06	0700-0700	1J ·	NA	ND	No WA TSC.
Fata (0840)	6-7 Dec 06	0700-0700	11	NA NA	ND	
100000000000000000000000000000000000000		144314 (256)				
Terms Veneral Roll	4-5 Dec 06	0700-0700			ND	No permit limit.
CHEEL 4-10 to troubelize tie			11	NA NA		No WA TSC.
75 (pg (bg (b) 4 7 °	5-6 Dec 06	0700-0700	5.1	NA NA	ND	NO WA 18C.
	6-7 Dec 06	0700-0700	5J	NA	ND	250
					See Section	
	4-5 Dec 06	0700-0700	7	NA NA	0.23	No permit limit. CShowled
- Naphalene (μέμ)	5-6 Dec 06	0700-0700	7	NA NA	ND	No WA TSC.
The state of the s	6-7 Dec 06	0700-0700	4J	NA	ND	
		A Maria	Selfer St	and an extension representation of the second		
	4-5 Dec 06	0700-0700	ND	NA	ND	No permit limit.
25 Phenantitene (ug.L)	5-6 Dec 06	0700-0700	1J	NA	ND	No WA TSC.
	6-7 Dec 06	0700-0700	0,61	NA	ND	
	100	18 19 E-12 F	Page 1	TANK SALES	114	
<b>""域"不"原现的</b>	4-5 Dec 06	0700-0700	· ND	NA	0.0079J	Effluent sample estimated concs.
Altha Chlordane	5-6 Dec 06	0700-0700	ND	NA	0.0061J	above acute/chronic WA TSC: Acute
As a (UgA).	6-7 Dec 06	0700-0700	0.00453	, NA	0.0059J	= 0.09 $\mu/L$ , Chronic = 0.004 $\mu/L$
	No. Page 19 and a second	al grant de la	100 E 100 E 100 E			
700 7500	4-5 Dec 06	0700-0700	0.094	NA.	ND	Influent sample concs. only above
	5-6 Dec 06	A	territoria de la companya de la comp		ND ND	WA TSC: Acute = 0.053 µ/L,
Heptachter (1g/L)	3-0 1360 00	0700-0700	0.52	NA	+ NU	Chronic = 0.0036 μ/L
	8 6-7 Dec 06	0700-0700	0.51	NA	ND	
	1	1				Not detected in effluent samples.
100	100	The state of the s	774.0%			
	4-5 Dec 06	0700-0700	ND	NA NA	ND	Influent sample estimated conc, above
op DDD	5-6 Dec 06	0700-0700	0.057J	NA	ND	WA TSC: Acute = 0.13 μ/L, Chronic
	6-7 Dec 06	0700-0700	ND	NA	ND	$= 0.001 \mu/L$
	260	1 0100	1 1100	1 *14 2	1	Not detected in effluent samples.

- 3) Laboratory quality assurance and quality control reports indicate that problems were encountered when analyzing some BOD<sub>5</sub> samples. The analytical lab reported that the problems suggested a "toxic interference in the samples." Further review of the lab QA/QC led to the discarding of days 2 and 3 BOD5 data and two individual BOD results from day 1.
- 4) A review of the concentration data indicates that pollutant concentrations generally decreased across each major unit process (primary clarifiers, trickling filters and secondary clarifiers), as expected. However, the day 3 TSS result for secondary clarifier effluent was uncharacteristically high and not consistent with the concentration reduction trend exhibited by the remainder of the data. The result suggests that a significant increase in TSS concentration (70 mg/L to 128 mg/L) occurred through the secondary clarifier, which is highly unlikely, especially considering the WWTP effluent concentration was 26.4 mg/L. The 128 mg/L result was considered an outlier and was excluded from the unit process performance evaluation.
  - d. Field Measurement Parameters (Wastewater).
- 1) Specific Conductivity, pH, Dissolved Oxygen and Temperature. These parameters were measured continuously with calibrated field instruments at select locations throughout the WWTP. A summary of the data is presented in Appendix B, Table B-2.
- 2) Effluent chlorine residual was randomly checked on three occasions during the 3-day sampling event using a HACH™ chlorine test kit. A summary of the data is provided in Appendix B, Table B-3. It should be noted that readings were performed on samples collected prior to de-chlorination. WWTP data for the same period is included in Table B-3; concentrations ranged from 0.11 to 0.21 mg/L after dechlorination.
- e. Sludge Sampling Results. A summary of detected parameters and their concentrations in sludge samples is provided in Appendix D, Table D-1, along with an evaluation of the sludge sample results and sludge management processes.
- f. WWTP and Unit Process Pollutant Removal Efficiencies. Flow rates and pollutant concentrations were used to calculate pollutant mass loadings and removal efficiencies.
- 1) Average WWTP removal efficiencies are summarized in Table 7 for all detected pollutants. Organic compounds were detected only in trace concentrations and often reported as estimated values. WWTP influent and effluent flow rates, pollutant concentrations and mass loadings, and removal efficiencies are detailed for detected analytical parameters (if applicable) in Appendix E, Table E-1. Note that when the effluent metals concentrations were non-detect, the removal efficiency was conservatively calculated with ½ of the reporting limit.
- 2) Unit process removal efficiencies for non-metals are summarized in Table 8. Metals were mostly removed in the primary and secondary clarifiers with sludge; the primary clarifiers removed most of the mass (of metals). Metals removal rates for the primary and secondary clarifiers are summarized in Tables 9 and 10, respectively. Metals were concentrated in the sludge (see Appendix D, Table D-1). Unit process influent and effluent flow rates, pollutant

concentrations and mass loadings, and removal efficiencies are detailed for detected analytical parameters (if applicable) in Appendix E, Table E-2. A detailed summary of unit process removals, including lbs/day removed is included in Appendix E, Table E-3.

- 3) The average influent BOD concentration (78 mg/L) was indicative of a low strength domestic wastewater. Influent TSS concentrations (54 204 mg/L) were consistent with low to medium strength wastewater. On average, the primary clarifiers removed 39.9 percent of BOD and 67.5 percent of TSS. These values were in the range of typical primary clarifier removal rates of 25 to 45% for BOD and 50 to 80% for TSS (WPCF 1990). The trickling filters effectively removed BOD, with an efficiency of 63.4 percent, within the typical range of 60 to 90% (Metcalf & Eddy 2003). Both trickling filters performed effectively. The secondary clarifiers removed 47.1 percent of BOD and 58.1 percent of TSS, resulting in a permit compliant effluent.
- 4) Influent total Kjeldahl nitrogen (TKN=organic nitrogen+ammonia+ammonium) concentrations (29 39 mg/L) and ammonia concentrations (24 26 mg/L) were consistent with a medium strength domestic wastewater. The WWTP effectively oxidized ammonia nitrogen to nitrite/nitrate as evidenced by similar mass increases and decreases in ammonia and nitrate/nitrite, respectively. On average, TKN was reduced by 77.5 percent. Significant nitrification occurred in the trickling filters, with a 71.5 percent reduction of ammonia nitrogen. This is an indication of an effective trickling filter, as significant nitrification occurs only after BOD concentration is appreciably reduced (i.e., to <30 mg/L) (Metcalf & Eddy 2003). Trickling filter effluent BOD concentrations ranged from 8.9 to 15 mg/L. Final effluent nitrate/nitrite concentrations ranged from 20 to 24 mg/L, most or all of which would be nitrate after chlorination. Final effluent ammonia concentrations ranged from 3.5 to 5.8 mg/L.
- 5) Influent phosphorus concentrations (3.6 4.8 mg/L) were consistent with typical low-strength domestic wastewater. Phosphorus persisted through the WWTP; however, the NPDES permit does not limit it.
- 6) Based on the averages of daily grab sample results, an estimated 314 lbs of diesel range TPH, 203 lbs of lube oil range TPH and 3.9 lbs of gasoline range TPH entered the WWTP each day. The lighter range TPH (gasoline and diesel) was more readily removed than the heavy range. An increase in TPH concentrations (based on grab samples) through the CCC was probably due to the floating scum layer at the end of the CCCs. Diesel range TPH effluent grab sample concentrations ranged from 0.83 to 4 mg/L. Heavy range TPH effluent concentrations ranged from 1.6 to 6.9 mg/L. The NPDES permit does not limit TPH, but requires no discharge of oily wastes which produce a sheen on the surface of the receiving water. No sheen was observed on the CCC effluent. The WWTP removed an estimated 79 percent of combined TPH.

Table 7. WWTP Average Removal Efficiencies.

Tasa sawa panasa	7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	Cemovai Emicie		
Analyte	Sample Dates	Sample Types	Average WWTP Removal Efficiency	<u>Comments</u>
ĐÔĐ.	4-5 Dec 06	24-hour composite	88.1	
TSS	4-7 Dec 06	Three 24-hour composites	80.2	
Ammonia	4-7 Dec 06	Three 24-hour composites	81.5	
Nitrate/Nitrite	4-7 Dec 06	Three 24-hour composites	See comment	The mass of nitrate/nitrite increased from non-detect (~0 lbs/day) in the influent to 453 lbs/day in the effluent due to nitrification of ammonia to nitrate/nitrite.
JKN	4-7 Dec 06	Three 24-hour composites	77.5	
Potal : Phosphorus	4-7 Dec 06	Three 24-hour composites	0.2	
Grease and Oil	4-7 Dec 06	Three grabs	See comment	Not detected in effluent at MRL (5.00 – 5.30 mg/L)
r TPHiDiesel Range	4-7 Dec 06	Three grabs	87.5 <sup>a b</sup>	
APHPHeavy Takinge	4-7 Dec 06	Three grabs	64.8 a b	
ATPHAGasoline	4-7 Dec 06	Three grabs	See comment	Not detected in effluent at MRL (48 µg/L) b
Aluminum	4-7 Dec 06	Three 24-hour composites	29.9	
Arsenic	4-7 Dec 06	Three 24-hour composites	See comments	Detected in one of three influent samples at 1.15 µg/L.  Detected in two of three effluent samples at 1.03 µg/L and 1.17 µg/L
Cadmium	4-7 Dec 06	Three 24-hour composites	See comments	Detected in one of three influent samples at $1.06 \mu g/L$ . Not detected in effluent at MRL $(1.0 - 2.0 \mu g/L)$
Chromium	4-7 Dec 06	Three 24-hour composites	See comments	Detected in two of three influent samples at 2.38 $\mu$ g/L and 2.59 $\mu$ g/L. Not detected in effluent at MRL (2.0 $\mu$ g/L)
титсоррег	4-7 Dec 06	Three 24-hour composites	41.0	
Jones Liveri	4-7 Dec 06	Three 24-hour composites	37.9	
Lead:	4-7 Dec 06	Three 24-hour composites	See comments	Detected in two of three influent samples at 1.28 µg/L and 1.22 µg/L. Detected in two of three effluent samples at 3.37 µg/L and 1.05 µg/L. Not detected on third sampling day in influent or effluent samples.
Mercury	4-7 Dec 06	Three 24-hour composites	See comments	Detected in one of three influent samples at 0.297 μg/L.  Not detected in effluent at MRL (0.2 μg/L).
Molybdenum	4-7 Dec 06	Three 24-hour composites	43.9	Notin Permit application but IN DMP
Nickel	4-7 Dec 06	Three 24-hour composites	75.5	
Selenium	4-7 Dec 06	Three 24-hour composites	ND	Not detected in influent or effluent samples at MRL (1.0 – 2.0 µg/L)
Silver	4-7 Dec 06	Three 24-hour composites	ND	Not detected in influent or effluent samples at MRL (1.0 µg/L)
Zinc	4-7 Dec 06	Three 24-hour composites	15.8	

a: Removal efficiency is based on grab samples taken during snapshots in time. Actual concentrations may fluctuate with time.

ND: not detected

b: Value is considered an estimate because it was calculated with grab sample results.

MRL: method reporting limit

Table 7. WWTP Average Removal Efficiencies (continued)

Table 7. WWIFAV	orage recinov	at Efficiencies	(continued)	
Analyte	Sample Dates	Sample Types	Average, WWTP Removal Efficiency (25)	Comments:
Chlaroforna	4-7 Dec 06	Three grabs	See comment	Not detected in influent samples. Detected in one effluent sample at estimated concentration of 1 µg/L. (Note: There are no Washington State marine surface water criteria for this pollutant)
5 14 dichlor benzene	4-7 Dec 06	Three grabs	See comment	Not detected in effluent samples.
H.2 dioblorobanzene	4-7 Dec 06	Three grabs	See comment	Not detected in effluent samples.
Tetrachlorosthene	4-7 Dec 06	Three grabs	See comment	Not detected in effluent samples.
A Tolucies	4-7 Dec 06	Three grabs	See comment	Not detected in effluent samples.
- A SPRENDING	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
Agenaphitiene	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
s ( -   Dietly philadae	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
den Bifylphijalate	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
Flüdener	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
e Buyllen, aphilain	3 <del>3</del> 4	Three 24-hour composites	See comment	Not detected in effluent samples.
Ba© anybekybpinikae	4-7 Dec 06	Three 24-hour composites	27.5	Note: There are no Washington State marine surface water criteria for this pollutant
E (1427) ichliciopensent	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
i I 44Dichlorobenzone	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
Nathalite 4	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
Pherpaulnerie*	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
Alpha Chlordene	4-7 Dec 06	Three 24-hour composites	See comment	to be exceeded).
THeptachor:	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.
c.p.DDD	4-7 Dec 06	Three 24-hour composites	See comment	Not detected in effluent samples.

a: Removal efficiency is based on grab samples taken during snapshots in time. Actual concentrations may fluctuate with time.

MRL: method reporting limit

ND: not detected

b: Value is considered an estimate because it was calculated with grab sample results.

Table 8. WWTP Process Data - Removal Efficiencies.

		ann a stair an an	100			
	er die		Primary"	Trickling .	Secondary	Chlorine 🤄
			Clärifier	r Gilter,	Clarifier :	or Contact
Analyte	Date	Sample Types	Removal : Efficiency	Removal	Removal-	Removal
			Efficiency	Efficiency (%)	Efficiency	Efficiency
						Yes and the second
FIFE BOD - 4.5	4-6 Dec 06	24-hour composites	39.9	63.4	46.9 ª	~0 ª
738	4-7 Dec 06	24-hour composites	67.5	26.3	58.1 b	2.9 <sup>b</sup>
Animopias "	4-7 Dec 06	24-hour composites	18.2	71.5	30.5	4.3
Nitrate/Nitrate	4-7 Dec 06	24-hour composites	Increase °	Increase °	17.9	3.2
: CALITRING	4-7 Dec 06	24-hour composites	27.5	65.3	34.6	-0.2
Cotal Phosphorus to	4-7 Dec 06	24-hour composites	33.4	-2.6	23.2	1.2
Grease and Oil	4-7 Dec 06	' Three grabs	71.1 <sup>d, e</sup>	51.9 d, e	ND d	ND d
TPH-Dievelskange	4-7 Dec 06	Three grabs	81.1 <sup>d, e</sup>	75.5 <sup>d, e</sup>	46.8 d, e	Increase d, f
TPH-Heavy Range	4-7 Dec 06	Three grabs	76.7 <sup>d, e</sup>	43.9 <sup>d, e</sup>	38.2 <sup>d, e</sup>	Increase d, f

a: Day 1 secondary clarifier effluent BOD result was discarded for laboratory QA/QC reasons. Removal efficiency across the secondary clarifier and CCC was calculated and all of the removal was presumed to occur in the secondary clarifier.

ND: not detected

Table 9. WWTP Process Data - Primary Clarifier Metals Removal Efficiencies (3-Day Average) Data.

		Primary Clarifier	
Analyte	Date	Refrioval Efficiency	Comments (1)
Aluminum	4-7 Dec 06	74.2	
Arsenic	4-7 Dec 06	36.0	Removal efficiency based on day one and two data. Not detected in influent or effluent on day three.
Cadmium	4-7 Dec 06	See comments	Detected in one of three clarifier influent samples at 1.39 μg/L. Not detected in clarifier effluent at MRL (1.0 - 2.0 μg/L).
Chromium	4-7 Dec 06	See comment	Not detected in clarifier effluent at MRL (2.0 µg/L).
Copper	4-7 Dec 06	56.1	
Iroficil	4-7 Dec 06	66.3	
Lead	4-7 Dec 06	73.0	Removal efficiency based on day one and two results. Not detected in clarifier effluent at MRL (5.0 µg/L) on day three.
Mercury	4-7 Dec 06	See comment	Not detected in clarifier effluent at MRL (0.2 µg/L).
Molybdenum	4-7 Dec 06	33.3	Not detected in clarifier effluent above MRL (5.0 µg/L) on day one; assume effluent concentration equals ½ MRL.
Nickel	4-7 Dec 06	45.0	
/Selenium	4-7 Dec 06	See comment	Detected in two of three clarifier influent samples at 1.15 and 1.39 $\mu$ g/L. Detected in one of three clarifier effluent samples at 1.04 $\mu$ g/L.
Silver!	4-7 Dec 06	See comment	Not detected in clarifier effluent at MRL (1.0 µg/L).
Zińc	4-7 Dec 06	60.0	

MRL: method reporting limit NA: not applicable ND: not detected

b: Removal efficiency was calculated with day 1 and day 2 TSS results.

c: Nitrate/nitrite concentration increases were indicative of nitrification of ammonia to nitrate/nitrite.

d: Removal efficiency is based on grab samples taken during snapshots in time. Actual concentrations may fluctuate with time.

e: Removal efficiency is considered an estimate because it was calculated with grab sample results.

f: TPH concentration increases through the WWTP/CCC were presumed to be attributed to the scum layer at the tail end of the CCCs. Diesel range TPH effluent concentrations ranged from 0.83 to 4 mg/L. Heavy range TPH effluent concentrations ranged from 1.6 to 6.9 mg/L.

Table 10. WWTP Process Data - Secondary Clarifier Metals Removal Efficiencies (3-Day Average) Data.

		Secondary	
Ånalyte	Date	Clatifier Removal Efficiency	Comments
	4.4	(%)!	
- Aluminum	4-7 Dec 06	54.1	
Assenic	4-7 Dec 06	25.1	Removal efficiency based on day one and two results. Not detected in clarifier effluent at MRL (2.0 µg/L) on day three.
:Cagmium	4-7 Dec 06	ND	Not detected in clarifier influent or effluent at MRL $(1.0-2.0 \mu/L)$
Chromium	4-7 Dec 06	ND	Not detected in clarifier influent or effluent at MRL (2.0 µ/L)
Copper	4-7 Dec 06	41.9	
Iron	4-7 Dec 06	48.4	
Lieade:	4-7 Dec 06	51.6	Removal efficiency based on day one and two results. Not detected in clarifier effluent at MRL (2.0 µg/L) on day three.
Mercury	4-7 Dec 06	ND	Not detected in clarifier influent or effluent at MRL (0.2 μ/L)
Molybdenum	4-7 Dec 06	31.2	
Nickel	4-7 Dec 06	49.6	Not detected in clarifier effluent above MRL (2.0 µg/L) on day one; assume effluent concentration equals ½ MRL.
Selenium	4-7 Dec 06	ND	Not detected in clarifier influent or effluent at MRL $(1.0-2.0 \mu/L)$
Silver ::	4-7 Dec 06	ND	Not detected in clarifier influent or effluent at MRL (1.0 µ/L)
Zinc	4-7 Dec 06	39.9	

ND: not detected MRL: method reporting limit

#### 8. PERMIT COMPLIANCE.

- a. Effluent data verified compliance with permit limits. A summary of effluent limits and sampling results is provided in Table 11.
- b. Based on a review of Monthly Facilities Engineering Operating Logs from 2004 to 2006; summarized in Appendix F, Tables F-1 through F-3, the WWTP was operated in compliance with permit effluent limitations, with one exception. In May 2006, treatment was inhibited by an unknown pollutant. Treatment in one of the two trickling filters was upset and effluent pH levels were below 6 for 6 days.

Table 11. NPDES Permit Effluent Limits and Evaluation Effluent Results.

Æfflüent Characteristic	Units of Weasure	Permit Efflu Average Monthly Discharge imit	LOCAL ALGERICA CATA SOCIAL AND	Darly Maximum Discharge Limit	WWTP Evaluation Epiluent Data
BOD.	mg/L	30	45	Min Ame	9.3 *
DU/U5	lbs/day	1902	2852	av itt	190 ª
TSS	mg/L	30	45	cus BY	23.7 b
	lbs/day	1902	2852	pa 49	495 b
Total Residual Chlorine	mg/L	en 04	Sia esc	0.5	0.11 - 0.21
pi		6.94 – 7.08°			

a: 6 Dec 2006 data

b: Three-day average

c: Three-day continuous monitoring

#### 9. CONCLUSIONS

- a. Data collected during the 3-day WWTP evaluation verified the following:
  - 1) The WWTP effluent was in compliance with effluent limitations.
- 2) The WWTP unit process removal efficiencies (for BOD and TSS) were within acceptable ranges.
- b. Based on a review of WWTP records (2004 to 2006), the WWTP was operated in compliance with permit effluent limitations, with one exception, when treatment was inhibited by an unknown pollutant in May 2006. One of the two trickling filters was upset, and effluent pH levels were below the lower effluent limit for six days.
- c. In addition to conventional wastewater pollutants (e.g., BOD<sub>5</sub>, TSS), WWTP influent and effluent samples were analyzed for numerous pollutants that are typically associated with "non-domestic discharges," including total petroleum hydrocarbons (TPH), metals, volatile organic compounds (VOCs), semi-volatile organic compounds (SVOCs), pesticides and polychlorinated biphenyls (PCBs). Several "non-domestic pollutants" were detected in WWTP samples.
- 1) TPH was detected in influent, effluent and sludge grab samples. The WWTP removed approximately 79 percent of influent TPH, some of which accumulated in the sludge with solids. The TPH concentrations in the WWTP effluent grab samples ranged from 2.3 to 10.9 mg/L. The discharge permit requires TPH monitoring, but does not include a concentration or mass limit. Available TPH data from Fort Lewis and this evaluation indicate that some components of influent TPH persist through the anaerobic digestion and composting processes. Biosolids management regulations (i.e., WAC 173-308) do not address TPH concentrations in biosolids.
- 2) Ten metals and eighteen organic compounds listed as toxic pollutants (per 40 CFR plane). Tables II and III) were detected in WWTP influent and/or primary clarifier influent samples. Five of the metals (arsenic, copper, lead, nickel and zinc) were detected in WWTP effluent samples. Only copper was detected in effluent samples at concentrations that exceeded the Washington marine surface water toxic substance criteria for the protection of aquatic life. Four of the organic compounds [chloroform, bis (2-ethylhexyl) phthalate, naphthalene, and alpha chlordane] were detected in WWTP effluent samples at trace concentrations. Only alpha chlordane was detected (at estimated trace concentrations) in effluent samples above. Washington marine surface water toxic substance criteria for the protection of aquatic life. It should be noted that the Washington toxic substance criteria apply to the receiving water, not the WWTP discharge; however, the criteria was compared directly to effluent concentrations to screen for pollutants that have potential to impact receiving waters.
- d. The Fort Lewis WWTP has the ability to produce biosolids that can meet the Class B biosolids criteria of WAC 173-308 (Biosolids Management). The combination of residence time (>15 days) and temperature (≥35 °C) in the primary digester meets the Class B biosolids pathogen reduction requirements of WAC 173-308-170. The vector attraction requirements may be met by incorporating the biosolids into the soil during land application or by one of the six

methods described in WAC 173-308-180. Metals concentrations in digested sludge samples were below the ceiling concentration limits (of WAC 173-308-160) for biosolids applied to land.

- e. A review of WWTP operating conditions and discussions with WWTP operators identified the following concerns.
  - One of two influent fine screens was inoperable; a permanent hoist is needed to lift the unit for maintenance and repair.
  - WWTP personnel indicated that several WWTP pumps were in need of maintenance, repair or replacement. These included several poor performing sludge transfer pumps. Most of the wastewater pumps were installed in the 1970s and lack variable speed operation and electronic controls that are necessary to optimize flow rates.
  - Broken plastic trickling filter media was observed on the top of the filters.
  - Cracks and evidence of leaking gas were observed in the cover/roof of primary digester No. 2.
  - Redundant unit processes were out of service for extended periods of time (i.e., primary digester No. 1 since October 2006, one primary clarifier since November 2006, and one chlorine contact chamber during February and March 2007).
  - Valves feeding digester sludge to drying beds are not water tight. When attempting to feed sludge to one drying bed, sludge leaks through valves to other beds.
  - A safety stairway platform and safety railing is needed on the grease vault to facilitate safe access for maintenance.
  - A catwalk is needed for safe sampling of digester sludge at the drying beds.
  - The grease collection container has an open top.
  - In-line magnetic flow meters had not been calibrated since they were installed in 2005.
  - Automatic samplers were not flow paced.
  - The chlorine feed system had not been calibrated for two years.
  - The chlorine feed system required more modern feed pumps and chlorine sensors.
  - Primary sludge pumping was not controlled based on sludge thickness (i.e., pumping was continuous and constant regardless of solids concentration). Pumping rates appeared to be excessive.
  - Constant-speed pumps feed wastewater (including recycle flows) to the trickling filters.

    The pumping flow rate and recycle flow rate cannot be adjusted and monitored to optimize treatment.
- f. The WWTP was staffed with only five operators and one lab technician, who covered day, night, and swing shifts for 24-hours per day, seven days per week. Operators were required to perform lab work in the absence of the lab technician and to work over-time to cover routine operations.
- g. Per Washington Administrative Code (WAC) 173-230, the "operator in responsible charge" is defined as "the individual who is routinely on-site and in direct charge." A Class III

WWTP requires a Group III (or higher) "operator in responsible charge" with at least a Group II "operator in charge of each shift." While the USEPA issued permit does not specify requirements for certification of operators, Army Regulation 420-49 (Facility Engineering Utility Services) states (in paragraph 2-4) that "utility plant operators...will meet applicable ... State... certification requirements for the State in which they are located." The WWTP supervisor was not routinely on site and did not have a Group III license.

#### 10. RECOMMENDATIONS.

- a. Initiate a pretreatment program to verify the presence/absence of non-domestic pollutants identified in this evaluation and identify pollutants of concern (POCs) and discharges that may interfere with the operation of a WWTP, pass through the WWTP, or interfere with sludge management (digestion, use, or disposal). A pretreatment program will serve to trace POCs (e.g., TPH, metals, toxic organic compounds) back to discharge source areas in the collection system and provide a mechanism to enforce limits on dischargers of POCs.
- b. Investigate alternative regulatory criteria (e.g., TPH soil remediation action levels) for reuse of TPH-containing biosolids and pursue regulatory approval for land application or properly dispose of biosolids.
  - c. Ensure that primary digester temperatures are maintained at a minimum of 35°C.
  - d. Install a permanent hoist to lift the fine screens for maintenance and repair.
- e. Repair or replace problematic pump components, as necessary. Prepare for the eventual replacement of primary/secondary sludge pumps and trickling filter feed pumps with variable speed, high efficiency pumps, with electronic controls.
- f. Remove and replace broken trickling filter media; inspect underlying media and replace, as necessary.
  - g. Repair the cracks in the cover of primary digester No. 2.
- h. Plan repairs of redundant major unit processes to minimize "out of service" time and, if possible, do not schedule maintenance and repairs of major wastewater treatment unit processes during the winter/wet season.
  - i. Repair or replace valves on digester sludge pipe to biosolids beds.
  - i. Install a stairway, platform and safety railing at the grease vault.
  - k. Install a catwalk for digester sludge sampling at the drying beds.
  - 1. Provide a covered container for grease collection.
  - m. Calibrate flow meters and the chlorine feed system semi-annually,

- n. Flow pace the influent sampler off of a new influent flume and flow meter and flow pace the primary clarifier effluent and WWTP effluent samplers off of an effluent flow meter.
  - o. Replace chlorine feed and sensor systems with new technology.
- p. Control primary and secondary sludge pumping based on sludge thickness by adjusting pumping and/or collection schedules. At a minimum, minimize unnecessary pumping of "thin" sludge and dilution water.
- q. Consider replacing trickling filter pumps with variable speed pumps and installing a flow measurement device on the trickling filter recycle line so that trickling filter treatment may be optimized.
  - r. Increase WWTP staff by one lab technician and at least one operator.
- s. The operator in responsible charge should be routinely on site and have a Group III WWTP operator license.

PREPARED BY:		
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APPROVED BY:		(b)(6)
•		Chief, Wastewater Section Surface Water and Wastewater Program

#### APPENDIX A

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Report No. 32-EE-05Y1-07, 29 November – 7 December 2006

#### APPENDIX B

WASTEWATER SAMPLING RESULTS

Table B-1. Detected Analytes and Concentrations in Wastewater.

Ambita	Desc		WILLIAM TO THE	Primary	Pinnay . Clarifier	Trickling	Trickling	Trickling Filler Combined	Secondary (Clarifier Effluent/	WWIP	Slödge Thickener Supernatant	Primary Digester Supernatant	Secondary Digester Supernatant		Equipmen
Analyte Date Time		WWIP Influent	Clarifier Influent	Effloent (Trickling Filter Influent)	Filter#1 Effluent	Filter#2 Effloent	Effluent/ Secondary Clarifier Influent	Chlorine Contact Chamber Influent	Effluent	(returned to Primary Clarifiers)	(flows to Secondary Digester) (grab)	(flows to Primary Clarifiers) (grab)	Field Blank	Blank	
Aura to	4-5 Dec 06	0700-0700	78	61	41	14/7.4 J, D	8.9	15	3.8 J, D	9,3	34			1.1	
BOD (mg/L)	5-6 Dec 06	0700-0700	340 J, D	50 J, D	82 D	24 D	15/29 J, D	22 J, D	29 J, D	26 J, D	46 J				6.4
September 1995	6-7 Dec 06	0700-0700	31 D	42/41 D	5.3 J, D	5.8J, D	28 D	34 J, D	38 J, D	27 J, D	33	720 J	680.0 J	2.7	
	F4.51 1857 F6	12 TE 16		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	9-05	A STATE OF THE STA	Section 1				2. 254.6-				
Talku arl-cui	4-5 Dec 06	0700-0700	54	228	80	44/50	41.0	45	22	20	62.2	<u> </u>	<u> </u>	ND (<3.3)	
(TSS (mg/L)	5-6 Dec 06	0700-0700	98	220	79	45	50.0/52	49	24	24.7	100				ND (<3.3)
Acceptable Link	6-7 Dec 06	0700-0700	204	178/220	68	34	48.0	70	128	26.4	95	19200	17900.0	ND (<3.3)	
	The State of	(A) (1) (A) (A) (A) (A)	THE SHIPPING	A, 80 YA 12		STANCE OF	A CONTRACTOR	Total Service	100	1446 156A	The control of	14. E 1. 1777	Carles Maria		
	4-5 Dec 06	0700-0700	24	21	19	3.4/3.6	4.0	4.1	3.4	3.5	9.4	ļ		0.1	
Ammonia (mg/L)	5-6 Dec 06	0700-0700	25	23	19	5.3	6,7/6,6	6.3	4.8	4,5	12		<u> </u>		ND (<0.050
	6-7 Dec 06	0700-0700	26	24/26	24	6,5	7.1	7.4	6.2	5.8	13	630	690.0	ND (<0.050)	<u> </u>
MARKET LEGISLATION	. ************************************			100		H4191 N. H. W. P. P. L.	Contract Contract	<b>图 28 阿勒拉克</b>	25 1896, 762	(1-3 XP)	11. 23.	Personal Control		Parks and	
	4-5 Dec 06	0700-0700	ND (<0.050)	1.3	4	20/20	18	19	21	20	13		<u> </u>	ND (<0.050)	ļ
Nitrate/Nurite (mg/L)	5-6 Dec 06	0700-0700	ND (<0.050)	3.5	4.8	23	25/23	23	20	21	81				ND (<0.050
19045-0072-07	6-7 Dec 06	0700-0700	ND (<0,050)	4/3.6	4.1	26	25	28	26	24	18	0.091	0.1	ND (<0.050)	
	Add Act			7 - 2480:55	The Late of the la	<b>6</b> 7 - 12	14-45-64		A. S. C. S. L. S.	the second		Carry Carry	A STATE	Type Switch	
	4-5 Dec 06	0700-0700	29	33	27	8.6/7.9	8.7	8.9	5.8	6.7	16			0.2	1
TKN (mg/L)	5-6 Dec 06	0700-0700	37	38	30	9.5	11/12	11	8.3	8.1	20				0.18
2 PMP 350 to	6-7 Dec 06	0700-0700	39	39/38	32	10	12	11	9.4	8.8	21	1300	1100.0	0,2	i
	100000			2200		AND STREET	r Than stage	(1) 100 (1)	THE PROPERTY.		/加州市州市(特別		E. 100 € 20		
	4-5 Dec 06	0700-0700	3,61	6.17	4.3	4.27/4.35	4.28	. 4,35	3.73	3.72	4.68			ND (<0.0100)	
Total Phosphorus (mg/L)	5-6 Dec 06	0700-0700	4.2	6.25	4.9	4.85	4,98/4.87	4,93	4,46	4,34	6.11				ND (<0.0100
	6-7 Dec 06	0700-0700	4.8	6.25/6.3	4.69	4.82	4.83	4.97	4,55	4.54	- 6.15	247	198.0	ND (<0.0100)	
	a service.				Jan Service	The state of the state of	W 155%				TO BENEFIT TO SERVE	Self in the residence in	4 4		
ANTENNE DE L'ANTE	4-Dec 06	grab	21	26	12	ND (<6.00)	ND (<6.00)	ND (<5.30)	ND (<5.50	ND (<5.30)	ND (<5.00)			ND (<6.00)	
Oil and Grease (mg/L)	5-Dec 06	grab	7.79	7.33	10.6	ND (<5.00)	ND (<5.00)	ND (<5.00)	ND (<5.00)	ND (<5.00)	ND (<5.00)			ND (<5.20)	
And the second second	6-Dec 06	grab	6,33	6,56	ND (<5.00)	ND (<5.00)	ND (<5.00)	ND (<5.00)	ND (<5.70)	ND (<5.10)	ND (<5.00)	552	312.0	ND (<5.20)	
THE PARTY OF THE PARTY OF THE	W-SHIELD OF	1.80				10000	1	500 M	<b>学型的公司等于</b>	は自然の信仰		777 200			
Take 1871 1871 1871 1871	4-Dec 06	grab	15	53	6.500	1,3	1.8	1.5	1.2	0,690J	7.4				
TPH Diesel Range (mg/L)	5-Dec 06	grab	12	14	5.800	2	2.1	1.5	0,790	0.830	4.1				
tate to	6-Dec 06	grab	18	13	4.500	1.1J .	1,3 .	1.13	0.5603	4	3	150J	ND(<80)		
Table 1-1	HE DEC			And the second	200		The state of the s	Military Carlot	7.9	4.00-48.00	Paris and South	San Asia Cara	क्ष्रसम्बद्धाः नद्धाः र ।	ay, f	
	4-Dec 06	grab	11	27J	6,4J	1.9J	2.63	2.2J	1.6	1.63	7.33				
PH Heavy Range (mg/L)	5-Dec 06	grab	7.21	11	3.7J	2.5	2.8	2,3J	1.7J	1.6	3.3J				
	6-Dec 06	grab	113	133	3.21	2.23	2.43	2.33	1.6J	6,9	3.63	570	380		
	STOREST STATE		74.5-20.05 TEST 15.7	100 Sept. 1	Table 11 1 74 1 1 1 1 1	Property Like	计可能记忆 计图		<b>第二十四十二十二</b>		n terkulsi (iku)				
TPH-Gasoline (mg/L)	4-Dec 06	grab	0.280							ND(<0.048)					
TPH-Gasoline (mg/L)	5-Dec 06	grab .	0,1403							ND(<0.048)					
生态 政治 经经济 化二元 化二二二二二二二二二二二二二二二二二二二二二二二二二二二二二二二二二	6-Dec 06	ereb	0.1503							ND(<0.048)				1	

J: estimated value ND: not detected D: data was discarded due to laboratory QA/QC findings Example: (<5.00) = the analyte was not detected above the 5.00 mg/L reporting limit

Analyte	Date	Time	WWIP Influent	Primary Clarifier Influent	Primary Clarifier Effluent (Trickling Filter Influent)	East Trickling Filter Effluent	West Trickling Filter Efficient	Inckling Filter Combined Effluent Secondary Clarifier Influent	Secondary Clarifier Effluent/ Chlorine Contact Chamber Influent	WWTP, Effluent	Studge Thickener Supernatent (returned to Primary Clarifiers)	Primary Digester Supernatunt (flows to Secondary Digester) (grab)	Secondary Digester Supernatant (flows to Primary Clarifiers) (grab)	Field Blank	Equipmen Blank
SERVELLO -	4-5 Dec 06	0700-0700	0,208	1.34	0.47	0.436	0.422	0.482	0.27 -	0,243/0,227	0.532		<u> </u>	ND (<0.200)	
Aliminum (mg/L)	5-6 Dec 06	0700-0700	0.291	1.46	0.414	0.459	0.464	0.474	0.261	0,252	0.907				ND (<0.200
A Charles Share and the	6-7 Dec 06	0700-0700	0,547	1.36	0.318	0.426	0.427	0.461	0.228	0.246	0.964	234	235	ND (<0.200)	
	in the second					1.4.4.2		行れている歴	AMERICAN.	<b>经产品的第三人</b>		THE COLUMN		4 \$ 3.5	1 100
and the state of	4-5 Dec 06	0700-0700	ND(<1.00)	1.49	1.14	1.06	1.02	1.16	1.09	1.03ND(<1.0)*	1.09			ND (<1.00)	
- Arsenic (ug/L)	5-6 Dec 06	0700-0700	1,15	1.74	1.17	1.15	1.21	1.23	. 1	1.17	1.32	<u> </u>			ND (<).00
* 41.4e4 (8**	6-7 Dec 06	0700-0700	ND(<2.00)	ND(<2.00)	ND(<2.00)	ND .	ND	ND(<2.00)	ND(<2.00)	ND(<2.00)	ND(<2.00)	101	94,4	ND (<2.00)	
				APPENDED	Marty	9-1.7-MARGEY		S. 12 14 15 12 12	4.7.		Charles Line	Branch Comment	aria Elber	1 2 2	1
	4-5 Dec 06	0700-0700	ND(<2.00)	ND(<2.00)	ND(<2.00)	ND	ND	ND(<2.00)	ND(<2.00)	ND(<2.00)/ ND(<2.00) <sup>6</sup>	ND(<2.00)			ND (<2.00)	
Cadmium (ng/L)	5-6 Dec 06	0700-0700	ND(<2,00)	ND(<2.00)	ND(<2.00)	ND .	ND	ND(<2.00)	ND(<2.00)	ND(<2.00)	ND(<2.00)		,		ND (<2.00
	6-7 Dec 06	0700-0700	1,06	1.39	ND(<1.00)	ND	ND	ND(<1.00)	ND(<1.00)	ND(<1,00)	1.03	174	153	ND (<1.00)	
			10041.73		PORT S-12034			3744	Section 1	Flack March	\$600 CO S			- + +	12
	4-5 Dec 06	0700-0700	16.9	20	17.3	17.6	17.4	17.9	17	16,6/16.2 d	18			ND (<0.100)	1
c Calcium (mg/L)	5-6 Dec 06	0700-0700	18,1	20.9	18.3	18.8	18.7	19	18	18.4	20,3			1	ND (<0.100
	6-7 Dec 06	0700-0700	19,3	21.1	18.6	19.3	18,8	19.2	18.1	18.9	21.2	569	597	ND (<0.100)	
		1 1 1 1 1 1 1 1		<b>全国的第三人称</b>	TE UT INST	- 175 Sept - 20	Z. OWNER TO THE	Carry Dates	CE TO SEE	2007 Carlo	11.745.04	異名的特別 英语			
	4-5 Dec 06	0700-0700	2.59	2.71	ND(<2.00)	ND	ND	ND(<2.00)	ND(<2.00)	ND(<2.00)/ ND(<2.00) <sup>4</sup>	ND(<2.00)			ND (<2.00)	
Chromium (cre/L)	5-6 Dec 06	0700-0700	ND(<2.00)	2.63	ND(<2.00)	ND	ND	ND(<2.00)	ND(<2,00)	ND(<2.00)	ND(<2,00)			·	ND (<2.00)
	6-7 Dec 06	0700-0700	2,38	2.82	ND(<2.00)	ND	ND	ND(<2.00)	ND(<2.00)	ND(<2,00)	2.05	471	375	ND (<2.00)	1.2 ( 4.55
A CARLO CONTRA		75,000 (F	a the state		Service of the	40466.14		G - 725.8	202 - 2045	100000000000000000000000000000000000000			THE SHARES	2	
	4-5 Dec 06	0700-0700	45,8	100	48.7	45.9	44,7	49.8	35.7	32.7/33.7	48.8	- ALDEC 1922 CR   C221 25 CA	<del></del>	ND (<1.00)	
Gopper (ug/L)	5-6 Dec 06	0700-0700	51.3	112	53	55.9	55.7	52,7	35.9	36.7 -	76.3			335	ND (<1.00)
	6-7 Dec 06	0700-0700	78,5	108	55.1	56.8	54.1	58,6	37.6	34.8	78.8	15300	12000	16.1	135 ( 135 )
	100		1 2000		STATE OF STREET	10 M	V 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	SOFT SECTION	CHARLEST CONTRACT	Col. C. C. Transaction				3.7.7.7	
964 G	4-5 Dec 06	0700-0700	0.362	1,04	0,471	0.437	0,445	0.512	0.333	0,269/0,178	0.488			ND (<0.0500)	
fron (mg/L)	5-6 Dec 06	0700-0700	0,337	1.11	0,42	0,465	0,463	0,459	0.279	0.258	0.718				ND (<0,0500
Transaction of the second	6-7 Dec 06	0700-0700	0,558	1,22	0,379	0,439	0,419	0.485	0.265	0.258	0,757	134	135	ND (<0.0500)	
		77. N. 897.		A PARTICIPATE	FR. LABOURY	Property of	45.20g(1)276	Berlin and B	31.14	100 May 11 15 15 15 15 15 15 15 15 15 15 15 15		<b>建筑建筑</b>			T
Market 28 Sept 6	4-5 Dec 06	0700-0700	1,28	6,08	1.84	1,67	2,04	1.67	1.14	3.37/1.03 d	1.91			ND (<1.00)	
, Lead (jug/L)	5-6 Dec 06	0700-0700	1,22	5.26	1.58	2,05	1,91	2.29	1.1	1.05	3.22				ND (<1.00)
	6-7 Dec 06	0700-0700	ND(<5.00)	6.67	ND(<5.00)	ND	ND	ND(<5,00)	ND(<5.00)	ND(<5.00)	ND(<5.00)	1170	1010	ND (<5.00)	
CHEST OF THE PARTY	10.44 A	34. 1.119.		6-19-64 THE BOOK	All the state of the state of	de la	TO A STANKE	<b>企业中国</b>		현고 연소화를	at street, S	<b>经制气进行</b>			
MARKET ALCOHOLOGIC	4-5 Dec 06	0700-0700	5.32	5.77	5,33	5.5	5,53	5.57	5.33	5.24/5.05 <sup>d</sup>	5.52			ND (<0.200)	
Mainesium ((mg/L)	5-6 Dec 06	0700-0700	5.63	5.9	5.54	5.67	5.67	5.74	5.49	5.64	5,91				ND (<0.200)
	6-7 Dec 06	0700-0700	5.74	5.93	5.66	5.79	5.6	5.75	5.47	5.66	6.06	70.6	71.9	ND (<0,200)	
12000	Anna Bangahan	Ar Asir Digit	Land Company	<b>经过程的</b>	12 14 15 17 THE PARTY	元 2000年2月16日	<b>建大路内别</b> 。	No. of the state of	(L=1) (A) (-)	F-34-5-749 15 1	過去。性質		HALL THAT	<b>对于人员。"他的代表</b>	Çakirin E. T. J
Para San	4-5 Dec 06	0700-0700	ND(<0.200)	0.278	ND(<0,200)	ND	ND	ND(<0.200)	ND(<0.200)	ND(<0.200)/ ND(<0.200)*	ND(<0.200)			ND (<0.200)	
Mercury (ug/L)	5-6 Dec 06	0700-0700	ND(<0,200)	0,699	ND(<0.200)	0,258	ND	ND(<0.200)	ND(<0.200)	ND(<0,200)	ND(<0.200)			1	ND (<0,200)
	6-7 Dec 06	0700-0700	0.297	0,527	ND(<0.200)	ND	ND	ND(<0.200)	ND(<0.200)	ND(<0.200)	ND(<0.200)	30.9	26.0	ND (<0.200)	
COLUMN TO SERVICE STREET				5 7 5 VA	AND THE SECOND				es albana fara	A STATE OF THE STATE OF		NAME OF THE OWNER, OWNER, OWNER, OWNER,	Sand House	पद्धा को हुए कर्मान्स	-42" "
	4-5 Dec 06	0700-0700	12.4	11.7	ND(<5.00)	8,59	9,45	9.61	6.28	5.67/ND(<5.00	8.03			ND (<5.00)	· · · · · · · · · · · · · · · · · · ·
Molybdenum (ug/L)	5-6 Dec 06	0700-0700	11.1	11.2	10,5	10.9	10.8	10.1	9,66	9,91	11,2				ND (<5,00)
	5-0 Dec 06	0700-0700	23.3	17.2	16.7	15.3	14.3	15,4	12.2	10.8	14.7	338	309.0	1.1	(
CONTRACTOR	0-1 Dec 00	0700-0700	######### 1 W 1	Salar Mara	545.55 Jan - 1	12	14.5	13.7 13.2 (1.1)	55-56-6-57P-3			1 v 0 4 4 4 4 5	(44	< = 1 € (m)	· · · · · · · · · · · · · · · · · · ·
THE PROPERTY OF STREET	4-5 Dec 06	0700-0700	11.2	4.49	2.47	2.19	2.54	2.32	2.24	2.45/4.00	5.62	a. 15160-5154		ND (<2.00)	<del></del>
	***JLRCCUO i	U20040700													ND (<2,00)
Nickel (ug/I)	5-6 Dec 06	0700-0700	6.93	3.79	2.41	2.56	3.18	3,87	ND(<2.00)	2.64	3.96	1	3		

J: estimated value ND: not detected d: dissolved metal concentration

Table B-1. Detected Analytes and Concentrations (continued).

Audys	18ble b-1. Detected Ana			TO THE PROPERTY OF THE PARTY.	YOUR AND DESIGNATION	the second second second	AND REPORTED IN	2014 - Carlo Lavor VIII (1977)	S. Carlos Cristoly Commercial	I I STATE OF THE S	entral restriction in the		Chr. March 1997			~
Authors			A 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		Primary		East					Thickener			N. St.	
Add   Dec     Dec     Dec	Analyte	Date	Time	WWTP Influent	Clarifier	Efflicent			Effluent/						Field Blank	
4.5 Dec   0700,0700   ND(=10)   1.15   ND(=100)   ND(	-	ſ			Influent	(Trickling					Effluent				I RIG DIGIA	Blank
4.5 Dec 65 0700-0700 ND(-1.07) 1.15 ND(-1.05) ND		1		-		Filter Influent).	EHHem	+ riment	Clarifier	Chamber			Digester)		1	
\$45   Dec   66   Price   Pri			1			Land Land	- 32		Influent -	Influent	T.V	Clammers)	(grab)	(grab)		
4-5 De 66	STATE NAME.			1			ND	ND	ND(<1.00)	ND(<1.00)		ND(<1,00)			ND (<1.00)	
4-5 De 66									ND(<1.00)	ND(<1.00)	ND(<1.00)	ND(<1,00)				ND (<1.00)
## 4-Dec 6				ND(<2.00)											ND (<2.00)	
Section   Sect		, (अनुष्याम् भयः स्	Bank Cale	STREET, CHOOSE	1			PARTICION NO.		<b>中华生产的</b>	大学学院 かんかん	地 机 图图程序	Section of the second		21.124	
4-50e 6 700-000 0.8 0.34 0.105 0.097 0.093 0.100 0.074 0.074 0.074 0.112 NPC-0.000		4-5 Dec 06	0700-0700	ND(<1.00)	1,26	ND(<1.00)	- ND	ND	ND(<1.00)	ND(<1.00)		ND(<1.00)			ND (<1.00)	
4-50e 6 700-000 0.8 0.34 0.105 0.097 0.093 0.100 0.074 0.074 0.074 0.112 NPC-0.000				ND(<1.00)		ND(<1.00)		ND	ND(<1.00)	ND(<1.00)	ND(<1.00)	ND(<1.00)				ND (<1.00)
4-5 Dec 66   0700-0700   0.08   0.433   0.105   0.097   0.093   0.101   0.074   0.076, 0.076   0.112   0.105   0.000	Tipe 22	6-7 Dec 06								ND(<1.00)	ND(<1.00)		31.9		ND (<1,00)	
March   Marc		Assistant Section												Section 1	STATE:	
April   Apri															ND (<0.0200)	
April   Apri	Sanc (mg/L)													<u> </u>		ND(<0.0200)
Company   Comp	200	6-7 Dec 06										0.178				
Some   No	VOCat(pg/s)			The state of the s					THE STATE OF THE STATE OF					14.7	Market State and a con-	
Section   Sect																
4-De	* *Guiomioro (ug/L)													l		
4-De	A STEEL															
Solution	TOP THE STATE OF T		The party of the last	Language Control of the Control of t	<b>公司中央公司</b>			12 THE P. LEW.	1.1	5 7 7 7 7 7			7.536		<b>7200年 1000 1000 1000 1000 1000 1000 1000 </b>	
Abba   21																A
Abba   21	"Talkdichiorobenzene"(µg/L)								ļ							
Abba   21								1								~
Section   Sect	A STATE OF THE STA		A.55.	-		100000000000000000000000000000000000000		F 42 100	200 March 200 M			- 10 Sec. 7	36 C. S.	Charles and Charles and		
4-Dec   31   ND   ND   ND   ND   ND   ND   ND   N								ļ	ļ							
4-Dec   31   ND   ND   ND   ND   ND   ND   ND   N	2 Additional inventor (ng/1)					-										
S-Dec   ND   ND   ND   ND   ND   ND   ND   N	A CONTRACTOR OF STREET								220200000000000000000000000000000000000	S 11 10 T CAN T 17 LT TOTAL			NAMES OF THE OWNERS OF THE OWNER		30.52.390	·
S-Dec   ND   ND   ND   ND   ND   ND   ND   N	Company of the second		Same and		R. H. Shian			C-14641-3	2012	10 St. 10 St.		1 (3 m 2 3 a - 1)	MARKET LEADING	S. Marie Land Millian	CHEST WAY	
4-Dec   21   ND   ND																
A-Dec   21	ar len schloroethene (up/L)		<del> </del>													
A-Dec   21		5-L/ec	the security of			0.200028199035	TOTAL COMMISSION	Commence of the Section	280-1903 NAPERWY	AND REPORT OF THE PERSON OF TH		active exercises out of	CONTRACTOR OF THE	SECTION SECTION	<del></del>	
Signature   Sign	STREET, STREET		BRAD SAF FAMILY		A COLUMN TO SECTION	04 500 40 - 51 TAV	Electrical State	100 F35 9 F37 F37	45 30 B	at a fair at a fair and a fair a		STATE OF STREET	E-977 Mark - 11. 12	27 23 24 24 24 25 25		<del></del>
A 5 Dec 06   0700-0700   6   ND   ND   ND	PARTY SECTION							<del> </del>								
A 5 Dec 06   0700-0700   6   ND   ND   ND						-		<del> </del>						<del>  </del>		
4-5 Dec 06		0-DEC	STATE STREET		NEL KORIN	(5.77@a/,az <b>cs</b> e)	****	CONTRACTOR OF THE RESERVE	J. P. T. LANSING SHOP	32.500 At 25.50		St. C. ARESTONES	AND CONTRACTOR	a carrage vers		
Section   Sect		4-5 Dec 06	0700-0700			CART - 1-4-5-4-2-4-2-4-2-4-2-4-3-4-4-4-4-4-4-4-4-4-4	Connect of the Party of the Connect of	To the section of the country of the	A SECTOR SWIDE, DESCRIPTION			100	As a recommendate of heart and	المستحدث المتالك	ND	
A-5 Dec 06   0700-0700   11   ND   ND								l								
45 Dec 06 0700-0700 0.51 ND					i			<b> </b>								
4-5 Dec 06 0700-0700 0.51 ND	Constitution of the second					KG CK	1176 2.736	55909555	COAS EVEN	833518.45		391 and 3500			Marie Company	
Administrative (see it)							Constitution for a first think the second	37.300.35						1		
4.5 Dec 06 0700-0700 ND	A A STATE OF THE S															
4-5 Dec 66 0700-0700 4J ND ND ND ND ND																
4-5 Dec 06 0700-0700 47 ND ND ND				ST 2 188-9504	5. HE 1885 (6)	ARCHES IN	71-18 - E I - E I	<b>建筑中间30%</b>	1450156	95.27	22 36 97 7	COLUMN TO SERVICE STREET	CONT. CENT	1840 F 1877	1975	
2017-000-000-000-000-000-000-000-000-000-		4-5 Dec 06	0700-0700	The same of the sa											ND	
6-7 Dec 06 0700-0700 5	Dietholphinalite (j.gd.)										ND					
											ND		4			

J: estimated value ND: not detected d: dissolved metal concentration

Table B-1. Detected Anabates, and Concentrations (continued).

ank Equipment Blank				3.6																			2 mm 2 m																
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estimated value ND: not detected

Table B-2. Wastewater Quality Field Measurements.

Parameter	Date/ Time	기속에게 걸맞잠시하다.	(P Influent	Primary C	Filter Inflaent / larifier Effluent		ng Filter Effluent/ y Clarifier Influent	ww	TP Effluent
		Readings	Comments	Readings	Comments	Readings	Comments	Readings	Comments
	4-5 Dec 06/ 0700-0700	Min.: 5.93 Max.: 6.80 Avg.: 6.49	Continuous readings	Min.: 6.88 Max.: 7.41 Avg.: 7.15	Continuous readings	7.46	Collected @ 0800 hrs	Min.: 6.99 Max.: 7.18 Avg.: 7.13	Continuous readings
PH.	5-6 Dec 06/ 0700-0700	7.12	Collected @ 1630 hrs	Min.: 6.84 Max.: 7.31 Avg.: 7.03	Continuous readings	7.05	Collected @ 1630 hrs	Min.: 6.94 Max.: 7.11 Avg.: 7.02	Continuous readings
Action in the Ac	6-7 Dec 06/ 0700-0700	Min.: 5.11 Max.: 7.53 Avg.: 6.05	Continuous readings	7.23	Collected @ 1000 hrs	6.75	Collected @ 1030 hrs	Min.: 6.95 Max.: 7.01 Avg.: 6.99	Continuous readings
						YST YET	Company of the second		, NA 12
	4-5 Dec 06/ 0700-0700	Min.: 296 Max.: 594 Avg.: 441	Continuous readings	Min.: 314 Max.: 391 Avg.: 357	Continuous readings	335	Collected @ 0800 hrs	Min.: 361 Max.: 400 Avg.: 377	Continuous readings
, Specific Conductivity ∴ (μS/cm)	5-6 Dec 06/ 0700-0700	544	Collected @ 1630 hrs	Min.: 333 Max.: 424 Avg.: 375	Continuous readings	414	Collected @ 1630 hrs	Min.: 385 Max.: 431 Avg.: 413	Continuous readings
	6-7 Dec 06/ 0700-0700	Min.: 345 Max.: 1269 Avg.: 495	Continuous readings	466	Collected @ 1000 hrs	344	Collected @ 1030 hrs	Min.: 428 Max.: 432 Avg.: 431	Continuous readings
	registry, in contrast of					30000000000000000000000000000000000000			April 1995 - Barton II.
	4-5 Dec 06/ 0700-0700	33.0	Collected @ 0730 hrs	Min.: 80.9 Max.: 97.7 Avg.: 84.4	Continuous readings	94	Collected @ 0800 hrs	Min.: 32.0 Max.: 43.9 Avg.: 38.4	Continuous readings
Dissolved COxygen (%))	5-6 Dec 06/ 0700-0700	10.2	Collected @ 1630 hrs	Min.: 70.7 Max.: 84.0 Avg.: 78.9	Continuous readings	90	Collected @ 1630 hrs	Min.: 31.4 Max.: 61.5 Avg.: 49.1	Continuous readings
	6-7 Dec 06/ 0700-0700	25.5	Collected @ 0800 hrs	31	Collected @ 1000 hrs	89	Collected @ 1030 hrs	Min.: 42.3 Max.: 47.2 Avg.: 46.1	Continuous readings
	St. Gangaganer - Inc. and the						And the second s	rana e de la Compania de la Paris.	A Telephone Control
	4-5 Dec 06/ 0700-0700	Min.: 14.93 Max.: 16.29 Avg.:15.76	Continuous readings	Min.: 13.54 Max.: 14.66 Avg.: 14.39	Continuous readings	13.43	Collected @ 0800 hrs	Min.: 12.68 Max.: 13.70 Avg.: 13.34	Continuous readings
Temperature (CO)	5-6 Dec 06/ 0700-0700	15.88	Collected @ 1630 hrs	Min.: 14.00 Max.: 14.97 Avg.: 14.66	Continuous readings	14.91	Collected @ 1630 hrs	Min.: 13.61 Max.: 14.18 Avg.: 14.07	Continuous readings
2160	6-7 Dec 06/ 0700-0700	Min.: 14.75 Max.: 16.27 Avg.: 15.61	Continuous readings	14.90	Collected @ 1000 hrs	14.37	Collected @ 1030 hrs	Min.: 13.98 Max.: 14.34 Avg.: 14.02	Continuous readings

Table B-3. Chlorine Contact Chamber (CCC) Effluent Total Residual Chlorine Concentrations.

Date/ Time	Pre-Dechli CCC Effluent Total (TRC) Conc (mg Bast CCC Effluent	Residual Chlorine entration*	WWTP Post- Dechlorination Effluent TRC Concentration (mg/L)
4 Dec 06	0.28	0.28	0.18
5 Dec 06	0.68	0.68	0.11
6 Dec 06	0.28	0.33	0.21

<sup>\*</sup>Residual chlorine was mistakenly measured prior to dechlorination

## APPENDIX C

WASHINGTON SURFACE WATER QUALITY TOXIC SUBSTANCE CRITERIA



## Water Quality Standards for Surface Waters of the State of Washington Chapter 173-201A WAC

Amended November 20, 2006

Washington State Department of Ecology

November 2006 Publication Number 06-10-091



blooms, toxic phytoplankton, or excessive aquatic plants, are examples of various sources of impairment. The following are examples of quantitative measures that a study may describe: Total phosphorus, total nitrogen, chlorophyll-a, dissolved oxygen in the hypolimnion if thermally stratified, pH, hardness, or other measures of existing conditions and potential changes in any one of these parameters.

- (b) Determine appropriate total phosphorus concentrations or other nutrient criteria to protect characteristic lake uses. If the existing total phosphorus concentration is protective of characteristic lake uses, then set criteria at existing total phosphorus concentration. If the existing total phosphorus concentration is not protective of the existing characteristic lake uses, then set criteria at a protective concentration. Proposals to adopt appropriate total phosphorus criteria to protect characteristic uses must be developed by considering technical information and stakeholder input as part of a public involvement process equivalent to the Administrative Procedure Act (chapter 34.05 RCW).
- (c) Determine if the proposed total phosphorus criteria necessary to protect characteristic uses is achievable. If the recommended criterion is not achievable and if the characteristic use the criterion is intended to protect is not an existing use, then a higher criterion may be proposed in conformance with 40 CFR part 131.10.
- (4) The department will consider proposed lake-specific nutrient criteria during any water quality standards rule making that follows development of a proposal. Adoption by rule formally establishes the criteria for that lake.
- (5) Prioritization and investigation of lakes by the department will be initiated by listing problem lakes in a watershed needs assessment, and scheduled as part of the water quality program's watershed approach to pollution control. This prioritization will apply to lakes identified as warranting a criteria based on the results of a lake-specific study, to lakes warranting a lakespecific study for establishing criteria, and to lakes requiring restoration and pollution control measures due to exceedance of an established criterion.

The adoption of nutrient criteria are generally not intended to apply to lakes or ponds with a surface area smaller than five acres; or to ponds wholly contained on private property owned and surrounded by a single landowner; and nutrients do not drain or leach from these lakes or private ponds to the detriment of other property owners or other water bodies; and do not impact designated uses in the lake. However, if the landowner proposes criteria the department may consider adoption.

(6) The department may not need to set a lake-specific criteria or further investigate a lake if existing water quality conditions are naturally poorer (higher TP) than the action value and uses have not been lost or degraded, per WAC 173-201A-260(1).

[Statutory Authority: Chapters 90.48 and 90.54 RCW, 03-14-129 (Order 02-14), § 173-201A-230, filed 7/1/03, effective 8/1/03.]

173-201A-240

Toxic substances.

(1) Toxic substances shall not be introduced above natural background levels in waters of the state which have the potential either singularly or cumulatively to adversely affect characteristic water uses, cause acute or chronic toxicity to the most sensitive biota dependent upon those waters, or adversely affect public health, as determined by the department.

- (2) The department shall employ or require chemical testing, acute and chronic toxicity testing, and biological assessments, as appropriate, to evaluate compliance with subsection (1) of this section and to ensure that aquatic communities and the existing and characteristic beneficial uses of waters are being fully protected.
- (3) The following criteria, found in Table 240(3), shall be applied to all surface waters of the state of Washington for the protection of aquatic life. The department may revise the following criteria on a statewide or water body-specific basis as needed to protect aquatic life occurring in waters of the state and to increase the technical accuracy of the criteria being applied. The department shall formally adopt any appropriate revised criteria as part of this chapter in accordance with the provisions established in chapter,34.05 RCW, the Administrative Procedure Act. The department shall ensure there are early opportunities for public review and comment on proposals to develop revised criteria. Values are μg/L for all substances except Ammonia and Chloride which are mg/L:

Table 240(3)
Toxics Substances Criteria

	Freshv	vater	Marine V	Vater
Substance	Acute	Chronic	Acute	Chronic
Aldrin/Dieldrin e	2.5a	0.0019b	0.71a	0.0019b
Ammonia (un-ionized NH3) hh	f,c	g,d	0.233h,c	0.035h,d
Arsenic dd	360.0c	190.0d	69.0c,II	36.0d,cc,ll
Cadmlum dd	l,c	J,d \	42.0c	9.3d
Chlordane	2.4a	0.0043b	0.09a	0.004b
Chloride (Dissolved) k	860.0h,c	230.0h,d		_
Chlorine (Total Residual)	19.0c	11.0d	13.0c	7.5d
Chlorpyrifos	0.083c	0.041d	0.011c	0.0056d
Chromium (Hex) dd	15.0c,l,ii	10.0d.jj	1,100.0c,1,11	50.0d,li
Chromium (Tri) gg	· m,c	n,d		tor
Copper dd	0,0	p,d	4.8c,il	3.1d,ll
Cyanide ee	22.0c	5.2d	1.0c,mm	d,mm
DDT (and metabolites)	1.1a	0.001b	0.13a	0.001b
Dieldrin/Aldrin e	2.5a	0.0019b	0.71a	0. <b>0019</b> b
Endosulfan	0.22a	0.056b	0.034a	0.0087b
Endrin	0.18a	0.0023b	0.037a	0. <b>002</b> 3b
Heptachlor	0.52a	0.0038b	0.053a	0.0036b
Hexachlorocyclohexane (Lindane)	2.0a	0.08b	0.16a	500
Lead dd	q,c	r,d	210.0c,ll	8.1d,II
Mercury s	2.1c,kk,dd	0.012d,ff	1.8c,ll,dd	0.025d,ff
Nickel dd	t,c	u,d	74.0c,II	8.2d,ll
Parathion	0.065c	0.013d	tes	Sec.
Pentachlorophenol (PCP)	w,c	. v,d	13.0c	7.9d
Polychlorinated Biphenyls (PCBs)	2.0b	0.014b	10. <b>0</b> b	0.030b
Selenium	20.0c,ff	5.0d,ff	290c,ll,dd	71.0d,x,ll,dd
Silver dd	y,a		1.9a,ll	80
Toxaphene	0.73c,z	0.0002d	0.21c,z	0.0002d
Zinc dd	aa,c	bb,d	90.0c,ll	81.0d,II

### Notes to Table 240(3):

a.	An instantaneous concentration not to be exceeded at any time.
b.	A 24-hour average not to be exceeded.
C.	A 1-hour average concentration not to be exceeded more than once every three years on the average.
d.	A 4-day average concentration not to be exceeded more than once every three years on the average.
e.	Aldrin is metabolically converted to Dieldrin. Therefore, the sum of the Aldrin and Dieldrin concentrations are compared with the Dieldrin criteria.
f.	Shall not exceed the numerical value in total ammonia nitrogen (mg N/L) given by:
	For salmonids present: $0.275 + 39.0 + 10^{PH-7.204}$

For salmonids present:  $0.275 + 39.0 + 10^{PH-7.204}$ 

For salmonids absent:  $\frac{0.411}{1 + 10^{7.204 + pH}} + \frac{58.4}{1 + 10^{pH - 7.204}}$ 

g. Shall not exceed the numerical concentration calculated as follows:

Unionized ammonia concentration for waters where salmonid habitat is an existing or designated use:

0.80 + (FT)(FPH)(RATIO)

where:

RATIO = 13.5;  $7.7 \le pH \le 9$ RATIO =  $(20.25 \times 10^{(7.7-pH)}) + (1 \cdot 10^{(7.4-pH)})$ ;  $6.5 \le pH \le 7.7$ FT = 1.4;  $15 \le T \le 30$ FT =  $10^{(0.03(20-T))}$ ;  $0 \le T \le 15$ FPH = 1;  $8 \le pH \le 9$ FPH =  $(1 + 10^{(7.4-pH)}) + 1.25$ ;  $6.5 \le pH \le 8.0$ 

Total ammonia concentrations for waters where saimonid habitat is not an existing or designated use and other fish early life stages are absent:

Chronic =  $\left(\begin{array}{cc} 0.0557 \\ 1+10^{7.888} \\ \end{array}\right)$  +  $\frac{2.487}{1+10^{9H-7.688}}$ 

where: A = the greater of either T (temperature in degrees Celsius) or 7.

Applied as a thirty-day average concentration of total ammonia nitrogen (in mg N/L) not to be exceeded more than once every three years on average. The highest four-day average within the thirty-day period should not exceed 2.5 times the chronic criterion.

Total ammonia concentration for waters where salmonid habitat is not an existing or designated use and other fish early life stages are present:

(B) Chronic criterion where: B = the lower of either 2.85, or 1.45 x  $10^{0.028 \times (25-T)}$ T = temperature in degrees Celsius. Applied as a thirty-day average concentration of total ammonia nitrogen (in mg N/L) not to be exceeded more than once every three years on the average. The highest four-day average within the thirty-day period should not exceed 2.5 times the chronic criterion. Measured in milligrams per liter rather than micrograms per liter. h. ١. ≤ (0.944)(e(1.128[in(hardness)]-3.828)) at hardness =100. Conversion factor (CF) of 0.944 is hardness dependent. CF is calculated for other hardnesses as follows: CF = 1.136672 - [(in hardness)(0.041838)]. ≤ (0.909)(e(0.7852[In(hardness)]-3.490)) at hardness =100. Conversions factor (CF) of 0.909 is hardness dependent. CF is calculated for other hardnesses as follows: CF = 1.101672 - [(in hardness)(0.041838)]. k. Criterion based on dissolved chloride in association with sodium. This criterion probably will not be adequately protective when the chloride is associated with potassium, calcium, or magnesium, rather than sodium. ĺ. Salinity dependent effects. At low salinity the 1-hour average may not be sufficiently protective.  $\leq (0.316)e^{(0.8190[\ln(\text{hardness})] 3.888)}$ m.  $\leq (0.860)e^{(0.8190[\ln(\text{hardness})] 1.561)}$ n.  $\leq (0.960)(e^{(0.9422[\ln(\text{hardness})] \cdot 1.464)})$  $\leq (0.960)(e^{(0.8545[\ln(hardness)] \cdot 1.465)})$ p.  $\leq$  (0.791)(e<sup>(1,273] In(hardness)] - 1,460)</sup>) at hardness = 100. Conversion factor (CF) of 0.791 is hardness q. dependent. CF is calculated for other hardnesses as follows: CF = 1.46203 - [(in hardness)(0.145712)).  $\leq$  (0.791)(e<sup>(1.273[In(hardness)]-4.705)</sup>) at hardness = 100. Conversion factor (CF) of 0.791 is hardness r. dependent. CF is calculated for other hardnesses as follows; CF = 1.46203 - [(In hardness)(0.145712)]. If the four-day average chronic concentration is exceeded more than once in a three-year period, the edible portion of the consumed species should be analyzed. Said edible tissue concentrations shall not be allowed to exceed 1.0 mg/kg of methylmercury.  $\leq (0.998)(e^{(0.8480[\ln(hardness)] 3.3812)})$ ŧ. ≤ (0.997)(e<sup>(0.8460[ in(hardness)] 1.1645)</sup>)

٧.	$\leq e^{(1.005(pH)-5.290)}$
ŵ.	≤ e <sup>[1.005(pH)-4.530]</sup>
x.	The status of the fish community should be monitored whenever the concentration of selenium exceeds 5.0 ug/l in salt water.
у.	$\leq (0.85)(e^{(1.72[ln(hardness)]-6.52)})$
Z.	Channel Catfish may be more acutely sensitive.
aa.	≤ (0.978)(e <sup>(0.8473[in(hardness)) 0.8604]</sup> )
bb.	≤ (0.986)(e <sup>(0.8473[in(hardness)] 0.7614)</sup> )
cc.	Noniethal effects (growth, C-14 uptake, and chlorophyll production) to diatoms ( <i>Thalassiosira aestivalis</i> and <i>Skeletonema costatum</i> ) which are common to Washington's waters have been noted at levels below the established criteria. The importance of these effects to the diatom populations and the aquatic system is sufficiently in question to persuade the state to adopt the USEPA National Criteria value (36 µg/L) as the state threshold criteria, however, wherever practical the ambient concentrations should not be allowed to exceed a chronic marine concentration of 21 µg/L.
dd.	These ambient criteria in the table are for the dissolved fraction. The cyanide criteria are based on the weak acid dissociable method. The metals criteria may not be used to calculate total recoverable effluent limits unless the seasonal partitioning of the dissolved to total metals in the ambient water are known. When this information is absent, these metals criteria shall be applied as total recoverable values, determined by back-calculation, using the conversion factors incorporated in the criterion equations. Metals criteria may be adjusted on a site-specific basis when data are made available to the department clearly demonstrating the effective use of the water effects ratio approach established by USEPA, as generally guided by the procedures in USEPA Water Quality Standards Handbook, December 1983, as supplemented or replaced by USEPA or ecology. Information which is used to develop effluent limits based on applying metals partitioning studies or the water effects ratio approach shall be identified in the permit fact sheet developed pursuant to WAC 173-220-060 or 173-226-110, as appropriate, and shall be made available for the public comment period required pursuant to WAC 173-220-050 or 173-226-130(3), as appropriate. Ecology has developed supplemental guidance for conducting water effect ratio studies.
ee.	The criteria for cyanide is based on the weak acid dissociable method in the 17th Ed. Standard Methods for the Examination of Water and Wastewater, 4500-CN I, and as revised (see footnote dd, above).
ff.	These criteria are based on the total-recoverable fraction of the metal.
gg.	Where methods to measure trivalent chromium are unavailable, these criteria are to be represented by total-recoverable chromium.
hh.	The listed fresh water criteria are based on unionized or total ammonia concentrations, while those for marine water are based on total ammonia concentrations. Tables for the conversion of total ammonia to un-ionized ammonia for freshwater can be found in the USEPA's Quality Criteria for Water, 1986. Criteria concentrations based on total ammonia for marine water can be found in USEPA Ambient Water Quality Criteria for Ammonia (Saltwater)-1989, EPA440/5-88-004, April 1989.

II. Th	ne conversion factor used to calculate the dissolved metal concentration was 0.982.
J. Th	ne conversion factor used to calculate the dissolved metal concentration was 0.962.
kk. Th	ne conversion factor used to calculate the dissolved metal concentration was 0.85.

II. Marine conversion factors (CF) which were used for calculating dissolved metals concentrations are given below. Conversion factors are applicable to both acute and chronic criteria for all metals except mercury. The CF for mercury was applied to the acute criterion only and is not applicable to the chronic criterion. Conversion factors are already incorporated into the criteria in the table. Dissolved criterion = criterion x CF

CF
1.000
0.994
0.993
0.83
0.951
0.85
0.990
0.998
0.85
0.946

mm. The cyanide criteria are: 2.8µg/i chronic and 9.1µg/i acute and are applicable only to waters which are east of a line from Point Roberts to Lawrence Point, to Green Point to Deception Pass; and south from Deception Pass and of a line from Partridge Point to Point Wilson. The chronic criterion applicable to the remainder of the marine waters is I µg/L.

- (4) USEPA Quality Criteria for Water, 1986, as revised, shall be used in the use and interpretation of the values listed in subsection (3) of this section.
- (5) Concentrations of toxic, and other substances with toxic propensities not listed in subsection (3) of this section shall be determined in consideration of USEPA Quality Criteria for Water, 1986, and as revised, and other relevant information as appropriate. Human health-based water quality criteria used by the state are contained in 40 CFR 131.36 (known as the National Toxics Rule).
- (6) Risk-based criteria for carcinogenic substances shall be selected such that the upper-bound excess cancer risk is less than or equal to one in one million.

[Bisiutory Authority: Chapters 90.48 and 90.54 RCW. 03-14-129 (Order 02-14), amended and recodified as § 173-201A-240, filed 7/1/03, effective 8/1/03. Statutory Authority: Chapter 90.48 RCW and 40 CFR 131. 97-23-064 (Order 94-18), § 173-201A-040, filed 11/18/97, effective 12/19/97. Statutory Authority: Chapter 90.48 RCW. 92-24-037 (Order 92-29), § 173-201A-040, filed 11/25/92, effective 12/26/92.]

#### Notes:

Reviser's note: The brackets and enclosed material in the text of the above section occurred in the copy filed by the agency.

## 173-201A-250 Radioactive substances.

- (1) Deleterious concentrations of radioactive materials for all classes shall be as determined by the lowest practicable concentration attainable and in no case shall exceed:
  - (a) 1/12.5 of the values listed in WAC 246-221-290 (Column 2, Table II, effluent concentrations, rules and regulations for radiation protection); or
  - (b) USEPA Drinking Water Regulations for radionuclides, as published in the Federal Register of July 9, 1976, or subsequent revisions thereto.
- (2) Nothing in this chapter shall be interpreted to be applicable to those aspects of governmental regulation of radioactive waters which have been preempted from state regulation by the Atomic Energy Act of 1954, as amended, as interpreted by the United States Supreme Court in the cases of Northern States Power Co. v. Minnesota 405 U.S. 1035 (1972) and Train v. Colorado Public Interest Research Group, 426 U.S. 1 (1976).

[Statutory Authority: Chapters 90.48 and 90.54 RCW. 03-14-129 (Order 02-14), recodified as § 173-201A-250, filed 7/1/03, effective 8/1/03. Statutory Authority: Chapter 90.48 RCW and 40 CFR 131. 97-23-064 (Order 94-19), § 173-201A-050, filed 11/18/97, effective 12/19/97. Statutory Authority: Chapter 90.48 RCW. 92-24-037 (Order 92-29), § 173-201A-050, filed 11/25/92, effective 12/26/82.]

#### 173-201A-260

Natural conditions and other water quality criteria and applications.

- (1) Natural and irreversible human conditions.
  - (a) It is recognized that portions of many water bodies cannot meet the assigned criteria due to the natural conditions of the water body. When a water body does not meet its assigned criteria due to natural climatic or landscape attributes, the natural conditions constitute the water quality criteria.
  - (b) When a water body does not meet its assigned criteria due to human structural changes that cannot be effectively remedied (as determined consistent with the federal regulations at 40 CFR 131.10), then alternative estimates of the attainable water quality conditions, plus any further allowances for human effects specified in this chapter for when natural conditions exceed the criteria, may be used to establish an alternative criteria for the water body (see WAC 173-201A-440).
- (2) **Toxics and aesthetics criteria.** The following narrative criteria apply to all existing and designated uses for fresh and marine water:
  - (a) Toxic, radioactive, or deleterious material concentrations must be below those which have the potential, either singularly or cumulatively, to adversely affect characteristic water uses, cause acute or chronic conditions to the most sensitive biota dependent upon those waters, or adversely affect public health (see WAC 173-201A-240, toxic substances, and 173-201A-250, radioactive substances).

- (b) Aesthetic values must not be impaired by the presence of materials or their effects, excluding those of natural origin, which offend the senses of sight, smell, touch, or taste (see WAC 173-201A-230 for guidance on establishing lake nutrient standards to protect aesthetics).
- (3) Procedures for applying water quality criteria. In applying the appropriate water quality criteria for a water, the department will use the following procedure:
  - (a) The department will establish water quality requirements for water bodies, in addition to those specifically listed in this chapter, on a case-specific basis where determined necessary to provide full support for designated and existing uses.
  - (b) Upstream actions must be conducted in manners that meet downstream water body criteria. Except where and to the extent described otherwise in this chapter, the criteria associated with the most upstream uses designated for a water body are to be applied to headwaters to protect nonfish aquatic species and the designated downstream uses.
  - (c) Where multiple criteria for the same water quality parameter are assigned to a water body to protect different uses, the most stringent criterion for each parameter is to be applied.
  - (d) At the boundary between water bodies protected for different uses, the more stringent criteria apply.
  - (e) In brackish waters of estuaries, where different criteria for the same use occurs for fresh and marine waters, the decision to use the fresh water or the marine water criteria must be selected and applied on the basis of vertically averaged daily maximum salinity, referred to below as "salinity."
    - (i) The fresh water criteria must be applied at any point where ninety-five percent of the salinity values are less than or equal to one part per thousand, except that the fresh water criteria for bacteria applies when the salinity is less than ten parts per thousand.
    - (ii) The marine water criteria must apply at all other locations where the salinity values are greater than one part per thousand, except that the marine criteria for bacteria applies when the salinity is ten parts per thousand or greater.
  - (f) Numeric criteria established in this chapter are not intended for application to human created waters managed primarily for the removal or containment of pollution. This special provision also includes private farm ponds created from upland sites that did not incorporate natural water bodies.
    - (i) Waters covered under this provision must be managed so that:
      - (A) They do not create unreasonable risks to human health or uses of the water.
      - (B) Discharges from these systems meet down gradient surface and ground water quality standards.

- (ii) This provision does not apply to waterways designed and managed primarily to convey or transport water from one location to another, rather than to remove pollution en route.
- (g) When applying the numeric criteria established in this chapter, the department will give consideration to the precision and accuracy of the sampling and analytical methods used, as well as the existing conditions at the time.
- (h) The analytical testing methods for these numeric criteria must be in accordance with the "Guidelines Establishing Test Procedures for the Analysis of Pollutants" (40 CFR Part 136) or superseding methods published. The department may also approve other methods following consultation with adjacent states and with the approval of the USEPA.
- (i) The primary means for protecting water quality in wetlands is through implementing the antidegradation procedures described in Part III of this chapter.
  - (i) in addition to designated uses, wetlands may have existing beneficial uses that are to be protected that include ground water exchange, shoreline stabilization, and storm water attenuation.
  - (ii) Water quality in wetlands is maintained and protected by maintaining the hydrologic conditions, hydrophytic vegetation, and substrate characteristics necessary to support existing and designated uses.
  - (iii) Wetlands must be delineated using the Washington State Wetlands Identification and Delineation Manual, in accordance with WAC 173-22-035.

[Statutory Authority: Chapters 90.48 and 90.54 RCW. 03-14-129 (Order 02-14), § 173-201A-280, flied 7/1/03, effective 8/1/03.]

APPENDIX D

SLUDGE SAMPLING RESULTS AND EVALUATION

# SLUDGE SAMPLING RESULTS AND EVALUATION WWTP PERFORMANCE EVALUATION 29 NOVEMBER - 7 DECEMBER 2006 SOLO POINT WASTEWATER TREATMENT PLANT FORT LEWIS, WASHINGTON

- 1. Sludge Data. A summary of detected parameters and their concentrations in sludge samples is provided in Table D-1.
- a. Metals concentrations were consistent with concentrations detected in Solo Point biosolids samples analyzed by Anatek Labs, Inc. in July 2003, April 2005, and June 2005. Metals concentrations in digested sludge samples were below the ceiling concentration limits (of WAC 173-308-160) for biosolids applied to land.
- b. TPH concentrations were consistent with concentrations detected in biosolids samples analyzed by Anatek Labs, Inc. in July, August and September 2006. TPH was detected in digested sludge samples at concentrations of 26,000 mg/kg (estimated) and 16,500 mg/kg of total solids. Lube oil range TPH was detected in samples collected by Fort Lewis from Fort Lewis composted biosolid piles on 31 July 2006 and analyzed by Anatek Labs, Inc.; concentrations ranged from 270 to 2390 mg/kg. The TPH data suggest that some heavier components of TPH persist through the anaerobic digestion and composting processes.
- c. Total solids and total volatile solids concentrations in thickener sludge and secondary digester sludge were virtually the same as the averages calculated with 2006 Solo Point WWTP data (see Table F-4).
- 2. Evaluation of Sludge Thickness and Volatile Solids Reduction Data.
- a. Approximately 16,000 gpd of thickened sludge was pumped from the thickener to the primary digester. The thickener produced sludge with a total solids concentration of ~3.2 percent with a total volatile solids component of 83 percent, based on 2006 WWTP data.
- b. Typical unthickened and thickened primary sludges have solids concentrations of 2-6 percent and 5-10 percent, respectively. No data was available on the percent solids in the WWTP primary sludge (unthickened); however, it is evident from the low percent solids (3.2 percent) of the thickened primary sludge that unthickened primary sludge was "thin," probably about 1 percent or less. A thin sludge may needlessly overburden downstream sludge handling processes.
- c. It should be noted that primary sludge, secondary sludge, and "dilution water" pumps were operated continuously and at constant rates, resulting in excessive flow (estimated at  $\sim 1.54$  mgd) to the sludge thickener and excessive thickener supernatant return flow to the head of the WWTP. At the estimated flow rate of 1.54 mgd (see Table 3) the thickener has a surface overflow rate of 969 gal/ft²-day, which exceeds the recommended maximum hydraulic overflow

rate range (380 to 760 gal/ft²-day) (Metcalf and Eddy 2003). This volume (~1.54 mgd) is returned to the primary clarifier influent as supernatant.

- d. Sludge was digested in a two-stage anaerobic process consisting of up to two mixed, heated primary digesters followed by one unheated secondary digester. Only one primary digester was in service at the time of sampling. The other digester was out of service for cleaning and maintenance. Approximately 16,000 gal/day of raw sludge was pumped to the 460,000 gallon primary digester. The primary digester provided approximately 29 days of residence time. In 2006, the primary digester was heated to a minimum temperature of 35 °C (95 °F). When in service, the other primary digester (800,000 gallons) would provide 50 days of residence time. The secondary digester (460,000 gals) provided approximately 29 days of residence time. In 2006, the secondary digester temperature was a minimum of 29 °C. Supernatant (estimated at ~16,000 gal/day by WWTP personnel) from the secondary digester was returned by gravity to the primary clarifier influent. The digesters produced biosolids with a total solids concentration of 4.7 percent with a total volatile solids component of 67 percent, based on 2006 Solo Point WWTP data. On average, the Solo Point digesters reduced volatile solids by about 37 percent. Digesters are typically designed to reduce volatile solids by 38 50 percent.
- e. The Fort Lewis WWTP has the ability to produce biosolids that can meet the Class B biosolids criteria of WAC 173-308. The combination of residence time and temperature (≥35 °C) in the primary digester meets the Class B biosolids pathogen reduction requirements of WAC 173-308-170, which requires values for the mean cell residence time and temperature to be between fifteen days at 35 to 55 °C and sixty days at 20 °C. The vector attraction requirements may be met by incorporating the biosolids into the soil during land application or by one of the six methods described in WAC 173-308-180.
- f. Controlling sludge pumping based on primary and secondary clarifier sludge solids concentrations would result in lower hydraulic load on the thickener and primary clarifier (i.e., lower return volumes) and lower dilution water volumes. This would likely result in: improved primary clarifier performance, thicker primary sludge, lower sludge volumes sent to digesters, lower digester supernatant volumes, improved digester removal of volatile solids, increased gas production, decreased heating requirements, and higher quality biosolids drawn to drying beds. Sludge pumping control would require the intermittent pumping of sludge and may require intermittent operation of primary clarifier sludge collectors. The process goal would be to find a blanket or sludge hopper level that provides a thick sludge without overloading collectors or allowing decomposition of the settled sludge.
- g. The quantity of sludge to be removed from the primary clarifier can be estimated with the influent and effluent total suspended solids (from Appendix D, Table D-2, page D-5), the percentage of dry solids in the primary sludge and the wastewater flow:

Dry solids removed (lbs) = (influent-effluent TSS, mg/L)X(Wastewater flow, mgd)X(8.34 lb/gal) =  $(6462 - 1827 \text{ mg/L}) \text{ X} \sim 3 \text{ mgd X} 8.34 \text{ lbs/gal} = 4635 \text{ lbs}$ 

Wet sludge removed, gal/day = [dry solids removed, lbs/day X (100/dry solids in sludge,%)]/8.34 lbs/gal

Assume dry solids in sludge = 1%

- = [4635 lbs X 100/1]/8.34
- = 55,576 gallons

The actual sludge pumping volume is estimated at ~420,000 gal/day.

Table D-1. Solo Point WWTP Sludge Data.

Analyte	Date	Sample Type	Thickener Sludge	Pfimary Digester Sludge	Secondary Digester Sludge	Sludge from Drying Bed
Total Solids (%)	6-Dec-06	grab	3.2	1.8	4.7	14.9
Total Volatile Solids (%)	6-Dec-06	grab	83	74	67	49
TPH	S. F. Walle W. L.		The North Armed A			- 5-1 (3-44.2.W)
TPH-Diesel Range (mg/kg-dry)	6-Dec-06	grab	9100.0	ND (<3300)	ND (<3200)	2500
TPH-Heavy Range (mg/kg-dry)	6-Dec-06	grab	9300J	22000J	26000J	14000
Metals (mg/kg-dry)				A Million Andrews		
Aluminum	6-Dec-06	grab	8000	7200.0	13000	15000
Arsenic	6-Dec-06	grab	3.6	ND (<3.7)	5.3	5.4
Cadmium	6-Dec-06	grab	4.7	4.8	6.9	6.8
Chromnim	6-Dec-06	grab .	27	26.0	34	37
Copper	6-Dec-06	grab	570	490.0	780	670
lion .	6-Dec-06	grab	7900	6900.0	11000	15000
Lead	6-Dec-06	grab	38	36.0	61	73
Mercury	6-Dec-06	grab	1.5	2.3	3.7	2.6
Molybdenum	6-Dec-06	grab	ND (<34)	ND (<47)	ND (<19)	14
Nickel	6-Dec-06	grab	12	11.0	21	24
Selenium	6-Dec-06	grab	8.1	<9.3	9	7.7
Silver	6-Dec-06	grab	14	14.0	11	8.4
Zinc ,	6-Dec-06	grab	1100.0	930.0	1500	1300

J: Estimated value ND: not detected

APPENDIX E WWTP PROCESS DATA SUMMARY

Table E-1. WWTP Process Data - WWTP Removal Efficiencies.

Analyte	Date	Time	WWIP Influent (TPIN) Cope.	WWIP Influent (IPIN) Flow (mgd)	WWTP influent (TPIN) Mess (lbs/dey)	WWTP Efficient (TPBF) Conc	WWTP Efficient (TPEF) /Flow (mgd)	WWTP Efficient (IPEF) Mess (libs/day)	WWTP RemEffic. (%)	WWTP Mass Removed (lbs/day)
BOD	4-5 Dec 06 5-6 Dec 06	FC FC	78	2.45	1593.77 Data dispersed of	9.3 un to Unsatisfacto	2,45	190.03 A/OC findings	88.1	1403.75
(mg/L)	6-7 Dao 06	FC			Data discarded o	ue to unsatisfacto	ry laboratory Q	A/QC findings	- November 1	
TSS	4-5 Dec 06 5-6 Dec 06	FC FC	54 b 98 b	2.45	1103.38	20 24.7	2.45 2.46	408.66 506.76	63.0 74.8	694.72 1503.85
(mg/L)	6-7 Dec 06	FC	204	2.59	4406.52	26.4	2.59	570.26	87.1	3836.27
	4-5 Dec 06	FC	24	2.45	2506.84 490.39	3.5	2,50	495.22 71.52	80.2 85.4	2011.61 418.88
Ammonia	5-6 Dec 06	FC	25	2.46	512.91	4.5	2.46	92.32	82.0	420.59
(mg/L)	6-7 Dec 06 Average	FC	26 25	2.59	561.62 521.64	5,8	2.59 2.50	96.37	77.7 8).5	436.33 425.26
	4-5 Dec 06	FC	ND(<0.050)	2.45	0.51	26	2.45	408.66	-79900.0	-40B.15
Nitrate/Nitrite (mg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	ND(<0.050) ND(<0.050)	2.46	0.51	21	2.46	430.84 518.41	-83900.0 -95900.0	-430.33 -517.87
	Average		ND(<0.050)	2.50	0.52		2.50	452.64	-86737.3	-452.12
TKN	4-5 Dec 06 5-6 Dec 06	FC FC	29 37	2.45	592.56 759.11	8.1	2.45	136.90 166.18	76.9 78.1	455.66 592.92
(mg/L)	6-7 Dec 06 Average	FC	39 35	2.59	731.36	8.8	2.59	190.09	77.4	652.34 566.97
	4-5 Dec 06	FC	3.61	2.45	73.76	3.72	2,45	76.01	-3.0	-2.25
Total Phosphurus (mg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	4,2 4,8	2.46 2.59	86.17 103.68	4.34 4.54	2.46 2.59	89.04 98.07	-3,3 5,4	-2.87 5.62
(	Average		4	2.50	67.87	7,57	2.50	87.71	0.2	0.17
Grease and Oil	4-5 Dec 06 5-6 Dec 06	grab grab	7.79	2.45 2.46	429.09 159.82	ND (<5.30) ND (<5.00)	2.45 2.46	54.15 51.29	87.4 57.9	374.95 108.53
(mg/L)	6-7 Dec 06	grab	6.33	2.59	136.73	ND(<5.10)	2.59	55.08	59.7	81.65
	Average 4-Dec-06	grab	12	2.50 2.45	241.88 306.50	690	2.50 2.45	53.51 14.10	77.9	188.38
IPH-Diasel Range	5-Dec-06	grab	12000	2.46	246.20	830	2.46	17.03	93.1	229.17
(ppb)	6-Dec-06 Average	grab	18000	2.59 2.50	388.81 313.83	4000	2.59 2.50	86.40 39.18	77.8 87.5	302.41 274.66
siz.	4-Dac-06	greb	11000	2.45	224.76	1600	2.45	32.69	85.5	192.07
PH-Heavy Range (ppb)	5-Dec-06 6-Dec-06	grab grab	72003 110003	2.46	147.72 237.61	1600 6900	2.46 2.59	32.83 149.04	77.8 37.3	114.89 88.56
I'm	Average		11000	2.50	203.36	S 1 A 2 D 2 D 2 D 2 D 2 D 2 D 2 D 2 D 2 D 2	2.50	71.52	64.8	131.84
TPH-Gasoline	4-Dec-06 5-Dec-06	grab grab	280 140	2.45	5.72 2.87	ND(<48) ND(<48)	2.45	0.49	91.4 82.9	2.38
(ppb)	6-Dec-06 Average	grab	150J 210	2.59 2.50	3.24 3.94	ND(<48)	2.59 2.50	0.52	84.0 87.3	3.44
	4-5 Dec 06	FC	0.208	2.45	4.250	0.243	2.45	4.965	-16,8	-0.715
Aluminum (mg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	0.291	2.46 2.59	5.970 11.816	0.252 0.246	2,46 2,59	5,170 5,314	13.4 55.0	6.502
(mg ~)	Average		0,547	2,50	7,345	3.210	2.50	5.150	29.9	2.196
Aratnio	4-5 Dec 06 5-6 Dec 06	FC FC	ND(<1.00)	2.45	0.010	1.03	2,45 2.46	0.021	-106.0 -1.7	-0.011
(µg/L)	6-7 Dec 06	FC	ND(<2.00)	2.59 2.50	0.022 0.018	ND(<2.00)	2.59 2,50	0.022	-20.3	0.000
	Avenge 4-5 Dec 06	FC	ND(<2.00)	2.45	0.020	ND(<2.00)	2.45	0.020	0.0	0.000
Cadmium	5-6 Dec 06 6-7 Dec 06	FC FC	ND(<2.00) 1.06	2.46 2.59	0.021	ND(<2.00) ND(<1.00)	2.46 2.59	0.021	0.0 52.8	0.000
(µg/L)	Average		1 1	2.50	0.021	AB(41.60)	2.50	0.017	18.9	0.004
Caloium	4-5 Dec 06 5-6 Dec 06	FC FC	16.9	2.45 2.46	345.318 371.347	16.6 18.4	2.45 2.46	339.188 377.502	1.B -1.7	6.130 -6.155
(mg/L)	6-7 Dec 06	FC	19.3	2.59	416.892	18.9	2.59	408,251	2.1	8,640
	Average 4-5 Dec 06	FC	2,50	2.50	377.852 0.053	ND(<2.00)	2,50	374.980 0,020	D.8	0.032
Chromium	5-6 Dec 06	FC	ND(<2.00)	2.46	0.021	ND(<2.00)	2,46	0.021	0.0	0.000
(We/L)	6-7 Dec 06 Average	FC	2.38	2.59	0.051	ND(<2.00)	2.59 2.50	0.022	58.0 49.9	0.030
(3 full) 1 (798) 1	4-5 Dec 06	FC	45,8	2.45	0,936	32.7	2,45	0.568	28.6	0.268
Copper (µg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	51.3 78.5	2,46 2.59	1.052	36.7	2.46 2.59	0.753 0.752	28.5 55.7	0.300
Figure	Average		59	2.50	1.228	-	2.50	6.724	41.0	0.504
Iron	4-5 Dec 06 5-6 Dec 06	FC FC	0,362	2.45 2.46	7.397 6.914	0,269	2.45 2.46	5,496 5,293	25.7 23.4	1.900
(ting/L.)	6-7 Dec 06 Average	FC	0.558	2.59	12.053 8.788	0.258	2.59	5,573 5,454	33.8 37.9	3.334
	4-5 Dec 06	FC	1.28	2.45	0.026	3.37	2.45	0.069	-163.3	-0.04
Lend (µg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	ND(<5.00)	2.46	0.025 0.034	1,05 ND(<5.00)	2.46	0.022	0.0	0.003
	Average		i	2.50	0.035		2,50	0.048	-37.3	-0.01
Magnosium	4-5 Dec 06 5-6 Dec 06	FC	5.52	2.45	108.794 115.507	5.24 5,64	2.45	107,069	1.5 -0.2	1.63 -0.20
(mg/L)	6-7 Dec.06 Average	FC	5.74	2.59	123.987 116.066	5.66	2,59 2,50	122.259 115.014	1.4	1.05
	4-5 Dec 06	FC	ND(<0.200)	2.45	0.002	ND(<0.200)	2.45	0.002	0.0	0.00
Meroury: (µg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	ND(<0,200) 0.297	2.46	0.002	ND(<0.200) ND(<0.200)	2.46	0.002	66.3	0.00
· · · · · · · · · · · · · · · · · · ·	Average		0	2.50	0.004		2.50	0.002	40.5	0.00
Molybdenum	4-5 Dec 06 5-6 Dec 06	PC PC	12.4	2,45	0.253 0.228	9.91	3.45 2.46	0,116	54.3 10.7	0.13
(μ <sub>β</sub> /L.)	6-7 Dec 06	FC	23,3	2.59	0.503	10.8	2.59	0.233	53.6	0.27
	4-5 Dec 06	FC	11.2	2.50	0.328 0.229	2.45	2.50	0.184	78.1	0.14
Nickel	5-6 Dec 06	FC	6.93	2.46	0.142	3.64	2.46	0.054	61.9	80.0
(h8/L)	6-7 Dec 06 Average	FC	6.56 8	2.59	0,142	ND(<2.00)	2.59 2.50	0.022	84.8 75.5	0.12
Polar:	4-5 Dec 06	FC FC	ND(<1.00)	2.45	0,010	MD(<1.00)	2.45	0,010	0,0	9,00
Selenium (µg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	ND(<1.00) ND(<2.00)	2.46 2.59	0.010	ND(<1,00) ND(<2.00)	2.46	0.010	0.0	0.00
	Average		ND	2.50	0.014		2.50	0.014	0.0	0.00
Silver	4-5 Dec 06 5-6 Dec 06	FC FC	ND(<1.00) ND(<1.00)	2.45 2.46	0.010	ND(<1.00) ND(<1.00)	2.45 2.46	0.010	0.0	0.00
(μg/L)	6-7 Dac 06 Average	FC	ND(<1.00) ND	2.59 2.50	0.011	ND(<1.00)	2,59 2,50	0.011	0.0	0.00
1.	4-5 Dec 06	FC	0.08	2.45	1.635	0.07	2.45	1,430	12.5	0.20
Zinc (mg/L)	5-6 Dec 06 6-7 Dec 06	FC FC	0.095 0.135	2.46	1.949 2.916	0.079	2.46 2.59	1.621 2.419	16.B 17.0	0.32
(100/10)	Average		0.133	2.50	2.167		2,59	1.823	15.8	0.49

FC: 24-hour flow composite collected from approximately 0700 – 0700 hrs

a: Removal efficiency and mass removed calculated with ½ the method reporting limit for ND results.

b: A review of headworks TSS mass inputs and outputs (assuming 0% or more influent TSS removal in preliminary treatment) suggests that the first and second day WWTP influent sample results for TSS appear to be erroneously low. The analysis suggests that day 1 and 2 influent TSS concentrations should be ≥201 mg/L and ≥163 mg/L.

respectively; thus the data suggests that day 3 data best represents the TSS removal efficiency (-87%) of the WWTP. Problems were noted during day 1 of sampling associated with rags elogging the sample intake strainer, which may have impacted WWTP influent sample quality. Therefore, the WWTP TSS removal efficiency will be reported as ≥ 80.2 percent.

Table E-1. WWTP Process Data - WWTP Removal Efficiencies (continued).

Married   Trans											
Chancelors		ATTACK TOTAL LANGER	Time	Inflient (TPIN)	Influent (TPIN) Flow	influent (TPDI) Mars	(TPEF)	Effluent (TPEF) Flow	Effluent (TPEF) Mass	Rem Effic. (%)	Mass Removed
Decided   main   MO			San Barata	N 30 2 - 0 1	15 1 W 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2 1 1 7%	11.7.2 3.7711		745 725 T	Z	1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1
Company   Comp	Chloroform		grab		2.45	0.000	ND	2.45			NA.
Company   Comp	(美国建筑图集)		grad		2.46				0.000	ND I	- NA
	1. 在2000年2月 1					0.000				ND	NA.
Company   Comp	1 4-dichlorobenzene		areh	21	245	0.041	ND.	1.45	0.000	Annual Assessment Company	Account the Contract of the Co
Color   Colo			gnab	3)	2.46				0.000		NA.
Color	· 人名斯利特尔 5.5					0.043		2.59	0.000		
Special Content		Average								ND	NA
G. De-Col.   June   1.   2.59   0.360   ND   1.59   0.000   ND   NA		4-Dec-06			2,45					ND	NA
Company   Comp	(HVD)		grab								
Company   Comp			RIMO	42	2,39	0.086	ND	2.39	0,000		
1.   1.   1.   1.   1.   1.   1.   1.	Take William Okasa								0.000	THE REPORT OF SAME PARTY OF SAME	
Check			anab anah				ND ND				
Tologon   Advance	44. Figure 1971	6-Dec-06	grab	ND	2.59	0,000	ND	2,59		ND	NA
Comparison   Com		Average									
SPICE   American   Spice   S			grab		2.45	0.041	ND	2.45			
PRODE   Average   NED   MA   MA   MA   MA   MA   MA   MA   M	(HB/L)	5-Dec-06	grab	2.1	2.46	0.041		2.46	0.000	מא	
Part	三人类的原理 连二人		grab	3)	2.59	0.065	ND	2.59	0.000	ND ND	NA NA
Pippop	SNOCI	Average	A 50 (50) 92mm 192	117-11 <b>23</b> 10-201	400000000000000000000000000000000000000	51-78 S207 S	7 25025030000	12.35 (1)25.02 (1)4		Figure 1 and	
S.   Dec 16			0700-0700	6	2.45	0.123	ND	2.45	0,000		NA .
Apert   Aper	CHANGE	5-6 Dec 06	0700-0700	24	2.46	0.492	ND	2.46 -	0.000	ND	
Accept@dens			0700-0700	11	2.59	0,238	ND	2.59	0.000		
3-6 Dec 06   0760-0700   0.41   2.46   0.006   ND   2.46   0.000   ND   NA	A 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	The same of the sa	USA BEAR OF THE		C 10 10 10 10 10 10 10 10 10 10 10 10 10	Section 1981	7 15 15 march 12 15 15 15 15 15 15 15 15 15 15 15 15 15				E. Harrison, Services Street, Street, St.
Color   Page	Acenaptitions	4-5 Dec 06	0700-0700	0.51	2.45		ND ND	2.45	000,0	ND	
Philipping   4-5 pec   0   0   0   0   0   0   0   0   0	<b>能对解键的方法</b> 。	6-7 Dec 06		ND			ND I	2.40	0.000		
Patry Politicing   4-5 Dec 06	in confidence of		1			0.000	1755				
## 3-6 Dec 66	Distrivishthalete		0700-0700	41		0.082	NO	2.45	0.000	ND	T NA
Average   ND   NA		5-6 Dec 96	0700-0700		2.46				0.000	ND	NA.
44-5  Dec 06	的复数加拉尔 图	6-7 Dec 06		5					0.000	MD	NA.
S-6   Dec   6   6760-6770   21   2.46   0.041   ND   2.46   0.000   ND   NA	EF AND BUILDING CO.		1		THE STREET	The manifest exists the		and the second second	1110000	THE PERSON NAMED OF THE PARTY O	THE RESIDENCE OF THE PARTY OF T
6-7   De 66   0700-0700   1   2.19   D.022   NID   2.59   D.000   NID   NA	dimibutylphtärlika								0.000	ND	
THINNING		5-6 Dec 06			2.46	0.041		2.46			
A. Dee 66		AVersos	0 /00-0 /00	1	2,59	0.022	MD	2,39	0.000		
Section   100	TANK PRINCIPLE STREET		0200 0200	0.41	- San	10000	the same state of the	2.45	0.000	APPLE DOMESTICATION OF THE PARTY.	
Section   Company   Comp	THU INC.										
No.   No.		6-7 Dac 06	0700-0700	0.43	2.59	0.009	NEO	2.59			
See   Dec   66   0760-0700   7   2.46   0.1144   ND   2.46   0.000   ND   NA	SS # ALTONOUS TO	Average				1			A STANCE OF THE		J NA
See   Dec   66   0760-0700   7   2.46   0.1144   ND   2.46   0.000   ND   NA	Buty benzylphthalate 4				2.45		ND				
Select   Average   ND   NA		5-6 Dec 06	0700-0700		2.46	0.144	ND	2.46		ND ND	
			0700-0700	<del>                                     </del>	2.39	0.151	ND	2.59	0.000		
1-1	A CONTRACTOR OF THE STATE OF TH	7	† · · · · · · · · · · · · · · · · · · ·	+	CANADA PARA	+	<del>†20.435.02</del> 5.55	1	THE REAL PROPERTY.		130-140-140-14
3-6 Dec 06   0700-0700   16   2.46   0.328   7   2.46   0.144   56.3   0.185	eth(flheky))phthajate	4-5 Dec 06	0700-0700	10	2.45	0.204	13	2.45	ŧ	-30.0	
6-7 Dec 06   0700-0700   16   2.39   0.346   7   2.59   0.151   36.2   0.166	5 7 6 2 6	5-6 Dec 06	0700-0700		2.46	0.328	7	2.46	0.144	56.3	
1-3-16-16-16-16-16-16-16-16-16-16-16-16-16-	i transferance	6-7 Dec 06	0700-0700	16	2.59		7	2.59	0.151	56,3	0.194
1-6   Dec   10   0700-0700   17   2.46   0.021   ND   2.46   0.000   ND   NA	AND MACHENANTING CO.O.		de la companya de la	400000000000000000000000000000000000000	L.	A STATE OF THE PARTY OF THE PAR	January and				
Color   Colo	1,2-Dichlorobenzana		0700-0700	17	2.45	0.020	ND	2.45			
A   A   A   A   A   A   A   A   A   A			0700-0700					2.59	0,000		
	<b>文章 医</b>		7,55 - 1,30	<b></b>	T	1	1	1	1	ND	NA
3-6 Dec 06   0700-0700   53   2.46   0.103   MD   2.46   0.000   ND   NA	-1,41Dichlordbehrank		0700-0700	Till	2.45	0.020	T ND	2,45	0.000	ND	NA
Average   ND   NA		5-6 Dec 06	0700-0700	53	2.46	0.103	ND	2.46	0.000	ND ·	NA .
1.5   1.5			0700-0700	53	2.59	0.108	ND	2.59	0.000	ND	NA.
1.5   1.5	HICLORIE ZAMESTICALIO		1000	I max material or		1	The second		A company		
A-7   Dec 06   O700-0700   A1   2.59   0.086   ND   2.59   0.000   ND   NA	Napillalene	4-5 Dec 06		7	2.45	0.143		2.45	0.004		
Average   ND   NA			0700-0700			0.144	ND		0.000		NA NA
			2,00-0,00	1-3-	1 22	1	1	1	1 200	ND	NA
1	A Phenarkhrene		0700-0700	NT)	2.45	0.000	ND	2.45	0.000	ND	
Companies   Comp		5-6 Dec 06	0700-0700		2.46			2.46	0.000	ND ND	NA.
GOLPackinder/FORB   1994   1			0700-0700	0.61	2.59				0.000		
	0.00	Average	Life Was No and Bull Company	The territories are single-	1		CANADA PROFILE SAN	1	19-27-19-19-12-13	I ND	
3-6   10   10   10   10   10   10   10   1	Alpha Chlordena			NATIONAL PROPERTY OF THE PARTY	2 45	O MHI				NA NA	
6-7   Dec 66   0700-0700   0.00453   2.59   0.000   0.00592   2.59   0.000   NA   NA   NA   NA   NA   NA   NA	(LICE)		0700-0700		2,46				0.000	NA	NA.
Average		6-7 Dec 06								NA	NA
(497)   3-6 Dec 06   0700-0700   0.52   2.46   0.011   ND   2.46   0.000   ND   NA		1 Average		1					1		
1.50   1.50		4-5 Dec 06	0700-0700		2.45				0.000	ND	N6
Average   ND   NA			8700-0700		2.46	0.011		2.46			
Health   H			9700-0700	0.51	2.59	0.011	ND	2.59	0.000		
(4974) 5-6 Dec 06 9700-0700 0.0571 2.46 0.001 ND 2.46 0.000 ND NA NA ND 2.59 0.000 ND NA NA ND NA NA ND 2.59 0.000 ND NA	AT DESCRIPTION							A Committee Comm		elegation and the second	The second secon
6-7 Dec 06 0700-0700 ND 2.59 0.000 ND 2.59 0.000 ND NA	op.p.EDD		0700-0700	ND 0.0572	2.45	0.000	ND	2,45			
ND NA	THE REAL PROPERTY.	6-7 Dec 06	0700-0700		2.46	0.001	ND ND		0.000		NA NA
			2139:0100		- 6:37	Danie -	115	1-22	1		

Table E-2. WWTP Unit Process Data.

Anslyte	Dats	Tires	Sindge Thickener (TSN) Come.	Sludge Thickener (TSN) Flow (mgd) (setimale)	Siudge Thickener (TSN) (Make (Ibadiay)	Secondary Digester Superture (2DSN) Coze (7 Dec)	Secondary Digaster Supernate (2DSN) (Flow (mgd)	Secondary Digester Supernate (2DSN) Mass ((by/day) Returned	W WTP/ Head- works Influent Mase (lbs/day)	Head- works Effluent to Prim. Clar. Mass (Bu/day)	Return Flows Added to Headworks Mass (lbs(day)	Influent + Return Flows Mass (lbs/day)	Removal Efficiency of Headwarks	Heed- works Mass Removed (lbs/day)
BOD	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	34 46	1,54	436.68 590.8)	680.0 680.0	0.016 0.016	90.74 90.74	1593.77	2029.87	527.42 681.54			
(mg/L)	6-7 Dec 06 Average	0700-0700	33	1.54	423.84 483.78	680.0 680.0	0.016	90.74 90.74	1593.77	2029.87	514.58 574.51	2168.29	8.7	138.42
TSS	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	62.2 100	1.54	798.87 1284.36	17900.0 17900.0	0,016 0,016	2388.58 2388.58	1103.38	7587.06 7339.20	3187.45 3672.94	4290.83 5683.54	-298.7 -82.3	-3296.23 -1655.66
(mg/L)	6-7 Dec 06	0700-0700	95	1.54	1220.14	17900.0	0.016	2388.58	4406.52	6131.07	3608.72	8015.24	42,8	1884.17
	4-5 Dec 06	0700-0700	9.4	1.54	1101.12	17900.0	0.016	2388.58	2506.84	7019.11	3489.70	5996.54	-40.B	-1022,57
Ammonia	5-6 Dec 06	0700-0700 0700-0700	12	1,54	154.12									
(mg/L)	6-7 Dac 06 Average	0700-0700	13	1,54 1,54	166.97	690,0	0,016	92.07	521.64	764.25	239.35	760.99	-0.6	-3.26
Nitrato/Nitrite	4-5 Dec 06 5-6 Dec 06	0700-0700	13	1.54	166.97							<b></b>	,	
l(mg/L)	6-7 Dec 06 Average	0700-0700	18	1,54	231.18 209.78	0.1	0,016	0.01	0.52	99.27	209.79	210.31	21302.9	111.04
	4-5 Dec 06	0700-0700	16	1.54	205.50			<u> </u>	A PROPERTY OF	200 Table 100			1000	COLUMN TO SERVICE
(nig/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	20	1.54	256.87 269.72									<del> </del>
Sale Fee	Average	I		1.54	244.03	1100.0	0.016	146.78	731.36	1236.38	390.81	1122.17	-15.6	-114.20
Total	4-5 Dec 06	0700-0700	6.11	1.54	60.11 78.47		<del> </del>	<del> </del>				<del> </del>		<del> </del>
Phosphorus (mg/L)	6-7 Dec 06	0700-0700	6.15	1.54	78.99							+		<del> </del>
25 (f.)	Average		ADDROGRAMM (1915)	1.54	72.52	198.0	0.016	26.42	87.87	209.70	98.94	186,82	-26.0	-22.88
Greese and Oil	4-5 Dec 06 5-6 Dec 06	grab	ND(<5.00) ND(<5.00)	1.54	32.11 32.11							<u> </u>		<del></del>
(mg/L)	6-7 Dec 06 Average	grab	ND(<5.00)	1,54	32.11	312.0	0.016	41.63	241.88	445.22	73.74	315.62	-53.6	-129.60
CENTRAL CONTRACTOR	4-Dec-06	grab	7400	1.54	95.04	OFFICE STREET, STREET, ST		- ALCOHOL:	S74872 S74126	2000 2000-000		2 2020 216 5	200000000000000000000000000000000000000	SECTION SPECIAL
TPH-Diesal	5-Dec-06 6-Dec-06	grab grab	4100 3000	1.54	52,66 38.53									
energy of	4-Dec-06	grab	73001	1.54	93.76	ND(<40,000)	0.016	5.34	313.83	892.82	67,42	3B1,25	-163.0	-511.58
TPH-Hoavy	5-Dec-06 6-Dec-06	grab	3300J 3600J	1.54	42.38 46.24			-	<del> </del>		<del> </del>			1
*(ppb)	Avenge	1 1	3,000	1.54	60.79	380000.0	0.016	50.71	203.36	571.07	111.50	314.86	-126.0	-256.20
Aluminum	4-5 Dec 06 5-6 Dec 06	0700-0700	0.532	1.54	6.833				-		-		ļ	+
(mg/4-)	6-7 Dec 06 Average	0700-0700	0.964	1.54	12.381	235	0.016	31.358	7,345	46.713	41.646	48.99	31.0	2.278
	4-5 Dec 06	0700-0700	1.09	1.54	0.014	+	1 - 0.57	+ 365	1 1111	1 70:77	11.070	1336.5		
Arasnic (µB/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	1.32 ND(<2.00)	1.54	0,017		-		-			T		+
(Carterian	Average	12.70.2		1.54	0.015	94.4	0.016	0.013	0.018	0.047	0.027	0.05	-9.1	-0.002
Cadmium	4-5 Dec 06 5-6 Dec 06		ND(<2.00) ND(<2.00)	1.54	0.013	-	<del> </del>		<del> </del>	<del> </del>				
(µg/L)	6-7 Dec 06 Average	0700-0700	1.03	1.54	0.013	153	0.016	0.020	0.021	0.038	0.033	0.05	77,5	0.016
19.175	4-5 Dec 06	0700-0700	18	1.54	231,185			A CONTRACTOR OF THE PARTY	11.15	1 10 10 10 10 10		- wetheres	100000000000000000000000000000000000000	
Calcium (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	20.3	1,54	260.725 272.284									1
2701-11	Average 4-5 Dec 06	-	ND(<2.00)	1.54	2.54.731 0.013	597	0.016	79,664	377.852	696.510	234,395	712.25	4.2	15,731
Chromium	5-6 Dec 06	0700-0700	ND(<2.00)	1.54	0.013		1			1				
(jig/L)	6-7 Dec 06 Average	0700-0700	2.05	1.54	0.026	375	0.016	0.050	0.042	0.092	0.067	0,11	41.6	0.017
	4-5 Dec 06			1.54	0.627				-					-
(jig/L)	6-7 Dec 06			1.54	1.012	10000	1	1 (6)	1	- 200	5.454	3.46	1	5.10
ration of the second	4-5 Dec Q6	0700-0700	0,488	1.54	0.873 6.268	12000	0.016	1.601	1.228	3,595	2.474	3.70	8.8	0.108
fron *(mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	0.718	1.54	9,222			-	-					-
7.967	Average		F 1	1.54	8.404	135	0.016	18.014	8,788	37.886	26.418	35,21	-30.5	-2.68
Lead	4-5 Dec 06			1.54	0.025	T	ļ		-					-
(Hg/L)	6-7 Dec 06			1.54	0.032	1010	0.016	0.135	0.035	0,203	0.167	0.20	0.0	0.00
	4-5 Dec 06	0700-0700	5.52	1.54	70.897	+ <del></del>	1 2.015		+ ***				en ement se il and	
Magnesion (big/L)	5-6 Dec 06	0700-0700		1.54	75.906 77.832		<del></del>	1					<del> </del>	
	Average	1.00.00		1.54	74.878	71.9	0.016	9.594	116.066	197.695	84,473	200.54	2.5	2.84
Mercury	4-5 Dec 06	0700-0700		1.54	0.001	-	-	-	+	-	-		-	-
(µg/L)	6-7 Dec 06		ND(<0.20)	1.54	0.001	26.0	0.016	0.003	0.004	0.017	0.005	0.01	-246.9	-0.00
	4-5 Dec 00			1.54	0.103			10 2 2 2 2 2 2 2				W   D   V   V		
Molybdenum (ug/L)	5-6 Dec 06			1.54	0.144		+						-	_
ASSET OF THE PARTY.	Average			1.54	0.145	309.0	0.016	0.041	0.328	0,452	0,186	0.51	19.1	0.08
Nickel	4-5 Dec 0:	6 0700-0700	3.96	1.54	0. <b>0</b> 72 0. <b>0</b> 51					1				
(ug/L)	6-7 Dec 0 Average		3,45	1.54	0.044	283.0	0.016	0.038	0.171	0.135	0.094	0.26	76.0	0.1.
	4-5 Dec D	6 0700-0700		1.54	0.006	1 22 2						7 2 2 3		
Scienium (µg/L)	5-6 Dec B	6 0700-0700		1.54	0.006 0.013							$\pm$		1.
- Indiana de la companion de l	Average			1.54	0.009	98.3	0.016	0.013	0.014	0.040	0.022	0.04	-28.4	-0.0
Silver	4-5 Dec 0 5-6 Dec 0	6 0709-0700	ND(<1.00)	1.54	0.006 0.006									
(µg/L)	6-7 Dec 0 Average		ND(<1.00)	1.54	0.006	31,0	0,016	0,004	0.010	0.039	0.011	0.02	-172.1	-0.0
TO SECURE OF THE PARTY OF THE P	4-5 Dec 0	6 0700-0700		1.54	1.438									2 11 11 11
Zinc (mg/L)	5-6 Dec 0 6-7 Dec 0	6 0700-0700		1.54 1,54	2.171							$\pm$		
	Average			1.54	1.965	29.7	0.016	3.963	2.167	7.880	5.928	8.09	9.9	0.2

Table E-2. WWTP Unit Process Data (continued).

Analyte	Date	Time	Primary Clapfier Influent (ICLIN) Conc. (ppm)	Primary Clarifier Influent (ICLIN) Flow (mgd)	Primary Clarifier Influent (ICLIN) Mess (bs/day)	Primary Cladifier Effluent (ICLEP) Cont. (ppm)	Primery Clerifier Efficient (ICLEF) Flow (mgd)	Primary Clarifier Efficient (ICLEP) Mass (Balday)	Primary Clarifier Rem Effic (%)	Primary Clarifier Mass Removed (lbs/day)
BOD (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	9700-0700 9700-0700 9700-0700	61	3,99	2029.87 Data discarded d Data discarded d	41 ue to unsatisfacto ue to unsatisfacto	3.57 ry laboratory Q	1220,04 A/QC findings A/QC findings	39.9	809.83
	Average 4-5 Dec 06	0700-0700	228	3.99	7587.06	B0 +	3.57	2380.57	68.6	5206.50
TSS (mg/L)	5-6 Dec 06 6-7 Dec 06	9700-0700 9700-0700	220 178	4.00	7339.20 6131.07	79	3.58	2357.40	67.9	4981.80 4028.19
(mg/L)	Average	3700-0700	1/8	4.13	7019.11	68	3.71 3.62	2102.88 2280.28	65.7 67.5	4738.83
Ammonia	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	21 23	3.99 4.00	698.81 767.28	19	3.57	565.39 566.97	19.1	133,42
(mg/L)	6-7 Dec 06	0700-0700	24	4:13	826.66	24	3.71	742.19	10.2	84.47
	Average 4-5 Dec 06	4-14	1.3	1.99	764.25 43.26	4	3.62	624.85 119.03	18.2 •175.1	-75.77
Nitrate/Nitrite	5-6 Dec 06	0700-0700	3.5	4,00	116.76	4.8	1.58	143.23	-22.7	-26,47
(mg/L)	6-7 Dec 06 Average	0700-0700	4	4.13	99.27	4.1	1.71 3.62	126.79 129.68	-30.6	10,99 -30,42
TKN	4-5 Dec 06 5-6 Dec 06	1(1-)(	33	3.99	1098.13	27	3.57	803.44	26.8	294.69
(mg/L)	6-7 Dec 06	0700-0700 0700-0700	18 39	4.00 4.13	1267.68 1343,32	30 32	3.58 3.7)	895.22 989.59	29.4 26.3	372.46 353.73
	Average 4-5 Dec 06	5700 0700		4.04	1236.38	en arrowani e	3.62	896.08	27.5	340.29 77.36
Cotal Phosphorus	5-6 Dec 06	0700-0700 0700-0700	6.17 6.25	3.99	205,32 208,50	4.3	3.57 3.58	127.96 146.22	29,9	62.28
(mg/L)	6-7 Dec 06 Average	0700-0700	6.25	4.04	215.28	4.69	3.71	145.04	32.6 33.4	70.24 69.96
	4-5 Dec 06	grab	26	3,99	865.19	12	3.57	157.71	8.18	707,48
Greats and Oil	5-6 Dec 06 6-7 Dec 06	grab grab	7.33	4.00	244,53 225,95	10.6 ND(<1.00)	3.58 3.71	149.20 78.86	39.0 65.1	95.33 147.10
¥-4	Average			4.04	445.22		3.62	128.59	71.1	316.63
PH-Diesel Range	4-Dec-06 5-Dec-06	grab grab	53000 14000	3.99 4.00	1763.66 467.04	6500 5800	3.57	193.42 173.08	89.0 62.9	1570.24 293.96
(ded)	6-Dec-06	grab	13000	4.13	447,77 892.82	4500	3.71	139.16 168.55	68.9	308.61 724.27
C. S. C. Park	4-Dec-06	grab	270003	3.99	892.82	6400J	3.57	190.45	81.i 78.B	708.02
PH-Heavy Rango (ppb)	5-Dec-06 6-Dec-06	grab grab	11000 13000)	4.00	366.96	3700J 3200J	3.58 3.71	98,96	69.9 77.9	256.55 348.82
100	Average	Rind	130007	4.13 4.04	447.77 571,07	32001	3.62	133.27	76.7	437.80
Aluminum	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	1.34	3.99 4.00	44.591	0.47 0.414	3,57 3.58	13.986	68.6 74.6	30.605 36,352
(mg/L)	6-7 Dec 06	0700-0700	1.36	4:13	48,706 46.844	0.318	3.71	9.834	79.0	37.010
Circ. Wa	Average	0700-0700		4.04	46.713	and constant	3.62	12.058	74.2	34.655
Amenic	4-5 Dec 06 5-6 Dec 06	0700-0700	1.49	3.99 4.00	0.050 0.058	1.14	3.57 3.58	0.034	31.6	0,016 0,023
(µg/L)	6-7 Dec 06 Average	0700-0700	ND(<2.00)	4.13	0.054	ND(<2.00)	3.71	0.034	36.6	0.019
	4-5 Dec 06	0700-0700	ND(<2.00)	3.99	0,033	ND(<2.00)	3.57	0.030	10.6	0.004
Cadmium (µg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	ND(<2.00) 1.39	4.00 -	0.033	ND(<2.00) ND(<1.00)	3.58	0.030	10.6	0.004 0.032
SMITTER OF	Average			4.04	0.038		3.62	0.025	34,5	0.013
Calcium	4-5 Dec 06	0700-0700	20.9	3,99 4,00	665,532	17.3	3,57	514.798 546.082	22.6	150.73
ev (hig/L)	6-7 Dec 06 Average	0700-0700	21.3	4.13	726.773 696.530	18.6	3.71	546.082 575.200 545.360	21.7 20.9 21.7	151.57
	4-5 Dec 06	0700-0700	2.71	3.99	0.090	ND(<2.00)	3,57	0.030	67.0	0.060
(Chromum (jig/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	2.63 2.82	4.00 4.13	0.088	ND(<2.00) ND(<2.00) ND(<2.00)	3.58	0,030	66.0 68,2	0.058
N. Walter	Average	1		4.04	0.092	142(-2,00)	3.62	0.030	67.1	0.062
e Copper	4-5 Dec 06 5-6 Dec 06	0700-0700	100	3,99	3,328	48.7	3,57 3,58	1.449	56.5 57.7	1.878
(Pg/L)	6-7 Dec 06	0700-0700	108	4.00 4.13	3,736 3,720	53 55,1	3.71	1.704	54.2	2.016
<b>#</b>	Average 4-5 Dec 06	0700-0700	1.04	4.04 3,99	3.595 34.608	0.471	3.62	1.578	56.1 59.5	20.59
(a) i Iron	5-6 Dec 06	0700-0700	1.11	4.00	37.030	0.42	3,58	12,533	66.2	24.49
(mg/L)	5-7 Dec 06 Average	0700-0700	1.22	4.13	42.022 37.886	0.379	3.71	11,720 12.756	72.1 66,3	30.30 25.13
Load	4-5 Dec 06 5-6 Dec 06	0700-0700	6.08	3,99	0.202	1.84	3,57	0,055	72.9	0.128
(ug/L)	6-7 Dac 06	0700-0700 0700-0700	5,26 6.67	4.13	0.175	ND(<5.00)	3,58 3,71		73.1	
	Average 4 - 5 Dec 06	0700-0700	+42	4.04	0.189	-	3.62	0.051	73.0	33.40
Magnesium	4-3 Dec 06 5-6 Dec 06	0700-0700	5.77	3.99 4.00	192,006 196,824	5.33 5.54	3,57	165,316	16.0	31.50
(hig/lo)	6-7 Dec 06 Average	0700-0700	5.93	4.13	204,254 197,695	5.66	3.71	175,034	14.3	29.22 31.37
	4-5 Dec 06	0700-0700	0.278	3.99	0.009	ND(<0.200)	3,57	0.003	67,8	0.00
Merciury (µg/L)	5-6 Dec 06	0700-0700	0,699	4.00	0.023	ND(<0.200) ND(<0.200)	3.58	0.003	87,2 83,0	0.02
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Average	Name of the Control o		4.04	0.017	PET La scott in case of	3,62	0.003	j 82.2	0.01
Molybdenum	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0760	11.7	3.99 4.00	0.389	ND(<5.00) 10.5	3,57	0.074	80.9	0.06
(μ)/L)	6-7 Dec 06 Average	0700-0700	17.2	4.13 4.04	0.592	16.7	3,71	0,516	12.8	0.07
M/AT	4-5 Dec 06	0700-0700	4.49	3.99	6,149	2.47	3,57	0.074	50.8	0.07
Nickel (µg/L)	5-6 Dec 06 6-7 Dec 06	0700-0780 0700-0700	3.79	4,00	0,126 0,128	2.41	3.58	0.072	43.1 40.2	G,05 0.05
393 FE/5	Average	I		4.04	0.135		3.62	0.074	45.0	0.06
Selenium	4-5 Dec 06 5-6 Dec 06	0700-0700	1.15	3.99 4.00	0.038 0.046	ND(<1.00) 1,04	3,57	0.015	61.1 33.1	0.02
(µg/L)	6-7 Dec 06	0700-0700	ND(<2.00)	4.13	0.034	ND(<2,00)	3.71	0.031	10.2	0.00
EFO	Average 4-5 Dec 06	0700-0700	1.26	3.99	0.040	I ND(e) no	3.62	0.026	35.5 64.5	0.01
Silver	5-6 Dec 06	0700-0700	1.19	4.00	0.840	ND(<1.00) ND(<1.00)	3.58	0.015	62.4	0.02
(μያ/ጌ)	6-7 Dac 86 Average	0700-0700	1.02	4.13	0.035	ND(<1.00)	3.71	0,015	56.0 61.2	0.02
LIST	4-5 Dec 66	0700-0700	0,243	3.99	8,086	0.105	3.57	3.124	61.4	4.96
Zinc (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	0.237	4,00	7,906 7,647	0.121	3.58 3.71	3.611 2.721	54.3 64.4	4.25
direct .	Average			4.04	7.880		3,62	3.152	60.0	4.72

Table E-2. WWTP Unit Process Data (continued).

Analyte	Date	Time:	Trickling Filter Influent (TFIN) Conc	Trickling Eiler Influent (TFIN) Flow (ingd)	Trickling Pil(er Telluent (TFLN) Mell (Barday)	Trickling Eilter Efficient (TPET) Come	Trickling Filter Efficient (TPEF) Flow (ngd)	Trickling Filter Efficient (TPER) Mass (lbs/day)	Trickling Filter Rem.Effic. (%)	Trickling Filier Meas Removed (he/dey)
BOD (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	41	3.57	1220.04 Data discarded Data discarded	due to unsatisfacto due to unsatisfacto	3,57 ry Inboratory Q.	446.36 A/QC findings A/QC findings	63,4	773.69
TSS	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	80 79	3.57 3.58	2380.57 2357.40	45	3.57 3.58	1339.07	43.8 38.0	1041.50 895.21
(mg/L)	6-7 Dec 06 Average	0700-0700	68	3.71 3.62	2102.88 2280.28	70	3.71 3.62	2164.73 1655.33	·2.9 26.3	-61.85 624.96
Ammonis	4-5 Dec 06 5-6 Dec 06	8700-0700 0700-0700	19	3.57 3.58	565.39	4.1	3.57	122.00	78.4 66.8	443.38 378.97
(mg/L)	6-7 Dec 06 Average	0700-0700	24	3.71 3.62	566.97 742.19 624.85	6.3 7.4	3.58 3.71 3.62	228.84 179.61	69.2 71.5	513.35 445.24
	4-5 Dec 06	0700-0700	4	3.57	119.03	19	3.57	565.39	-375.0	-446.36
Nitrate/Nitrite (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	4.8 4.1	3,58 3.71	143.23 126.79	23 28	3,58 3,71	686.33 865.89	-379.2 -582.9	-543.10 -739.10
	Average 4-5 Dec 06	6700-0700	27	3.62	129.68 803.44	8.9	3.57	705.87	-445.7 67.0	-576.19 538.60
TKN :(mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	30 32	3.58 3.71	895.22 989.59	11	3.58 3.71	328.25 340.17	63.3 65.6	566.97 649.42
2.752.75 (c)	Average 4-5 Dec 06	0700-0709	4.3	3.62	896.08 127.96	4.35	3,62	311.09 129.44	65.3	585.00 -1.49
Total Phosphonis (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	4,9	3.58 3.71	146.22	4.93 4.97	3,57 3,58 3,71	147.11	-0.6 -6.0	-0.90 -8.66
ATTACK TO A STATE OF THE STATE	Average		12	3.62 3.57	139.74		3.62	143.42	-2.6	-3.68
Grease and Oil	4-5 Dec 06 5-6 Dec 06	grab grab	10.6	3,58	357.09 316.31	ND(<5.30) ND(<5.00)	3.57 3.58	74.39 74.60	79.2 76.4	282.69 241.71
(mg/L)	6-7 Dec 06 Average	8 rach	ND(<5.00)	3.71 3.62	77.31 250.24	ND(<5.00)	3.71 3.62	77.31 75.44	51,9	0.00 174,80
TPH-Dissel Reinge	4-Dec-06 5-Dec-06	grab grat	6500 5800	3,57 3,58	193.42 173.08	1500 1500	.3.57 3.58	44.64 44.76	76.9 74.1	148.79
(p <b>p</b> b)	6-Dec-06 Average	grab	4500	3.71 3.62	139.16 168.55	1100)	3.71 3.62	34.02 41.14	75.6 75.5	105.14
TPH-Heavy Range	4-Dec-06 5-Dec-06	grab grab	6400J 3700J	3,57 3,58	190,45	22007 2300)	3.57 3.58	65,47 68.63	65.6 37.8	124.98 41.78
(upb)	6-Dec-06 Average	grab	32007	3,71	98.96 133.27	23007	3,71 3,62	71.13	28.3 43.9	27,83 64.86
C122515. 11	4-5 Dec 06	0700-0700	0.47	3.57	13.986	0.482	3.57	14.343	-2.6	-0.357
Aluminum (mg4-)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	0.414	3.5B 3.7i	9.834	0.474	3.58	14.144	-14.5 -45.0	-1.790 -4.422
	Average 4-5 Dec 06	0700-0700	1.14	3.62	12.058	1.16	3.62	0.035	-20.7 -1.8	-2.190 -0.001
Arsenic (up/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	1.17 ND(<2.00)	3.58	0.035	1,23 ND(<2,00)	3,58	0.037	-5.1 0.0	-0.002 0.000
<del>Farter vere</del>	Average 4-5 Dec 06	0700-0700	ND(<2.00)	3.62	0.033	ND(<2.00)	3.62	0.034	-2.3 0.0	0.001
Cadmium (µg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	ND(<2.00) ND(<1.00)	3,58	0.030	ND(<2.00) ND(<1.00)	3,58	0.030	0.0 0.D	0,000
F / 14 T   10 T	Average			3.62	0.025	and the second second second	3.62	0.025	0.0	-17.854
Catoism	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700 0700-0700	17.3 18.3 18.6	3.57	514.798 546.082	17.9 19 19.2	3.57 3.58 3.71	532.652 566,970 593.755	-3.5 -3.8 -3.2	-17.839 -20.888 -18.555
(mg/L)	6-7 Dec 06 Average			3.62	575,200 545,360		3.62	564.459	-3.5	-19.099
Chropium	4-5 Dec 06 5-6 Dec 06	9790-0700 9790-0700	ND(<2.00) ND(<2.00)	3.57 3.58	0.030 0.030	ND(<2.00) ND(<2.00)	3.57 3.58	0.030	0.0	0.000
(Jug/L)	6-7 Dec 96 Average	0700-0700	ND(<2.00)	3.71	0.031	ND(<2.00)	3.71 3.62	0.031	0.0	0.000
Copper	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	48.7 53	3.57	1.449	49.8 52.7	3,57	1.482	-2.3 0.6	-0.033 0.009
(agat.)	6-7 Dec 06 Average	0700-0700	55.1	3.71	1.704	58.6	3.71 3.62	1.812	+6.4 -2.7	-0.108 -0.044
	4-5 Dec 06	0700-0700	0.471	3.57	14.016	0,512	3.57	15.236 13.697	-8.7 -9.1	-1.220 -1.164
(mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	0.42	3.58 3.71 3.62	12.533 11.720 12.756	0.485	3.58 3.71 3.62	14,998	-28.0 -15.3	-3.278 -1.887
	4-5 Dec 06	0700-0700	1.84	3.57	0.055	1.67	3.57	0.050	9,2	0.005
Lead (rig/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	1.58 ND(<5.00)	3.58	0.047	2.29 ND(<5.00)	3.58	0.068	-44.9 0.0 -11.9	-0.021 0.000 -0.005
	Average 4-5 Dec 96	0700-0700	5.33	3.62	0.060	5.57	3.62	0.065 165,747	-11.9 -4.5	-7.142
Magnesium (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	5.54 5.66	3.58	165.316 175.034	5.74 5.75	3,58	171.285 177.817	-3.6 -i.6	-5.968 -2.783
	Average 4-5 Dec 06	9700-0700	ND(<0,200)	3.62	166,319 0.003	ND(<0.200)	3.62	171.616	-3.2 0.0	-5.298 0.000
Mercury (µg/L)	5-6 Dec 05 6-7 Dec 05	0700-0700 0700-0700	ND(<0,200) ND(<0.200)	3.58	0.003	ND(<0.200) ND(<0.200)	3.58	0.003	0.0	0,000
	Average 4-5 Dec 06	9700-0700	ND(<5.90)	3.62	0.003	9.61	3.62	0.003	-284.4	-0.212
Molybdenum (ul/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	10.5	3,58	0.313 0.516	10.1	3.58 3.71	0.301 0.476	3.8	0.012
	Average	1		3.62	0.301		3.62	0.355	-90.9	-0.053
Nickel	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	2.47	3.57 3.58	0.074 0.072	2.32 3.87	3.57 3.58	0.069 0.115	6.1	0.004
(µg/L)	6-7 Dec 06 Average	3700-0700	2.47	3.71	0.076	3.01	3.71	0.093 0.093	-21.9 -25.5	-0.017 -0.019
Selenain	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<1.06) 1.04	3.58	0.015 0.031	ND(<1.00) ND(<1.00)	3.57	0.015 0.015	0.0 51,9	0.000
(µg/L)	6-7 Dec 06 Average	9700-0700	ND(<2.00)	3.71	0.031	ND(<2.00)	3.71 3.62	0.031 0.020	0.0 17.3	0.000
Silver	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<1.00) ND(<1.00)	3.57 3.58	0.015	ND(<1.00) ND(<1.00)	3.57	0,015	0.0	0.000
(µg/L)	6-7 Dec 06 Average	0709-0700	ND(<1.00)	3.71 3.62	0.015 0.015	ND(<1.00)	3,58 3,71 3,62	0.015	0.0	0.000
	4-5 Dec 06	0700-0700	0.105	3.57	3,124	0,103	3.57 3.58	3,065	1.9	0.060
Zine (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	0.121 0.088	3.58	3.611	0.114	3.58	3,402	5.8 -23.9	0.209 -0.64

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Table E-2. WWTP Unit Process Data (continued).

Analyte	Date	Time	Trickling Filter Influent (TFDY) Cong.	Trickling Filter Influent (TETM) Flow (mad)	Trickling Filler Influent (TFIN) Mere (Be/day)	East Tricking Filter Efficient (TP IEF) Conn	East. Trickling Filter Effluent (In IEF) Flow (mgd)	Bass Trickling Filler Efflueds (PELEF) Mass (Postaly)	East Triokling Filter Romeffic (%)	East Trickling Pilto: Mass Removed (lbs/day)
BOD (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	41	1,78	610.02 Data disparded Data disparded	141 lue to unsatisfact lue to unsatisfact	1.78 ory laboratory Q	208.30 A/QC findings	65.9	401.72
TSS (mg/L)	Average 4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	80 79 68	1.78 1.79 1.85 1.81	1190.28 1178.70 1051.44 1140.14	44 45 34	1.78 1.79 1.85 1.81	654.66 671.41 525.72 617.26	45.0 43.0 50.0 45.9	535,63 507,29 525,72 522,88
Aarmbuig (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	19 19 24	1.78 (.79 1.85 1.81	282.69 283.48 371.10 312.42	3.4 5.3 6.5	1.78 1.79 1.85 1.81	50.59 79.08 100.51 76.72	82.1 72.1 72.9 75.4	232.11 204.41 270.59 235.70
Nitrato/Nitrite (rog/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	4 4.8 4.1	1.78 1.79 1.85 1.81	59.51 71.62 63.40 64.84	20 23 26	1.78 1.79 1.85 1.81	297.57 343.17 402.02 347.59	-400.0 -379.2 -534.1 -436.0	-238.06 -271.55 -338.63 -282.74
TKN (mg/L;)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700	27 30 32	1.78 1.79 1.85 1.81	401.72 447.61 494.80 448.04	8.6 9.5 10	1.78 1.79 1.85 1.81	127.96 141.74 154.62 141.44	68.1 68.3 68.8 68.4	273,77 305,87 340,17 306.60
Total Phosphorus (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	4,3 4,9 4,69	1.78 1.79 1.85 1.83	63,98 73.11 72.52 69.87	4.27 4.85 4.82	1.78 1.79 1.85 1.81	63,53 72,36 74,53 70,14	0.7 1.0 -2.8 -0.4	0.45 0.75 -2.01 -0.27
Greate and Oil (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	grab grab grati	10.6 ND(<5.00)	1.78 1.79 1.85 1.81	178.54 158.15 38.66 125.12	ND(<6.00) ND(<5.00) ND(<5.00)	1.78 1.79 1.85 1.81	44.64 37.30 38.66 40.20	75.0 76.4 0.0 67.9	133.91 120.85 0.00 84.92
TPH Diesel Range (ppb)	4-Dec-06 5-Dec-06 6-Dec-06 Average	grab grab grab	6500 5800 4500	1.78 1.79 1.85 1.81	96.71 86.54 69.58 84.28	1300 2000 1100J	1.78 1.79 1.85 1.81	19.34 29.84 17.01 22.06	80.0 65.5 75.6 73.8	77,37 56,70 52,57 62,21
TPH-Heavy, Range (ppb)	4-Dec-06 5-Dec-06 6-Dec-06 Average	grab grab grab	6400J 3700J 3200J	1.78 1.79 1.85 1.81	95.22 55.20 49.48 66.64	19003 2500 22003	1.78 1.79 1.85 1.61	28.27 37.30 34.02 33.20	70.3 32.4 31.3 50.2	66.95 17.90 15.46 33.44
Aluminim (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	0.47 0.414 0.318	1.78 1.79 1.85 1.81	6.993 6.177 4.917 6.029	0.436 0.459 0.426	1.78 1.79 1.85 1.81	6.487 6.848 6.587 6.641	7,2 -10,9 -34,0 -10,1	0.506 -0.671 -1.670 -0.612
Amenio (µg/l.)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	1.14 (.17 ND(<2.00)	1.78 1.79 1.83 1.81	0.017 0.017 0.015 0.017	1.06 1.15 ND(<2.00)	1.78 1.79 1.85 1.81	0.016 0.017 0.015 0.016	7.0 1.7 0.6 3.0	0.001 0.000 0.000 0.000
Cadmium (µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	ND(<2,00) ND(<2,00) ND(<1,00)	1.78 1.79 1.85 1.81	0.015 0.015 0.008 0.013	ND(<2.00) ND(<2.00) ND(<1.00)	1.78 1.79 1.85 1.81	0.015 0.015 0.008 0.008	0.0 0.0 0.0 0.0	0.000 0.000 0.000 0.000
Celò(um (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	17.3 18.3 18.6	1.78 1.79 1.85 1.81	257.399 273.041 287.600 272.680	17.6 18.8 19.3	1.78 1.79 1.85 1.81	261.863 280.501 298.424 280.262	-1.7 -2.7 -3.8 -2.8	-4.464 -7.460 -10.824 -7.582
Chromum (#g/L)	4-5 Dea 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	ND(<2.00) ND(<2.00) ND(<2.00)	1.78 1.79 1.85 1.81	0.015 0.015 0.015 0.015	ND(<2.00) ND(<2.00) ND(<2.00)	1.78 1.79 1.85 1.83	0.015 0.015 0.015 0.015	0.0 0.0 0.0 0.0	0.000 0.000 0.000 0.000
Copper (µBL)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0706 0708-0700 0700-0700	48.7 53 55.1	1.78 1.79 1.85 1.81	0.725 0.791 0.852 0.789	45,9 55,9 56,8	1.78 1.79 1.85 1.81	0.683 0.834 0.878 0.798	5.7 -5,5 -3,1 -1.2	0.042 -0.043 -0.026 -0.009
jron (njg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0780 0700-0700 0700-0700	0.471 0.42 0.379	1.78 1.79 1.85 1.81	7,008 6,267 5,860 6,378	0.437 0.465 0.439	1.78 1.79 1.85 1.81	6.502 6.938 6.788 6,743	7.2 -10.7 -15.8 -5.7	0.506 -0.671 -0.928 -0.364
Lead (kg/L)	4-5 Dec 96 5-6 Dec 96 6-7 Dec 96 Average	0700-0700 0700-0700 0700-0700	1.84 1.58 ND(<5.00)	1.78 1.79 1.85 1.81	0,027 0,024 0,039 0,030	1.67 2.05 ND(<5.00)	1.78 1.79 1.85 1.81	0.025 0.031 0.039 0.031	9,2 -29,7 0,6 -5,6	0.003 -0.007 0.000 -0.001
Magnesii/m (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0760-0760 0760-0700 0790-0700	5.33 5.54 5.66	1.78 1.79 1.85 1.81	79.303 82.658 87.517 83.159	5.5 5.67 5.79	1.78 1.79 1.83 1.81	81.832 84.598 89.527 85.319	-3.2 -2.3 -2.3 -2.6	-2,529 -1,940 -2,010 -2,160
Meropcy (lig/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0760-0700 0700-0700	ND(<0.200) ND(<0.200) ND(<0.200)	1.78 1.79 1.85 1.81	0.001 0.001 0.002 0.002	ND(<0.200 0.258 ND(<0.200	1.79 1.85 L.81	0.001 0.001 0.002 0.002	0.0 0.0 0.0 0.0	0.000 0.000 0.000 0.000
Molybdanuss (#g/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	9700-9700 9700-9700 9700-9700	ND(<5.60) 10,5 16.7	1.78 1.79 1.85 1.81	0.037 9.157 0.258 0.151	8.59 10.9 13.3	1.78 1.79 1.85 1.81	0.128 0,163 0.237 0.176	-243.6 -3.8 8.4 -16.6	-0.091 -0.006 0.022 -0.025
Nicksi (jig/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	2.47 2.41 2.47	1.78 1.79 1.85 1.81	0.037 0.036 0.038 0.037	2.19 2.56 2.52	1.78 1.79 1.85 1.81	0.033 0.038 0.039 0.037	11,3 -6.2 -2.0 1.0	0.004 -0.002 -0.001 0.000
Selenium (L'gil)	4-5 Dec 86 5-6 Dec 86 6-7 Dec 86 Average	0700-0700 0700-0700 0700-0700	ND(<1.00) 1.04 ND(<2.00)	1.78 1.79 1.85 1.81	0.007 0.016 0.015 0.013	ND(<).00 ND(<).00 ND(<2.00	1.79 1.85 1.81	0.007 0.007 0.015 0.010	0.0 51.9 0.0 21.0	0.000 0.008 0.000 0.003
Silver (pg/L)	4-5 Dec 06 3-6 Dec 06 6-7 Dec 06 Average	9700-0700 9700-0700 9700-0700	ND(<1.00) ND(<1.00) ND(<1.00)	1.78 1.79 1.85 3.81	0.007 0.007 0.008 0.008	ND(<1.00 ND(<1.00 ND(<1.00	1.79	0.007 0.007 0.008 0.008	0.0 0.0 0.0 0.0	0.000 0.000 0.000 0.000
Zinc (mg/L)	4-5 Dec 96 3-6 Dec 96 6-7 Dec 96 Average	0700-0700 0700-0700 0700-0700	0.105 - 0.121 0.088	1.78 1.79 1.85 1.81	1.562 1.805 1.361 1.576	0.097 0.109 0.104	1.78 1.79 1.85 1.81	1.443 1.626 1.608 1.559	7.6 9.9 -18.2	0.119 0.179 -0.247 0.017

Table E-2. WWTP Unit Process Data (continued).

Analyte	Dela	Time	Trickling Filier Influent (FFD) Cons	Inckling Filler Inflient (TFIN) Rlow (mgd)	Tripking Filler! Influent (TPIN) Mass (Ibs/day)	West Topkling Filter Editions (172EF) -Conc.	Yest Trickling Filler (TP2HF) : Flow (mgd)	West Trickling Filter! (FF2EF) Mast (lbs/day)	West Trickling Fijler Rem Effic (%)	West Trickling Filter Mass Removed (bs/day)
BOD (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	41	1.78	610.02 Data discarded Data discarded	8.90 due to unsatisfact due to unsatisfact	1.78 ory laboratory Q ory laboratory Q	132.42 A/QC findings A/QC findings	78.3	477.60
TES	Average 4-5 Dec 06	0700-0700	80	1.78	1190.28	41.00	1.78	610.02	48.8	580.26
(mg/L)	5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700	79 68	1,79 1,85 1,81	1178.70 1051.44 1140.14	50.00 48.00	1.79 1.85 1.81	746.01 742.19 699.41	36.7 29.4 38.7	432.69 309.25 440.73
Ammonia (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	19 19 24	1.78 1.79 1.85 1.81	282.69 283.48 371.10 312.42	4.00 6.70 7.10	1.78 1.79 1.85 1.81	59.51 99.97 109.78 89.75	78.9 64.7 70.4 71.3	223.18 183.52 261.31 222.67
Nifrete/Nitrite (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	4 4.8 4.1	1.78 1.79 1.85 1.81	59.51 71.62 63.40 64.84	18.00 25.00 25.00	1.78 1.79 1.85 1.81	267.81 373.01 386.56	-350.0 -420.8 -509.8	-208.30 -301.39 -323.16
TKN (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	27 30 32	1.7B 1.79 1.85	401.72 447.61 494.80	8,70 11.00 12.00	1.78 1.79 1.85	342.46 129.44 164.12 185.55	67.8 63.3 62.5	-277.62 272.28 283.48 309.25
Total Phosphorus	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	4.3 4.9 . 4.69	1.81 1.78 1.79 1.85	63.98 73.11 72.52	4.28 4.98 4.83	1.81 1.78 1.79 1.85	159.70 63.68 74.30 74.68	0.5 -1.6 -3.0	288,34 0.30 -1,19 -2.16
18.10.24 18.11.24	Average 4-5 Dec 06	grab	12	1.81	69.87 178.54	ND(<6.00)	1.81	70.89 44.64	75,0	-1.02 133.91
Grease and Oil (mg/L)	5-6 Dec 06 6-7 Dec 06 Average	grab grab	10.6 ND(<5.00)	1,79 1,85 1,81	158.15 38.66 125.12	ND(<5.00) ND(<5.00)	1.79 1.85 1.81	37.30 38.66 40.20	76.4 0.0 57.9	0.00 84.92
TPH-Diosel Rango	4-Dec-06 5-Dec-06	grab grab	6500 5800	1.78	96.71 86.54	1800 2100	1.78	26.78 31.33	72.3 63.8	69.93 55.20
(tipb)	6-Dec-06 Average	grab	4500	1.85	69.58 84.28	1300	1.85	20,10	71.1 69.1	49.48 58.20
TPH-Heavy Range (ppb)	4-Dec-06 5-Dec-06 6-Dec-06 Average	grab grab grab	6400J 3700J 3200J	1.78 1.79 1.85 1.81	95.22 55.20 49.48 66.64	26003 2800 24003	1.78 1.79 1.85 1.81	38.68 41.78 37.11 39.19	59.4 24.3 25.0 41.2	\$6.54 13.43 12,37 27.45
Altiminum (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0796-0700 0700-0700 0700-0700	0.47 0.414 0.318	1.78 1.79 1.85 1.81	6.993 6.177 4.917 6.029	0.464 0.427	1.79 1.85 1.81	6.923 6.602 6.601	10.2 -12.1 -34.3 -9.5	0.714 -0.746 -1.685 -0.572
Afrenic (µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-6700 0700-0700 0700-0700	1.14 1.17 ND(<2.00)	1.78 1.79 1.85 1.81	0.017 0.017 0.015 0.017	1.02 1.21 ND(<2.00)	1.78 1.79 1.85 1.81	0.015 0.018 0.015 0.016	10.5 -3.4 0.6 2.4	0.002 -0.001 0.000 0.000
Cedmium (ug/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	ND(<2.00) ND(<2.00) ND(<1.00)	1.78 1.79 1.85 1.81	0.015 0.015 0.008 0.013	ND(<2.00) ND(<2.00) ND(<1.00)	1.78 1.79 1.85 1.81	0.015 0.015 - 0.008 0.013	0.0 0.0 0.0 0.0	0.000 0.000 0.000 0.000
Celcium	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	17.3 18.3	-1.78 1.79	257.399 273.041	17.4	1.78	258.887 279.009	-0.6 -2.2	-1.488 -5.968
(trig/L)	6-7 Dec 06 Average	0700-0700	18.6	1.85	287.600 272.680	18.8	1.85 1.81	290.692 276.196	-1.1	-3,092 -3,516
Chromium (µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	ND(<2.00) ND(<2.00) ND(<2.00)	1.78 1.79 1.85 1.81	0,015 0,015 0,015 0,015	ND(<2.00) ND(<2.00) ND(<2.00)	1.78 1.79 1.85 1.81	0.015 0.015 0.015 0.015	0.0 0,0 0.0 0.0	0.000 0.000 0.000 0.000
Copper (44/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	48.7 53 55.1	1.78 1.79 1.85 1.81	0.725 0.791 0.852 0.789	44.7 55.7 54.1	1.78 1.79 1.85 1.81	0.665 0.831 0.837 0.778	8.2 -5,1 1.8 1.5	0,060 -0.040 0.015 0.012
Jon (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0760-0760 0760-0760 0760-0760	0.471 0.42 0.379	1.78 1.79 1.85 1.81	7.008 6.267 5.860 6.378	0.445 0.463 0.419	1.78 1.79 1.85 1.81	6.621 6.908 6.479 6.669	5.5 -10.2 -10.6 -4.6	0.387 -0.642 -0.618 -0.291
Lead Gig/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	1.84 1.58 ND(<5.00)	1.78 1.79 1.85	0.027 0.024 0.039	2.04 1.91 ND(<5.00)	1.78 1.79 1.85	0.030 0.028 0.039 0.033	-10.9 -20.9 0.0 -8.8	-0.003 -0.005 0.000 -0.003
Magnesium (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	5.33 3.54 5.66	1.81 1.78 1.79 1.85	79.303 82.658 87.517	5.53 5.67 5.6	1.78 1.79 1.85	82.278 84,598 86.589	-3.8 -2.3 i.1	-2.976 -1.940 0.928
Maroury (µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0709-0700 0700-0700 9700-0700	ND(<0.200) ND(<0.200) ND(<0.200)	1.81 1.78 1.79 1.85	0.001 0.001 0.002	ND(<0.200) ND(<0.200) ND(<0.200)	1.81 1.78 1.79 1.85	0.001 0.001 0.002	0.0 0.0 0.0 0.0	0.900 0.000 0.000
Molybdenum (µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	ND(<5.00) 10.5 16.7	1.81 1.78 1.79 1.85	0.002 0.037 0.157 0.258	9.45 10.8 14.3	1.81 3.78 1.79 1.85	0.002 0.141 0.161 0.221	0.0 -278.0 -2.9 14.4	0.000 -0.103 -0.004 0.037
Nickel ((µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	2.47 2.41 2.47	1.78 1.78 1.79 1.85	0.151 0.037 0.036 0.038	2,54 3,18 2.81	1.81 1.78 1.79 1.85	0,174 0,038 0,047 0,043	-15.7 -2.8 -32.0 -13,8	-0.024 -0.001 -0.011 -0.005
Selenium (µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	ND(<).00) 1.04 ND(<2.00)	1.81 1.78 1.79 1.83	0.037 0.007 0.016 0.015	ND(<1.00) ND(<1.00) ND(<2.00)	1.81 1.78 1.79 1.85	0.043 0.007 0.007 0.015	-16.0 0.0 51.9 0.0	-0.006 0.000 0.008 0.000
Silver (µg/L)	4-5 Dec 96 5-6 Dec 96 6-7 Dec 96	0700-0700 0700-0700 0700-0700	ND(<1.00) ND(<1.00) ND(<1.00)	1,81 1,78 1,79 1,85	0.013 0.007 0.007 0.008	ND(<1.00) ND(<1.00) ND(<1.00)	1.81 1.78 1.79 1.85	0.010 0.007 0.007 0.008	21.0 0.0 0.0 0.0	0.003 0.000 0.000 0.000
Zino	Average 4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	0.105 0.121	1.78	0.008 1.562 1.805	0.093 0.109 0.103	1.81 1.78 1.79	0.008 1.384 1.626	0.0 11.4 9.9	0,000 0,179 0,179

Table E-2. WWTP Unit Process Data (continued).

Apalyta	Date.	Tinhe	Secondary Clanifier Influent (4CLIN)	Secondary Clarifler Influent (2CLIN) Flow (mgd)	Secondary Clarifier Influent (2CLIN) Mass ((bs/day)	Secondary Clarifier Efficient (2CLEF) Conc	Secondary Clarifier Efficient (2CLEF) (Flow (mgd)	Secondary Clarifier Effluent (2CLEF) 1 Mass (lbs/day)	Secondary Clarifier Rem Effici (%)	Secondary Clarifier Mass Removed (lbs/day)
BOD (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	15	2.87	358.41 Data discarded of Data discarded of	9.3 ive to unsatisfacto ive to unsatisfacto	2.45 ory laboratory Q ory laboratory Q	190.18 A/QC findings A/QC findings	46.9	168.23
TSS	4-5 Dec 86 5-6 Dec 86	0700-0700 0700-0700	4.5 4.9	2.87 2.88	1075,23 1174,90	22 24	2.45 2.46	449.R9 492.79	58.2 58.1	625.34 682.10
(mg/L)	6-7 Dec 06 Average	0700-0700		2.87	67.5% rem 1125.07	oval by combine	d secondary clar 2.46		56.1	653.72
Ammonia (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06 Average	0700-0700 0700-0700 0700-0700	4.1 6.3 7.4	2.87 2.88 3.01 2.92	97.97 151.06 185.46 144.R3	3.4 4.8 6.2	2.45 2.46 2.59 2.50	69.53 98.56 134.03 100.70	29.0 34.8 27.7 30.5	28.44 52.50 51.43 44.12
Niimte/Nitrito	4-5 Dec 06 3-6 Dec 06	0700-0700 0700-0700	19 23	2,87	453.99	21 20	2.45 2.46	429.44 410.66	5.4 25.5	24.54 140.82
(mg/L)	6-7 Dec 06 Average	0700-0700	28	2.88 3.01 2.92	551.48 701.73 569.07	26	2.59 2.50	562.05 467.38	19.9	139.68
TKIN	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	8.9 11	2.87 2.88	212.66 263.75	5.B 8.3	2.45 2.46	170,42	44.2 35.4	94.05 93.33
(m <b>g/L</b> )	6-7 Dec 06 Average	0700-0700	ii	3.01 2.92	275.68 250.70	9.4	2,59 2,50	203,30 164.08	26.3 34.6	72,48 86.62
Total Phosphorus	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	4,35 4,93	2,87 2.88	103.94 118.21	4,46	2.46	91,58	26.6 22,5	27.66 26.63
(mg/L)	6-7 Dec 06 Average	0700-0700	4,97	3.01 2.92	124,56 115,57	4,55	2,59 2,50	98.36 88.74	23.2	26.20 26.83
Greec and Gil	4-5 Dec 06 5-6 Dec 06	grab grab	ND(<5.30) ND(<5.00)	2,87 2,88	63.32 59.94	ND(<5.50 ND(<5.00)	2.45 2.46	56.24 51.33	11.2	7.Q8 8.61
(mg/L)	6-7 Dec 06 Average	grab	ND(<5,00)	3,01 2,92	62.65 61.97	ND(<5.70)	2.59 2.50	61.61 56.39	9.0	1.05 5.58
PH Diesei Range	4-Dec-06 5-Dec-06	grab grab	1500 1500	2,87 2,88	35.84 35.97	1200 790	2.45 2.46	24.54 16.22	31.5 54.9	11.30 19.75
(0°pb)	6-Dec-06 Average	grab	11003	3,01 2,92	27,57 33,13	5603	2,59 2,50	12,11 17,62	56.1 46.8	15.46 15.50
TPH-Heavy Range	4-Dec-06 5-Dec-06	grab grab	2200J 2300J	2.87	52,57 55.15	1600 1700J	2.45 2.46	32.72 34.91	37,8	19.85 20.24
(pp6)	6-Dec-06 Average	gmb	2300)	3.01 2.92	57,64 55.12	16003	2.59 2.50	34.59 34.07	38.2	23.05
Alumunum	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	0.482	2,87 2,88	11.517	0.27	2.45	5.521 5.359	52.1 52.8	5.996 6,006
(mg/L)	6-7 Dec 06 Average	0706-0700	0.461	3.01 2.92	11.553	0.228	2.59 2.50	4,929 5,270	57.3 54.1	6,625 6,209
Amenic	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	1.16	2.87 2.88	0.028	1.09	2.45 2.46	0.022	19.6 30.4	0,005
GIBNO T	6-7 Dec 06 Average	0700-0700	ND(<2.00)	3.01 2.92	0.029	ND(<2.00)	2.59 2.50	0.021	25.1	0.007
Cadrijoni	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<2.00) ND(<2.00)	2.87 2.88	0.024	ND(<2.00) ND(<2.00)	2.45 2.46	0.020	14.4 14.4	0,003
(µg/L)	6-7 Dec 06 Average	0700-0700	ND(<1.00)	3.01 2.92	0,013	ND(<1.00)	2.59 2.50	0,011	13.7	0.002
Calcium	4-5 Dec 06 5-6 Dec 06	0700-0700	17.9 19	2.87 2.88	427.704 455.573	17	2.45 2.46	347.645 369.595	18.7 18.9	80.060 85.977
(mg/L)	6-7 Dec 06 Average	9700-0700	19.2	3.01 2.92	481.185 454.821	18.1	2.59 2.50	391.273 369.504	18.7	89.912 85.316
Chloidlin	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<2.00) ND(<2.00)	2.87 2.88	0.024	ND(<2.00) ND(<2.00)	2.45 2.46	0.020 0.021	14.4	0.003
(018/L)	6-7 Dec 06 Average	0700-0700	ND(<2.00)	3.01	0,025 0,024	ND(<2.00)	2.59 2.50	0.022 0.021	13.7	0.003
Copper	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	49.8 52.7	2.87 2.88	1.190	35.7 35.9	2,45 2.45	0.730 0.737	38.6 41.7	0.460 0,526
(lig/L)	6-7 Dec 06 Average	0700-0700	58.6	3.01	1.469	17.6	2.59 2.50	0.813	44.7	0.656
/ Tron	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	0,512 0,459	2.87	12.234 11.006	0.333 0.279	2.45 2.46	6,810 5,729	44.3 47.9	5.424 5.277
(mg/L)	6-7 Dec 06 Average	0700-0700	0,485	3,01	12,155	0.265	2.59 2.50	5,729 6,089	52.9 48.4	6.426 5.709
Lead	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	1.67 2.29	2.87	0.040 0.055	1.14	2.45 2.46	0.023 0.023	41.6 58.9	0.017 0.032
(µg/L)	6-7 Dec 96 Average	0700-0700	ND(<5.00)	3,01	0.047	ND(<3.00)	2.59	0.023	51.6	0.024
Magnesium	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	5.57 5.74	2.87	133,090	5.33 5.49	2.45 2.46	108.997 112.727	18.1	24.093 24.904
(mg/k)	6-7 Dec 06 Average	0700-0700	5.75	3.01	144,105	5,47 ND(<0,200)	2,59 2.50	118.247 113.323	17.9 18.0	25.858 24.952
Mercury	4-5 Dec 06 5-6 Dec 06	0700-0700	ND(<0.200) ND(<0.200)	2.87	0.002 0.002	ND(<0.200)	2.46	8.002 0.002	14.4	0.000
(Dat)	6-7 Dec 06 Average	0700-0700	ND(<0.200)	3.01	0,003 0.002	ND(<0.200)	2.59 2.50	0.002	13.7	0,000
Malybdenum	5-6 Dec 06	0700-0700 0700-0700	10.1	2,88	0.242	6.28 9.66	2.45 2.46	0.128 0.198	44.i 18.1	0.101
((g/L)	6-7 Dec 06 Average	0700-0700	15.4	3.01	0.386 0.286	12.2	2.59 2.50	0.264	31.7 31.2	0.122 0.089
Niokel	4-5 Dec 06 5-6 Dec 06	9700-0700 9700-9700	2.32 3.87	2.87 2.88	0.055 0.093	2.24 ND(<2.00)		0.046	17.4 77.9	0.610
(ag/1)	6-7 Dec 06 Average	0700-0700	3,01	3.01 2.92	0.075 0.075	2.15	2.59 2.50	0.046 0.038	38.4 49.6	0.029
Selection	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<1.00) ND(<1.00)	2.87 2.88	0.012 0.012	ND(<1.00) ND(<1.00)	2.46	0.010	14.4	0.002
(lug/L)	6-7 Dec 06 Average	0700-0700	ND(<2.00)	3.01 2.92	0.025 0.016	ND(<2.00)	2.59	0.022 0.014	13.7	0.003
. Bilver-	4-5 Dec 06 5-6 Dec 06	9700-0700 0700-0700	ND(<1.00) ND(<1.00)	2.87	0.012 0.012	ND(<1.00) ND(<1.00)	2.46	0.010 0.010	14.4	0.00
(µg/L)	6-7 Dec 06 Average	9700-9700	ND(<1.00)	3.01	0.013 0.012	ND(<1.00	2.59	0.011	13.7 14.2	0.00
Zipe	4-5 Dec 06 5-6 Dec 06	8700-9700 8700-9700	0.103 0.114	2,87 2.8E	2.46 t 2.733	0.074 0.076	2.45 2.46	1.513 1.561	38.5 42,9	0.941
(mg/L)	6-7 Dec 06 Average	0700-0700	0.109	3.01	2,732 2,642	0.078	2.59	1,686	38.3 39.9	1.04

<sup>\*</sup> Secondary clarifier removal efficiency calculated with the WWTP effluent conc. on day 1 was ~46.9% mass removed 168.2 lbs/day; assume zero removal in CCC.

Table E-2. WWTP Unit Process Data (continued).

Analyte	Date	Time	Chlorine Contact Influent (CCCIN) Cong.	Chlorine Contact Influent (CCCIN) Flow (mgd)	Chlorine Contest Influent (CCCPI) Mars (line/day)	WWTP Efficient (TPEF) Gone)	WWTP Efficient (TPET) Flow (mgd)	WWTP Efficient (TPEF) (Mass (Ibs/day)	Chlorine Contact (CCC) Remilifrid	Chlorine Contact (CCC) Mass Removed
BOD (mg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	3.83	2.45	Data discarded Data discarded	9.3 due la unsatisfact due la unsatisfact	2.45 ary Inboratory Q ory Inboratory Q	A/QC findings A/QC findings	Azsume 0*	Assums 0°
	Average 4-5 Dec 06	0700-0700	22	2.45	449.89	20	2.45	408.66	9.2	41,23
TSS (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	24	2.46		24.7 novel by combine			-2.8	-13.96
	Average 4-5 Dec 06	0700-0700	3.4	2.46	471.34 69.53	3.5	2.46	457,71	2.9	-1.99
Ammonia (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	4.8 6.2	2.46 2.59 2.50	98.56 134.03	4.5 5.8	2.46 2.59	92.32 125.28	6.3	6.23 8.74
Vie Allien	Average 4-5 Dec 06	0700-0700	21	2.45	100.70 429.44	20	2.50	96.37 408.66	4.8	20.78
Nitrate/Nitrite (mg/L)	5-6 Dec 06 6-7 Dec 05 Average	0700-0700 0700-0700	20 26	2.46 2.59 2.50	410.66 562.05 467.38	21	2.46 2.59 2.50	430.84 518.41 452.64	-4.9 7.8 3.2	-20.18 43.63 14.75
TKN	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	5,8 8,3	2.45 2.46	118.61 170.42	6.7	2.45	136.90	-15.4 2.5	-18.29
(mg/L)	6-7 Dec 06 Average	0700-0700	9.4	2.59 2.50	203.20	8.1 8.8	2.46 2.59 2.50	166.18 190.09 164.39	6.5	4.24 13.12 -0.31
Total Phosphorus	4-5 Dec 06 5-6 Dec 06	0700-0700	3,73 4,46	2.45 2.46	76.28 91.58	3.72	2.45 2.46	76.01 89.04	0.3	0.27
(mg/L)	6-7 Dec 06 Average	0700-0700	4.55	2.59 2.50	98.36 88.74	4.54	2.59	98.07 87.71	0.3	0.29
Grease and Oil	4-5 Dac 06 5-6 Dec 06	grab grab	ND(<5.50 ND(<5.00)	2.45 2.46	56.24 51.33	ND(<5.30) ND(<5.00)	2.45 2.46	54.15 51.29	3.7	2.09
(mg/L)	6-7 Dec 06 Average	Busp	ND(<5.70)	2.59 2.50	61.61 56.39	ND(<5.10)	2.59 2.50	55.08 53.51	10.6 5.1	6.53 2.89
TPH Diesel Range	4-Dec-06 5-Dec-06	greb grab	1200 790	2.45 2.46	24.54 16.22	690 830	2,45 2,46	14.10	42.5 -5.0	10.44
(ppb)	6-Dec-06 Average	grab	5601	2.59 2.50	12,11 17.62	4000	2,59 2.50	86.40 39.18	-613.7 -122.3	-74.30 -21.55
TPH-Heavy Range	4-Dec-06 5-Dec-06	grab grab	1700)	2.46	34,91	1600	2,46	32.83	6.0	0.03 2.08
(ppb)	6-Dec-06 Average	grab	1600)	2.59 2.50	34.59 34.07	6900	2.59 2.50	149.04 71.52	-330.9 -109.9	-114.46 -37.45
Aluminum	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	0.27	2.45 2.46	5,521 5,359	0.243 0.252	2.45 2.46	4.965 5.170	10.1 3.5	0.556 0.189
(ting/L)	6-7 Dec 06 Average	0700-0700	0.228	2.59 2.50	4.929 5.270	0.246	2.59 2.50	5.314 5.150	-7.8 2.3	-0.385 0.120
Antonic	4-5 Dec 06 5-6 Dec 06	0700-0706 0700-0700	1.09	2.45	0.022	1.03	2.45 2.46 2.59	0.021	5.6	-0.003 -0.000
(μg/L)	6-7 Dec 06 Average	0700-0700	ND(<2.00)	2.59 2.50	0.022	ND(<2.00)	2.50	0.022 6.022	0.1 -3.4	-0.001
Cadmium (µg/L)	4-5 Dec 06 5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700 0700-0700	ND(<2.00) ND(<2.00) ND(<1.00)	2.45 2.46 2.59	0.020 0.021 0.011	ND(<2.00) ND(<2.00) ND(<1.00)	2.45 2.46 2.59	0.020 0.021 0.011	0.1	0.000 0.000 0.000
	Average 4-5 Dec 06	0700-0700	17	2.50	347.645	16.6	2.50	0.017 339.188	0.1	0.000 8.457
Calcium (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	18.1	2.46 2.59	369.595 391.273	18.4	2.46	377,502 408.251	-2,1 -4.3	-7.906 -16.979
Kan She Fish St	Average 4-5 Dec 06	0700-0760	ND(<2.00)	2.50	369.504 8.020	ND(<2.00)	2.50	374,980	-1.5	-5.476 0.000
(Chromium	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	ND(<2.00) ND(<2.00)	2.46 2.59	0.021	ND(<2.00) ND(<2.00)	2.46 2.59	0.021	0.1	0.000
April Personal	Average 4-5 Dec 06	0700-0700	35.7	2.50	0.021	4.10	2.50	0.021	0.1 8.5	0.000
Copper (jug/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	35.9 37.6	2.46 2.59	0.737	36.7 34.8	2.46 2.59	0,753 0,752	-2.1 7.5	-0.016 0.061
Angel Comment	Average 4-5 Dec 06	0700-0700	0.333	2.50	0.760 6.810	0.269	2.50	0.724 5.496	19.3	1.313
Lron  ≠ (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700 0700-0700	0.279 0.265	2.46 2.59 2.50	5.729 5.729 6.089	0.258 0.258	2.46	5.293 5,573 5,454	7.6 2.7 10.4	0.435 0.156
le de la companya de Companya de la companya de la compa	4-5 Dec 06	0700-0700 0700-0700	1,14	2.45	0.023	3.37	2.50	0.069	-195.4	0.635 -0.046
Lead (LEAL)	5-6 Dec 06 6-7 Dec 06 Average	0700-0700	ND(<5.00)	2.46 2.59 2.50	0.023 0.054 0.033	1.05 ND(<5.00)	2.46 2.59 2.50	0,022 0,054 0,048	4.6 0.1 -44.5	0.001 0.000 -0.015
Magnesium	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	5.33	2.45	108.997	5.24 5.64	2.45	107,069	1.8	1,928
(mg/L)	6-7 Dec 06 Average	0700-0700	5,47	2,59 2,50	118.247	5.66	2.59	122,259	-3.4 -1.5	-4.013 -1.690
Merousy	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<0.200) ND(<0.200)	2.45	0.002 0.002	ND(<0.200) ND(<0.200)	2.45 2.46	0.002	0.1	0.00.0
(μg/L)	6-7 Dec 86 Average	0700-0700	ND(<0.200)	2.59 2.50	0.602 0.002	ND(<0.200)	2.59 2.50	0,002	0,1	0.000
Molybdenum	4-5 Dec 06 5-6 Dec 06	9700-9700 9700-9700	6.28 9.66	2,45	0.128 0.198	5.67 9.91	2.45 2.46	0,116	9,8 -2.5	0.013
(μg/L)	6-7 Dac 06 Average	6700-0700	12.2	2.59 2.50	0.264 0.197	10.8	2.59 2.50	0,233 0.184	11.5 6.4	0.030 0.013
Nickel	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	2.24 ND(<2.00)	2.45 2.46	0.046 0,021	2.45 2.64	2.45 2.46	0.050 0.054	-9.3 -163.8	-0.064 -0.034
(hg/L)	6-7 Dec 06 Average	6700-0706	2.15	2.59 2.50	0.046 0.038	ND(⊴.00)	2.59 2.50	0.022 0.042	53.5 -11.5	0,025 -0.004
Solonium	4-3 Dec 06 5-6 Dec 06	0700-0700 0700-0700	ND(<1.00) ND(<1.00)	2.45 2.46	0.010	ND(<1.00) ND(<1.00)	2,45 2,46	0.010 0.010	0.1 0.1	0.000 0.000
(µg/L)	6-7 Dec 06 Average	0700-0700	ND(<2.00)	2.59 2.50	0.022 0.014	ND(<2.00)	2.59 2.50	0.022 0.014	0.1	0.00G 0.000
Silver	4-5 Dec 06 5-6 Dec 06	9700-0700 9700-0700	ND(<1.00) ND(<1.00)	2.45 2.46	9,010 0.010	ND(<1.00) ND(<1.00)	2.46	0.010	0.1	0.000
(µg/L)	6-7 Dec 06 Average	5700-5700	ND(<1.00)	2.59 2.50	0.011 0.010	ND(<1.00)	2.50	0.011	0.1	0,000
Zinc	4-5 Dec 06 5-6 Dec 06	0700-07 <b>0</b> 0 0700-07 <b>0</b> 0	0.074 0.076	2.45 2.46	1.513	0.07 0.079	2,45 2,46	1.430	5.5	-0.083
(mg/L)	6-7 Dec 06 Average	0700-0700	0.078	2.59	1.686 1.587	0.112	2.59 2.50	2.419 1.823	-43.5 -14.9	-0.73 -0.23

<sup>\*</sup> Secondary clarifier removal efficiency calculated with the WWTP effluent conc. (9.3 mg/L) on day 1 was ~46.9% mass removed 168.2 lbs/day; assume zero removal in CCC.

Table E-3. WWTP Unit Process Removal Efficiency Summary.

Analyta	Date	Time	Primary Classifies	Primary Clarifier Removal	Primery Clerifier Mass	Trickling Filter Removal	Trickling Filter Mass	Secondary Clarifier Removal	Second- ary Clarifier	Chiorina Contact Removal	Chlories Contact CCC	WWTP Efficient Mass	(the below values should approxima	Check in the left column to those in the right inni)
			Influent Mair	Efficiency (%)	Removed (be/day)	Efficiency (%)	Removed (lbs/day)	Efficiency (%)	Mass Removed (lbs/day)	Eme. (%)	Mass Removed (ibs/day)	(ibs/day)	Sum of Unit Process Mass Removed (lbs/day)	Primary Clerifier Influent Mars Minus Effluent Mars (los/day)
BOD	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	2029.87	39.9	809,83	63.4		46,9 scarded due to					1751.7	1839.8
(mg/L)	6-7 Dec 06	0700-0700 0700-0700	7587.06	68.6	5206.50	43.8	Data di 1041.50	scarded due to	unsatisfactory 625.34	9.2	JQC finding 41.23	408.66	6914.57	7178.40
TSS	5-6 Dec 06	0700-0700	7339.20	67.9	4981,80	38.0	895,22	58.1	682.10	-2.8	-11.96	506.76	6545,16	6832,44
(aug/L)	6-7 Dec 06 Average	0700-0700	6131.07 7019.11	65.7	4028.19 4738.83	-2.9	-61.85 624.96	58.)	clarifier	/CCC	13.64	570.3 495.22	4969.0 6031.14	5085.8 6561.40
	4-5 Dec 06	0700-0700	698.81	19.1	133.42	78.4	443.38	29.0	653.72 28.44	-2.9	-1.99	71.52	603.25	627.29
Ammonia (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	767.28 826.66	26.1 10.2	200,31 84.47	65.8 69.2	378,97 513.35	34.8 27.7	52.50 51.43	6.3	6.23 8.74	92.32 125.28	638.02 657.99	674.96 701.38
	4-5 Dec 06	0700-0700	764.25	18.2	139.40	71.5 -375.0	445,24	30.5	44.12	4.3	4.33	96.37	633.09	667.88 -365.40
Mitrate/Nitrite	5-6 Dec 06	0700-0700	116.76	-175.1 -22.7	-75.77 -26.47	-379.2	-446.36 -543.10	5.4 25.5	24.54 140.82	4.8	20.78 -20.18	430.84	-476.80 -448.93	-314.08
(mg/L)	6-7 Dec 06 Average	0700-0700	137.78	8.D -30.6	10.99	-582.9 -445.7	-739.10 -576.19	19.9 17.9	139.68 101.68	7.B 3.2	14.75	518.41 452.64	-544.80 -490.18	-380.64 -353.37
TKN	4-5 Dec 06 5-6 Dec 06	0700-0700 0700-0700	1098.13	26.8 19.4	294.69 372.46	67.0 63.3	538.60 566.97	44.2 35.4	94.03	-15.4 2.5	-18.29 4.24	136.90	909.05	961.23 1101.50
(mg/L)	6-7 Dec 06 Average	0700-0700	1343.32	26.3 27.5	353,73 340,29	65.6 65.3	649.42 585.00	26.3	72.48 86.62	6.5	13.12	190.09	1088.75 1011.60	1153.24 1071.99
31	4-5 Dea D6	0700-0700	205.32	37.7	77.36	-1.2	-1.49	26.6	27.66	0.3	0.27	76.01	103.80	129.31
Total Phosphorus (mg/L)	5-6 06 6-7 Dec 06	0700-0700	208.50 215.28	29.9 32.6	62,28 70,24	-0.6 -6.0	-0.90 -8.66	21.0	26.63 26,20	2.B 0.3	0.29	89.04 98.07	90.55 88.07	119.46
	4-5 Dec 06		209.70 865.19	81.8	69.96 707.48	79.2	·3.68	23.2	26.83	1.2	2.09	87.71	94.14	121.99 811.04
Greass and Oll' (mg/L)	5-6 Dec 06 6-7 Dec 06	grab grab	244.53 225.95	39.0	95.33	76.4	282.69	34,4	7.08	0.1	0.04	54.15 51.29	345.69 154.67	193.24 170.87
15. y	Average	grab	445.22	65.1 71.1	147.10 316.63	51.9	0.00 174.80	9.0	1.05 5.58	10.6	6.53 2.89	55,08 53.51	499.98	391.72
TPH Diesel Range	4-Dec-06 5-Dec-06	grab	1763,66 467.04	89.0 62.9	1570.24 293.96	76.9 74.1	148.79	31,5 54.9	11,30	42.5 -5.0	10.44	14.10	1740.77 441.22	1749.56 450.01
(ppb)	6-Dec-06 Average	grab	447.77 892,82	68.9 81.1	308.61 724.27	75.6 75,5	105.14	56.1 46.8	15.46 15.50	-613.7 -122.3	-74.30 -21.55	86.40 39.18	354.92 845.64	361,37 853.65
CONTROL OF	4-Dec-06	grab	898.47	78.E	708.02	65.6	124.98	37.8	19.85	0.1	0.03	32.69	852.88	865.7E
TPH-Heavy Range (ppb)	5-Dec-06 6-Dec-06	gint	366.96 447.77	69,9 77,9	256,55 348,82	37.8 28.1	41.78 27.83	36.7 40.0	20.24 23.05	6.0 -330.9	2.08 -114.46	32.83 149.04	320.65 285.25	334.13 298.73
Maria.	4-5 Dec 06	0700-0700	571.07 44.591	76,7	437,80 30,605	-2.6	-0.357	38.2 52.1	5.996	-109.9	0.556	71.52 4.97	486.26 36.799	499.55 39.625
Aluminum (sig/L)	5-6 Dec 06 6-7 Dec 06	0786-0760 0700-0700	48,706 46,844	74.6 79.0	36,352 37,010	-14.5 -45.0	-1.790 -4.422	52.8 57.3	6.006 6.625	3.5 -7.8	0.189	5.17	40.756 38.828	43.535 41.530
SMINT 7	Average		46.713	74.2	34.655	-20.7	-2.190	54.3	6.209	2.3	0.120	5.15	38.794	41.564
Arsenio	4-5 Dag 06 5-6 Dec 06	0700-0700	0.050 0.058	31.6 39.9	0.016 0.023	-1.8 -5.1	-0.001	19.6 30.4	0.005	5,6 -16,9	-0.003	0.02	0.022	0,029
(re/l)	6-7 Dec 06 Average	0700-0700	0.000	36.0	0.000	0.0	0.000	0,0 25.1	0.000	0.1 -3.4	-0.000	0.02	0.000 0.025	-0.022 0.032
Cadnuom	4-5 Dec 06 5-6 Dec 06		0.033 0.033	10.6	0.004 0.004	0.0	0.000	14.4	0.003	0.1	0.000	0.02	0,007 0,007	0.013 0.013
(µg/L)	6-7 Dec 06		0.048	10.6 67.7	0.032	0.0	0.000	13.7	0.003 0.002	0.1	0.000	9.01 9.02	0.034 0.016	0.037
#70 max	Average 4-5 Dec 06		0.038 665,532	34.5	0.013 150.734	-3.5	-17.854	14.3	80.060	2.4	8.457	339.19	221.396	326.344
Galejum (mg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	697.224 726.773	21.7	151.142 151.573	-3.8 -3.2	-20.888 -18.555	18.9	85.977 89.912	-2.1 -4.3	-7.906 -16,979		208.325 205.951	319.722 318.521
egil Marios (S. 1975) Marios	Average 4-5 Dec 06	0700-0700	696.510	21.7	151.150	-3.5	-19.099	8.81	85.316	-1.5	-5.476 0.000	374.98	0.064	321,529 0.070
Chromium	5-6 Dec 06 6-7 Dec 06	0700-0700	0.090 0.088 0.097	67.0	0.060	0.0	0.000	14.4	0.003	0.1 0.1 0.1	0.000	0.02	0,061 0,070	0.067
(µg/L)	Average	## T. O. P. V. A. V. 17 A	0,092	68.2 67.1	0.066 0.062	0.0	0.000	13.7	0.003	0.1	0.000	0.02	0.065	0.071
Copper	4-5 Dec 06 5-6 Dec 06		3.328 3.736	36.5 57.7	I.878 2.155	-2.3 0.6	-0.033 0.009	38.6 41.7	0.460 0.526	8.5 -2.1	0.062		2.368 2.674	2.660 2.983
(µg/L)	6-7 Dec 06 Average	0700-0700	3.720 3.595	54.2 56.1	2.016 2.016	-6.4 -2.7	-0.108 -0.044	44.7	0.656 0.547	7.5	0.061		2.625 2.556	2.968 2.870
	F. 4-5 Dec 06	0700-0700	34.60H	59,5	20.592	-8.7	-1.220	44.3	5.424	19.3	1.313	5,50	26.109	29.111
lron (mg/L)	5-6 Dec 06 6-7 Dec 06		37.030 42.022	66,2 72,1	24.497 30.301	-9,3 -28.0	-1.164 -3.278	47.9 52.9	5,277 6,426	7.6	0.435 0.156	5.57	29.045 33,605	31.736 36.449
	4-5 Dec 06	0700-0700	37.886 0.202	66.3 72.9	25.130 0,148	9.2	-1.887 0.905	48.4	5.709 0.017	10.4 -195.4	-0.046	a State of the late of the lat	29.587 0.124	32.432 0.133
Load (pg/L)	5-6 Dec 06 6-7 Dec 06	0700-0700	0.175	73.1	0.128	-44.9 0.0	0.000	58.9 0.0	0.032	4.6 0.1	0.001	0.02	0.141	0.154 -0.054
The state of the s	Average		0.189	73,0	0,138	-11.9	-0.005	51.6	0,024	-44.5	) -0.013	0.05	0,142	0.141
Magnesium	4-5 Dec 06 5-6 Dec 06	0700-0700	196.824	17.4	33,401 31,508	-4.5 -3.6	-7.142 -5.968	18.1	24.093 24.904	-2.6	1.928	6 115.71	47.458	84.937 81.112
(org/L)	6-7 Dec 96 Average	0700-0700	204.254 197,695	14.3	29.220 31.376	-1.6	-2.783 -5.298	17.9	25.858 24.952	-3,4 -1.5	-4.013	3 122.26 0 115.01	48,282 49,340	81,995 82.681
Mercury	4-5 Dec 06	0700-0700 0700-0700		67.8 87.2	0,006	0.0	0.000	14.4	0.000	0.1	0.000			0.007
(µg/L)	6-7 Dec 06 Average			83.0 82.2	0.013	0,0	0.000	13.7	0.000	0,1	0.000	0.002	0.015	0.016
AVA D	4-5 Dec 06		0.389	80.9	0.315	-284.4	-0.212	14.2	0,101	9,8	0.013	-	0.217	0.273
Molybdonum (µg/L)	5-6 Dec 86 6-7 Dec 86		0.592	16.1	0.050	3.8 7.8	0.012	18.1	0.044	-2.5 11.5	0.036	0.23	0,111	0.170 0.359
	Average 4-5 Dec 66	5 0700-0700	0.452	33.3 50.8	0.150	-90.9 6.1	-0.053 0.0045	31.2	0.089	-9.3	-0.004	The state of the s	THE CASE STREET, STREE	0.268
Nickel (µg/L)	5-6 Dec 00	5 0700-0700	0.126	43.1	0.0545 0.0514	-60.6 -21.9	-0.0436	77.9	0.0723	-163.8	-0.03	36 0.05	0.050	0.072 0.106
(lefters)	Average		0.135	40.2 45.0	0,0606	-25.5	-0.0167 -0.0186	49.6	0.0290	-11.5	-0.00	43 0.04	0.075	0.093
Belenium	4-5 Dec 66 5-6 Dec 06	0700-0700	0.046	61.1	0.023	0.0 51.9	0.000	14.4	0.002	0.1	00.00			0.028 0.036
(µg/L)	6-7 Dec 0s Average		0.034	10.2 35.5	0.004 0.014	0.0 17.3	0.000	13.7	0.003	0, i D. I	0.00	0.02	9.007	0.013 0.026
	4-5 Dec 66		0.042	64.5	0.027	0.0	0.000	14.4	0.002	0.1	0.00	0 0.01	0.029	0.032
Bilver (µg/L)	5-6 Dec 06 6-7 Dec 0	6 0700-070	0.035	62.4 56.0	0.025 9.020	0,0	0.000	14.4	0,002	0.1	0.00	0.01	0.021	0.029 0.024
- <u> </u>	Average 4-5 Dec 0		0.039	61.2	0.024	0.0	0.000	14.2 38.5	0.002	0.1	00,00 80,0	0.01	0.026	0.028 6.656
Zinc	5-6 Dec 0	6 0700-070	7,906	54.3	4.962 4.296	1.9 5.8	0.060	42.9	1.173	-3.9	-0.06	60 1.62	5.617	6.286
(mg/L)	6-7 Dac 0		7.647	64.4	4,925 4,728	-23.9 -5.4	-0.649 -0.127	38,3 39.9	1.046				4.588	5.227 6.056

<sup>\*</sup> Secondary clarifier removal efficiency calculated with the WWTP effluent conc. (9.3 mg/L) on day 1 was -42.7% mass removed 141.5 lbs/day; assume zero removal in CCC.

## APPENDIX F SOLO POINT WWTP DATA

Table F-1. 2004 Solo Point Data Summary.

2004	Flow (mgd)	Sludge Pumped (gal)	Influent BOD (mg/L)	BOD Primary Effluent (mg/L)	BOD Einal Effluent (mg/L)	% Removal BOD	Influent ISS (mg/L)	Primary Effluent (mg/L)	Final Effluent (mg/L)	% Removal TSS	Fecal Coliform (col/100 ml)	Chlorine Residual	pН
Max.	4.6	33300	924	264	49	95	250	98	27	93	0.43		7.3
Jan Min	2.49	3060	99	70	13	74	114	45	14	79	0.08		7.6
Avg	3.47	10277	223	130	25	89	185	66	20	89	0.21	<200	
<u> Max.</u>	4.99	12870	203	126	20	92	381	81	30	96	0.39		6.9
Feb. Min	2.74	8010	78	48	12	74	95	33	9	76	0.03		6.6
Ave	3.86	10471	143	82	16	89	169	58	21	88	0.19	<200	
Max.	3.52	12150	223	107	24	94	218	83	27	97	0.23		7.2
-Mar : Min	2.48	5130	69	30	8	83	117	32	5	84	0.05		6.4
Ave	3	8419	154	74	- 16	90	169	51	17	90	0.14	<200	
Max Max	3.38	18000	291	165	29	94	360	93	27	95	0.41		7.4
Apr Min	2.06	8010	102	41	14	83	38	22	10	74	0.07 -		5.3
Ave	2.91 -	11283	180	91	20	89	222	67	19	91	0.15	<200	
Max :	3.36	18000	330	195	24	95	446	149	31	96	0.4		6.9
.∍May <u>Min</u>	2.37	9000	120	72	11	86	105	40	14	80	0.04		6.1
Ave	2.84	11642	212	104	18	92	233	. 78	21	91	0.15	<200	
Max	3.02	17100	375	150	24	95	450	200	31	96	0.23		7.0
Jun . Min	2.63	7200	126	66	12	86	154	40	17	84	. 0		6.3
Ave.	2.84	12261	216	111	19	91	272	96	23	92	0.15	<200	
hul Man	3.05	22500	477	141	29	96	816	101	29	98	0.23		6.9
Jul Mm	2.13	8100	124	78	9	85	203	40	11	. 86	0		6.5
- Ave	2.82	14255	264	114	19	93	286	79	19	93	0.12	<200	
Max	4	38700	300	126	23	96	381	94	26	96	0.26		7.1
Aug Mm.	2.4	9000	102	48	8	86	187	15	11	86	0.03		. 6.6
Ave	2.96	17623	186	88	15	92	251	70	17	93	0.14	<200	
Max	3.7	17100	285	114	31	95	366	76	22	98	0.39		7.2
Sep Min	2.8	9000	93	53	8	0	157	34	8	86	0.1		6.8
Avg.	3.21	12603	170	84	15	91	219	57	15	93	0.19	<200	
Max	4	25200	320	129	30	97	330	135	16	97	0.41		7.2
Oct. L. Min.	2.66	10800	99	71	10	75	102	43	7	85	0.1		6.7
Ave.	3.12	13094	193	102	16	92	214	63	11	95	0.22	<200	
Max.	3.83	20700	288	141	25	97	319	86	25	95	0.3		6.9
Nov at Min.	2.62	9000	54	42	7	84	166	48	12	88	0.07		6.5
Ave.	3.14	11880	183	103	17	91	235	68	18	92	0.16	<200	
- Max	3.87	17100	309	159	33	94	348	91	30	96	0.27		7.0
Dec Min	2.29	9000	45	54	9	56	168	40	13	87	0.07		6,5
Ave	3.07	11119	173	99	20	88	227	65	19	92	0.15	<200	
Average of Monthly Averages	3.10	11002	184	91	24	101	211	64	25	92	0.16		

Table F-2. 2005 Solo Point Data Summary.

	2005	Flow (mgd)	Sludge Pumped (gal)	Influent BOD (mg/L)	BOD Primary Effluent (mg/L)	BOD Final Effluent (mg/L)	% Removal BOD	Influent TSS (mg/L)	Primary Effluent (mg/L)	Emal Effluent (mg/L)	% Removal TSS	Fecal Coliform (col/100 ml)	Chlorine Residual	pН
1 2 4 40 4 3	Max.	4.29	18900	381	165	34	94	455	89	39	95		0.3	7.5
Jan	Min	2.52	8100	108	14	_ 13	_ 0	57	23	9	79		0.04	6.6
	Ave	3.16	12861	188	109	23	88	216	63	20	91	<200	0.14	
	Max.	3.86	18900	300	177	27	95	324	140	· 42	96		0.21	7.0
. Feb	Min.	2.46	9900	119	82	8	87	147	37	8	. 86		0.08	6.3
-5-65 jal	Avg	2.98	13243	203	126	16	92	244	74	19	92	<200	0.14	
	- Max	4.09	20700	354	168	23	95	388	115	29	- 94		0.24	7.2
Mar	Min	2.48	12600	111	72	12	87	156	56	15	87		0	6.0
	Ave	3.08	15823	197	117	16	92	243	79	21	91	<200	0.11	
	Max.	4.78	30960	408	162	22	96	331	107	25	95		0.15	6,9
Apr	Min.	2.28	11700	117	41	11	87	152	54	14	89		0.16	6.3
\$255 (A)	Avg	3.1	15402	209	113	16	92	237	78	19	92	<200	0.1	Processor and annual process of the state of
	Max.	3.87	24300	342	168	44	95	343	110	26	95 ·		0.22	6.9
May	· Min-	2.25	16200	117	62	11	70	99	41	. 11	81		0.07	6.5
The state of the s	· Avg.	3.15	19074	174	101	18	90	220	79	19	91	<200	0.12	None of the last o
	Max	3.58	27900	299	167	21	94	335	97	26	95		0.24	7.1
Jun	Min.	1.64	16200	125	86	. 13	87	199	57	12	90		0.05	6.5
	Avg -	2.93	18780	200	116	18	91	254	7:3	17	93	<200	0.14	
	Max.	3.54	31700	332	149	22	94	289	115	49	96		0.21	7.0
Jul	Min -	1.73	12600	132	68	14	86	161	62	12	70		0.08	6.5
	Avg	2.93	20825	185	115	18	90	231	81	18	92	<200	0.13	-
444,749	Max	3.7	29430	272	178	23	96	317	86	26	96		0.28	7.0
Aug	Min.	2.16	17190	122	68	7	86	131	45	9	89		0.08	6.5
	Ave.	3.07	21137	179	105	15	92	240	68	13	95	<200	0.13	
	Max	3.9	24660	268	140	19	94	333	102	38	96		0.19	7.0
Sep .	Min.	1.93	11520	118	. 65	13	88	128	56	10	85		0.04	-
	Avg	3.07	20117	186	106	16	91	251	76	16	94	<200	0.1	6.5
	Max	4.23	24210	244	157	20	95	345	111	20	96		0.21	
-Oct	Mbn	2.71	18000	140	70	12	88	187	52	12	91		0.04	7,0
	Avg	3.34	20665	172	102	16	91	258	73	16	94	<200	0.1	6.4
	Max	4.41	29070	347	173	22	94	334	100	22	95		0.35	
Nov	Min.	2.47	12600	123	0	14	87	165	53	14	90		0.05	6.9
15.00	Avg	3.44	21612	185	119	18	91	248	73	18	93	<200	0.13	6.3
1.415	Max.	4	27360	264	149	24	93	377	219	32	97		0.28	
Dec	Min	2.99	14130	84	56	10	84	144	57	8	85		0.01	6.8
14 14	Ave	3.48	19893	156	99	18	88	227	88	22	90	<200	0.12	6.0
			- 25 T ( FILL - 3)											
Mor	age of ably ages	3,14	16578	180	104	24	105	224	71	25	92	<200	0.12	

Table F-3. 2006 Solo Point Data Summary.

2006	Flow	Sludge Pumped	Influent BOD	BOD Primary	BOD Final	-%	Influent TSS	Pu <del>rsuy</del> Effluent	Final Efflyent	%	Fecal	Chlorine	
2000	(mgd)	(gal)	(mg/L)	Effluent (mg/L)	Effluent (mg/L)	Removal BOD	(mg/L)	(mg/L)	(mg/L)	Removal	(col/100 ml)	Residual	pН
Max.	10.13	19080	199	124	27	92	368	101	26	96	0.34		7.1-
Jan ₹ . Min.	3.48	14400	41	33	9	67	82	42	15	77	0.08		6.1
- Ave	6.84	17211	80	59	14	82	132	68	19	85	0.18	<200	
≥ Max	11.67	19080	114	69	17	93	167	86	22	91	0.38		7.2
Feb  Mm.	4.66	8370	31	25	4	58	62	30	6	76	0.2		6.5
Ave	7.21	12064	67	45	10	85	107	54	15	86	0.29	<200	
Max Max	5,94	15390	204	136	33	91	230	92	23	92	0.36		6.9
Mar Min	3,28	9900	77	56	10	75	117	53	15	81	0.08		6.3
Avg.	4.62	12289	122	85	17	86	170	72	19	89	0.19	<200	
Max	4.09	61560	230	147	20	93	414	. 89	32	96	0.22		6,9
Apr Min	2.91	10800	57	4	4	84	134	52	17	84	0.04		5.9
TAVE.	3.74	18981	140	86	15	89	202	75	22	* 89	0.1	<200	
Max	4.49	22320	- 280	147	22	94	351	108	28	96	0.17		6.4
May Min	2.59	9000	97	84	12	84	161	38	13	88	0.06		5.4
Avg.	3.43	15901	172	111	16	91	246	73	18	93	0.11	<200	
Max Max	4.06	27270	290	139	28	94	379	94	20	96	0.21		7.1
Jun. Min	2.48	14400	62	68	16	68	131	35	. 12	89	0.02	-	6.6
Avg	3.33	21160	171	99	20	88	244	68	16	93	0.13	<200	
Max	3.45	34020	338	221	30	95	302	168	24	97	0.31		7.3
Jul Min	2.55	13500	103	55	10	82	170	57	5	90	0.08		6.6
Avg	3.03	19975	183	101	18	90	237	83	16	93	0.15	<200	
i a Max.	3.08	23130	261	120	27	95	326	77	15	98	0.47		7.0
Aug Min	2.49	11160	109	51	7	85	184	33	7	93	80.0		6.3
Avg	2.78	15137	164	81	14	91	250	61	10	96	0.19	<200	
L. Max	3.13	16740	247	98	20	94	287	197	15	98	0.21		7.1
Sep. Min	2.4	11160	92	43	7	86	120	38	6	91	0.05		6,3
-Ave	2,75	. 13824	151	69	15	90	221	69	11	95	0.13	<200	
Max.	3.3	15680	746	192	34	95	501	74	23	98	0.34		7.2
Oct Min.	2.54	9270	118	54	9	80	127	35	7	89	0.09		6.4
Ave	2.88	12267	185	87	19	90	224	58	13	94	0.19	<200	
Max.	6.12	23200	330	193	40	95	474	122	25	96	0.8		7.2
Nov Min	1.81	10710	51	36	11	67	126	42	12	84	0.08		6.5
± Avp	3.96	18332	137	77	18	87	188	65	17	91	0.25	<200	
Max	7.27	16560	211	107	26	90	236	77	24	94	0.31		7.2
Dec Min	2.8	10530	47	28	12	68	49	16	9	74	0		6.7
Avg	4.64	13819	110	56	17	85	148	49	17	89	0.18	<200	
		erman ik										ernétri III	
Average of Monthly Averages	4.10	15913	140	80	16	88	197	66	16	91	0.17		

Table F-4. Solo Point WWTP Sludge Data (2006)

2006	Thickener		Secondary Digester Sludge to Drying Beds	
	%TS	%TVS	%TS	%TVS
Jan	3.81	84.40	none	попе
	1.32	78.00		
	2.46	83.30		
	2.07	74.40		
Feb	1.92	84.40	5.18	68.06
	2.40	77.90		
	2.82	89.50		
	3.97	86.50		
<b>%</b> ZE-851	4.32	87.00	4.49	67.62
	3.42	86.00		
Mar	3.32	78.50		
	2.72	85.40		
	3.42	83.70		
	3.85	87.60	4.84	67.47
	2.93	82.10		
Apr	2.63	85.80		
	3.62	83.20		
	2.90	84.40		
	3.23	83.00	none	none
May	2.83			
1777		81.90		
<b>沙江外对抗</b>	3.42	81.90		
	2.99	86.60		
	3.47	76.10	4.93	66.88
Jun'	2,76	79.30		
(ALAS)	3.09	77.90		
100 E	3.17	80.30		
	3.09	78.80	5.03	67.1
A Jul	2.75	78.70		
100	2.69	77.30		
	2.96	79.60	4.87	68.29
Aug	2.76	81.70		
9,670 d	3.20	86.50		
50.	2.68	83.50		
	2.42	82.50		65.87
Sep	2.84	82.20	4.43	
	2.78	81,20		
\$4.1%	3.34	85.00		
	2.67	81.60	4.68	68.29
Oct	3,24	82.60		
∲Oct	3.80	88.20		
	3.87	88.30		
	3.86	83.90	4.33	66.58
Nov	3.95	80.00		
	2.69	75.20		
	3.23	<b>7</b> 9.50		
	3,37	82,30	4.42 67.23	67.23
	3.35	81.10		
Dec	4.21	74.90		
	2.80	86,60		
	3.55	77.40		
Average	3.10	82.15	4.72	67.34

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APPENDIX G

WWTP PHOTOS

Photo 1.36-inch influent sewer line (view from manhole)

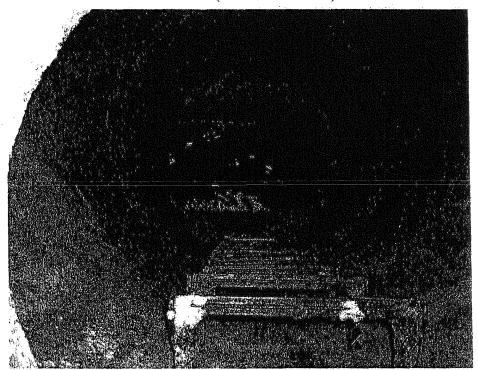


Photo 2. View of headworks (preliminary treatment including screening and grit removal)

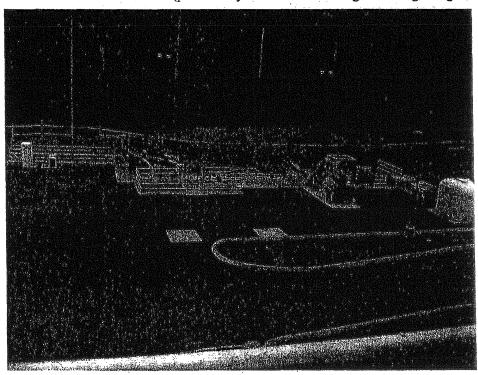


Photo 3. Influent sampler and split channel.

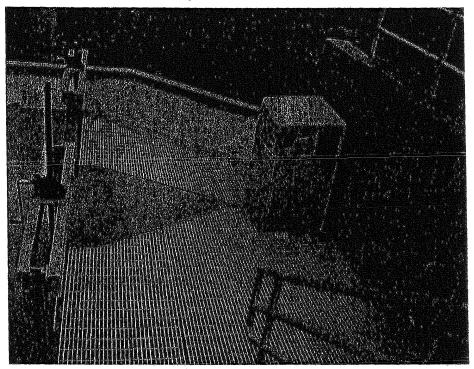


Photo 4. Parallel self-cleaning screens.

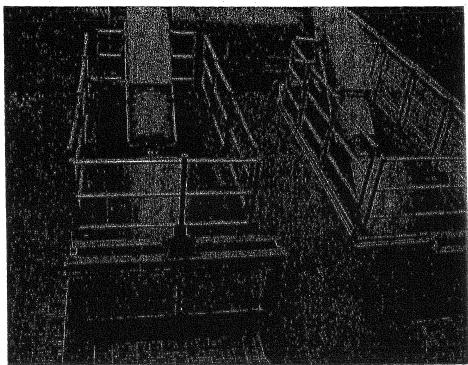


Photo 5. View of parallel influent screens, conveyor and dumpster.

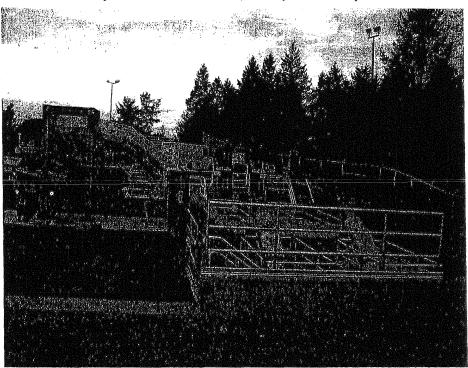


Photo 6. Close-up of screen

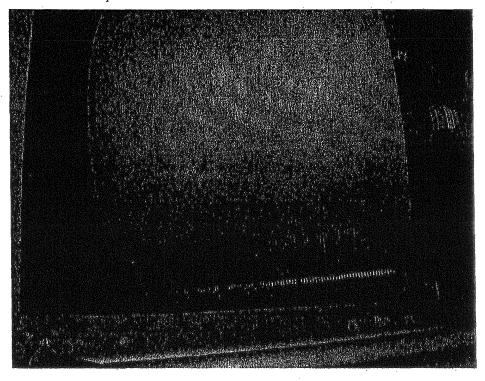


Photo 7. Conveyor belt for screenings.

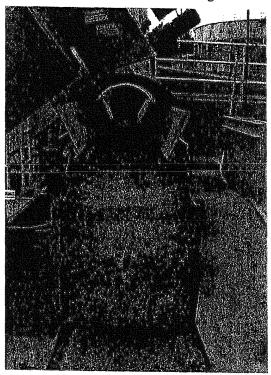


Photo 8. Empty grit chamber.

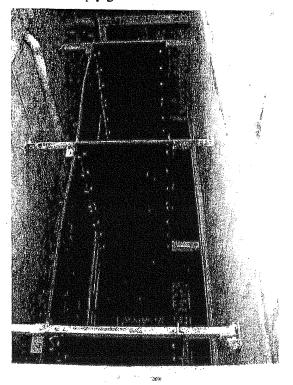


Photo 9. Empty grit chamber

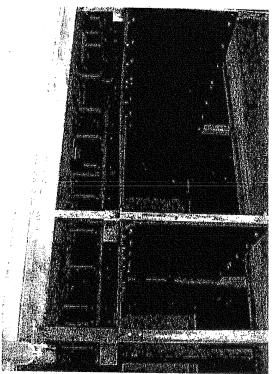


Photo 10. Empty grit chamber

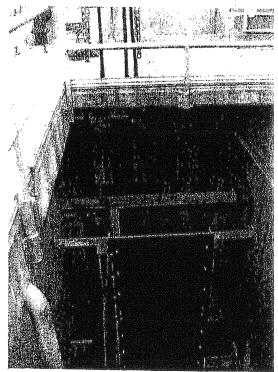


Photo 11. Sludge thickener supernatant return to primary clarifier influent.

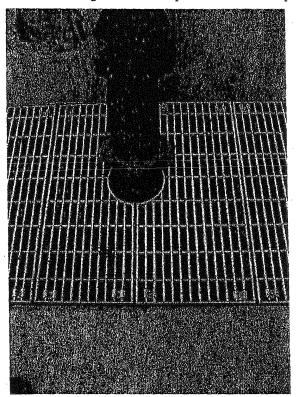


Photo 12. Empty primary clarifier.

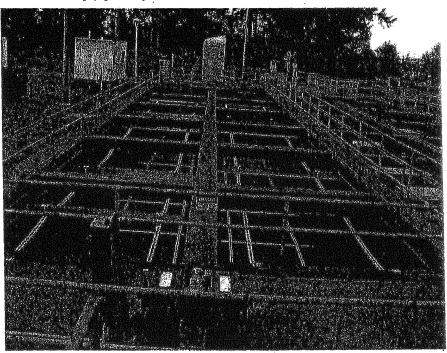


Photo 13. Empty primary clarifier.

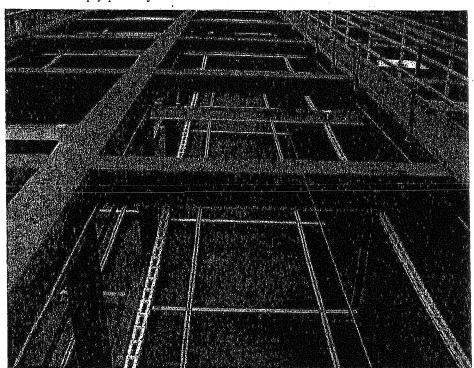


Photo 14. Empty primary clarifier effluent weir

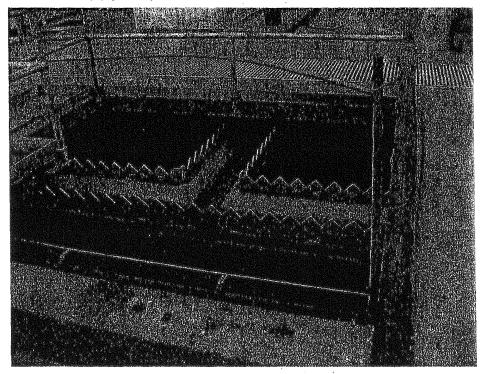


Photo 15. Primary clarifier effluent weir (note grease/oil scum)

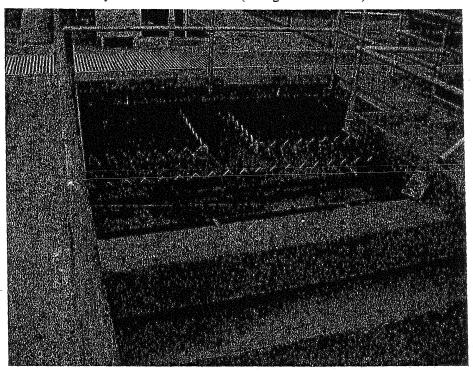


Photo 16. One (west) of two primary clarifier influent 24-inch pipes.

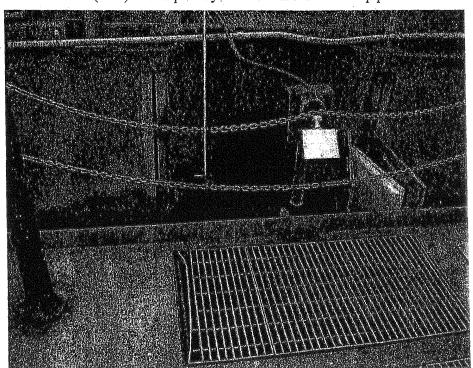


Photo 17. One (east) of two primary clarifier influent 24-inch pipes.

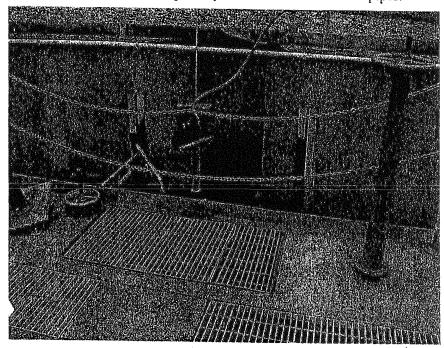


Photo 18. Channels that split flow to parallel primary clarifiers

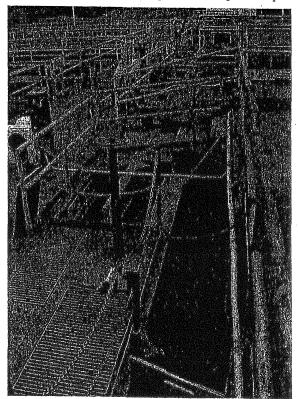


Photo 19. Primary clarifiers



Photo 20. Three pumps that feed primary clarifier effluent to trickling filters

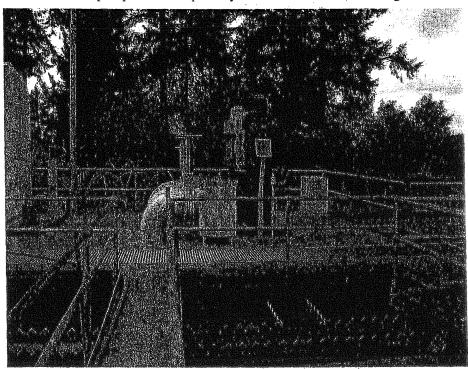


Photo 21. Primary sludge collection hopper

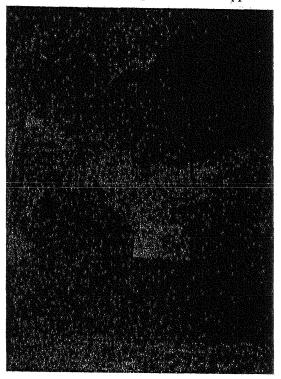


Photo 22. Scum on primary clarifiers

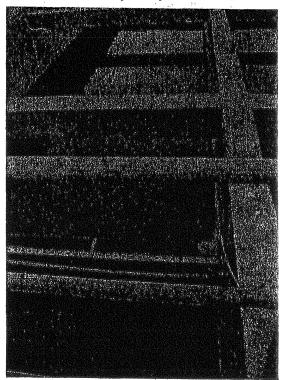


Photo 23. View of primary clarifiers and chlorine contact chambers

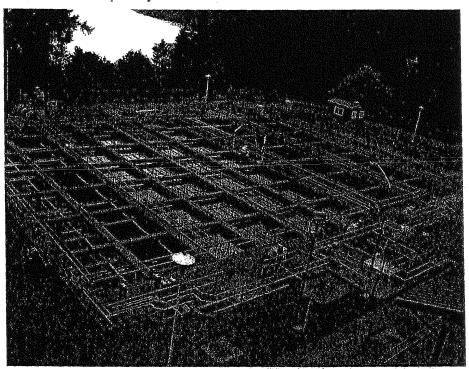


Photo 24. Three pumps that feed primary clarifier effluent to trickling filters

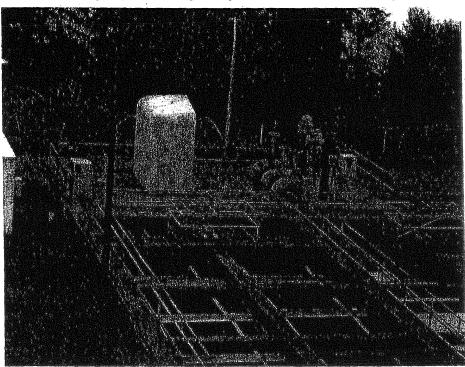


Photo 25. Parallel Trickling Filters

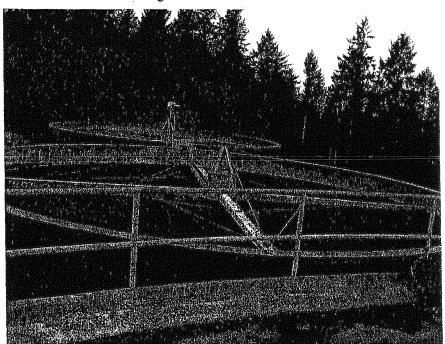


Photo 26. Top of west trickling filter

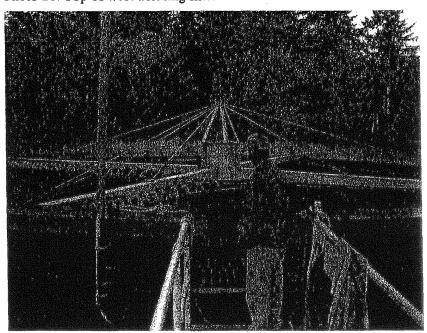


Photo 27. Top of east trickling filter

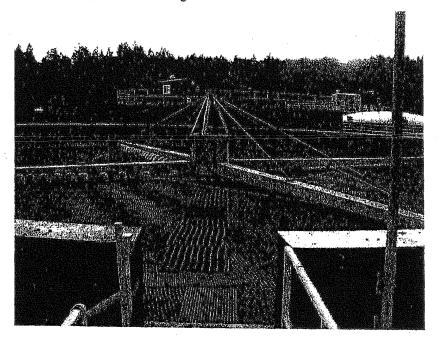


Photo 28. Trickling filter distribution arm and plastic media

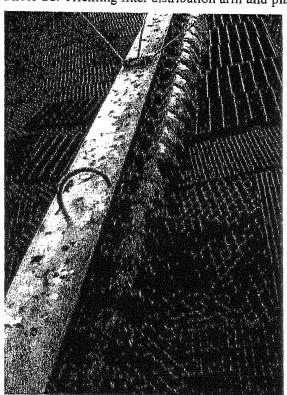


Photo 29. Splitter box that gravity feeds trickling filter effluent to secondary clarifiers

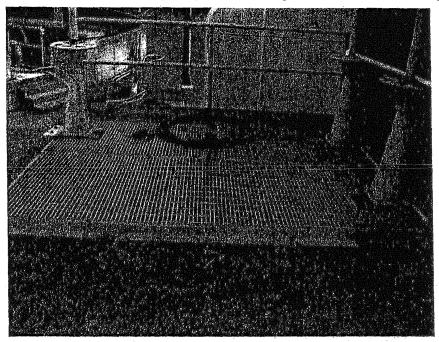


Photo 30. East secondary clarifier

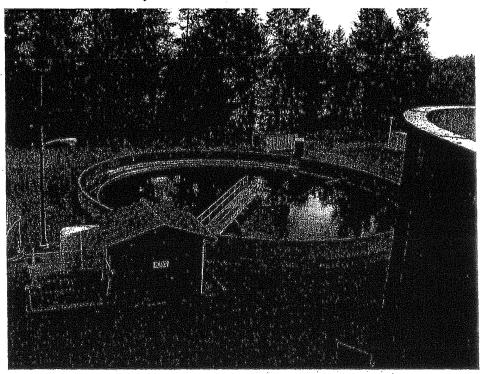


Photo 31. West secondary clarifier

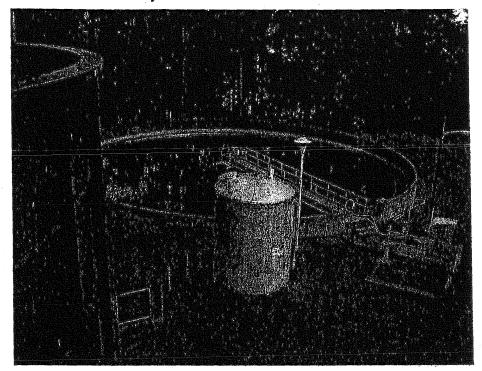


Photo 32. Secondary clarifier scraper arm

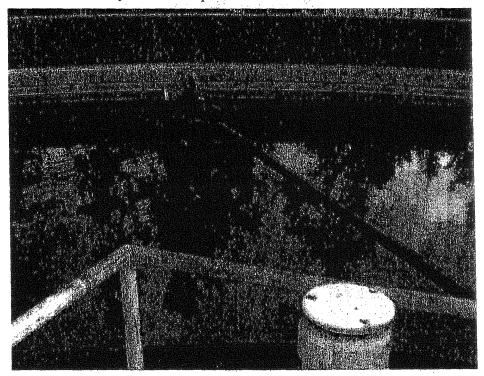


Photo 33. Secondary clarifier scum collector

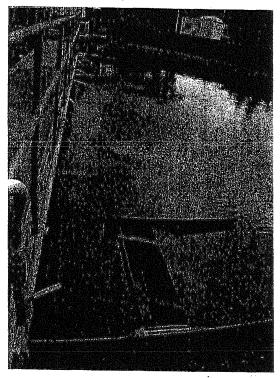


Photo 34. Secondary clarifier brushes on scraper arm

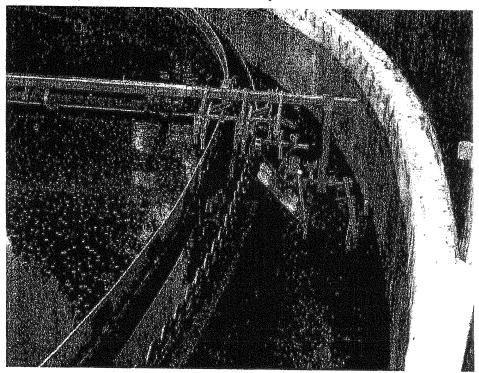


Photo 35. Empty east chlorine contact chamber

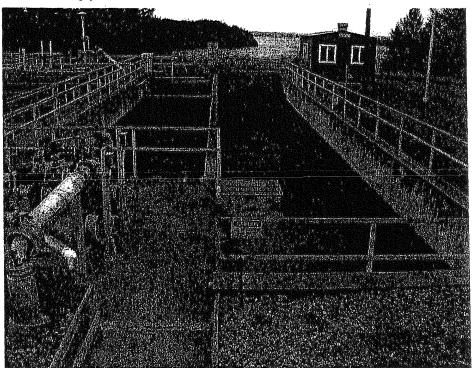


Photo 36. Empty chlorine contact chamber

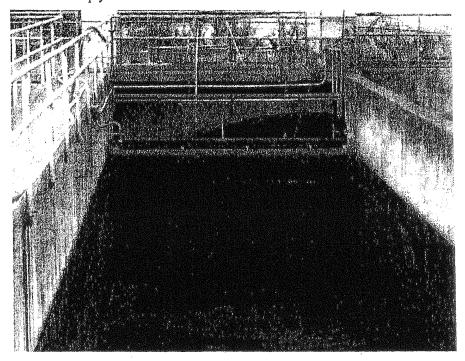


Photo 37. Chlorine contact chamber - effluent scum collection and weir

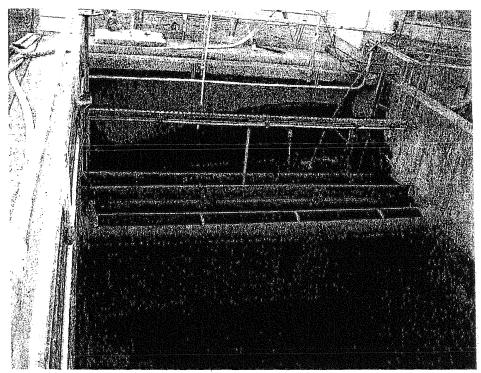


Photo 38. Chlorine contact chamber - close-up of scum collector and weir

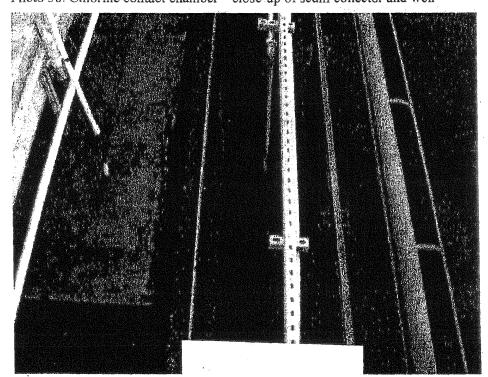


Photo 39. West chlorine contact chamber

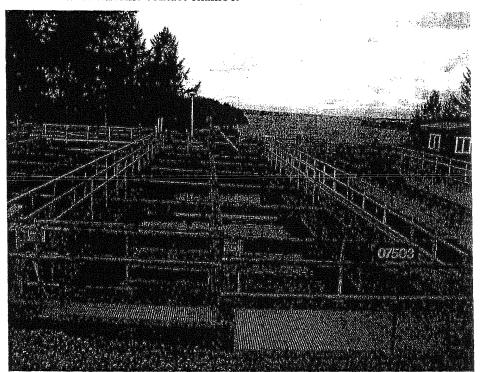


Photo 40. Chlorine contact chamber effluent weir and seum collector

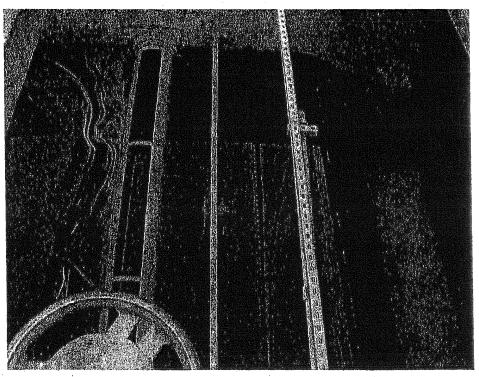


Photo 41. Chlorine contact chamber effluent weir

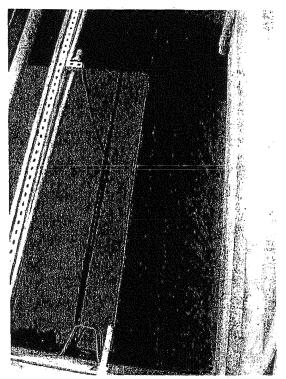


Photo 42. Sludge thickener and grease concentrator.



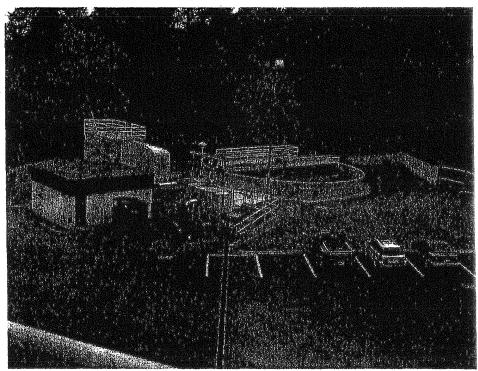


Photo 43. Sludge thickener

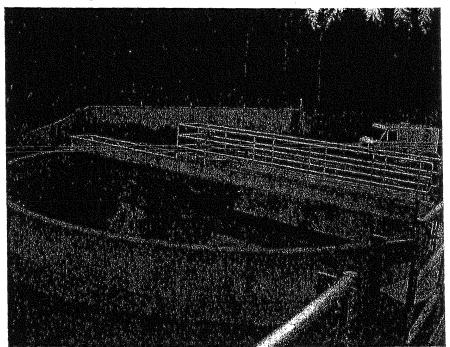


Photo 44. Two-stage anaerobic digestion tanks (two primary tanks – left and right, one secondary tank – center)

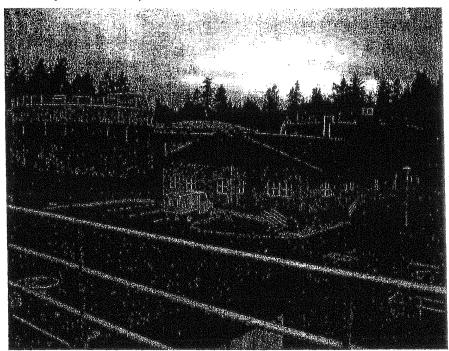


Photo 45. Anaerobic digesters

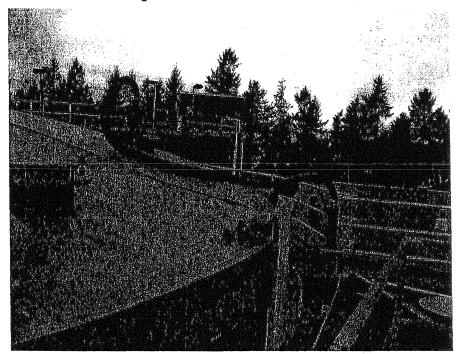


Photo 46. Tops of secondary (front) and primary (rear) digesters.

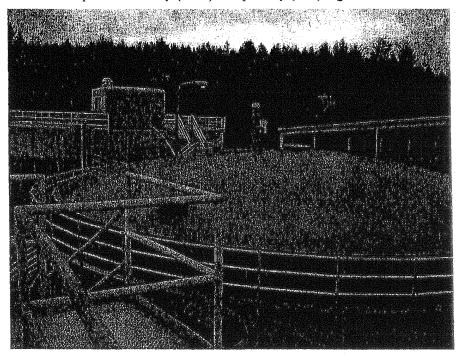


Photo 47. Digester supernatant

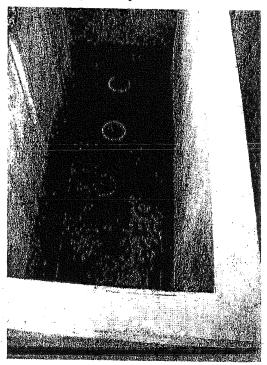


Photo 48. Digester supernatant

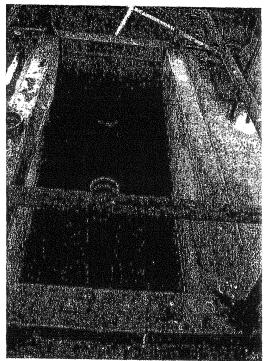


Photo 49. Secondary digester and sludge drying beds

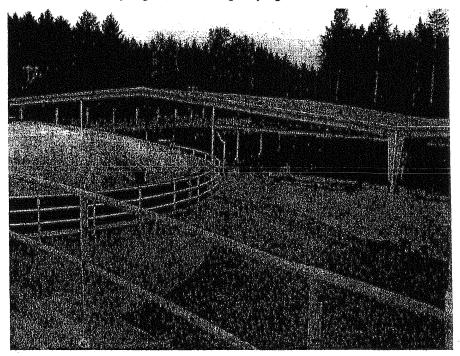


Photo 50. Excess gas flare and drying beds

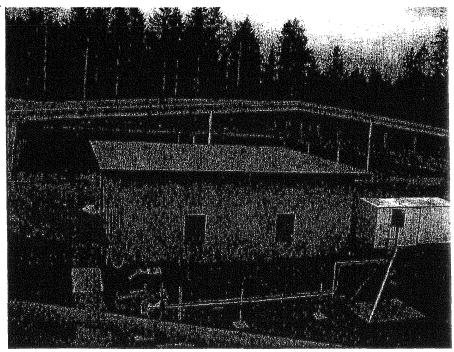
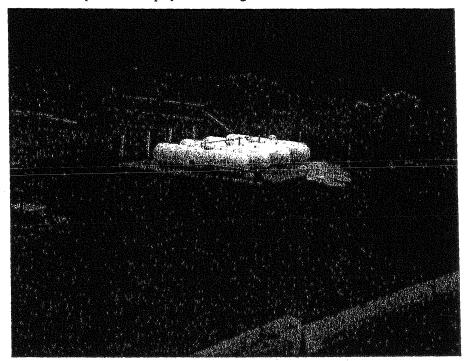


Photo 51. Propane back-up system for digesters/heat



## APPENDIX H

SAMPLING-BASED
WWTP PERFORMANCE EVALUATION
ANALYTICAL REPORTS
(IN ELECTRONIC VERSION ONLY)